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DNS of turbulent channel flow: can we imitate conjugate heat-transfer with a Robin boundary condition?

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Abstract – Turbulent heat fluxes, temperature variance and associated budgets obtained from the Direct Numerical Simulation of an incompressible turbulent channel flow with a Reynolds number of 150 based on the wall friction velocity and a Prandtl number of 0.71 are presented and analysed for four different cases: imposed temperature at the wall (Dirichlet), imposed heat flux (Neumann), heat exchange coefficient (Robin) and 3D conjugate heat transfer. Present results show that a Robin boundary condition can imitate most of the one point statistics obtained with conjugate heat-transfer accurately compared to the statistics obtained with an imposed temperature or heat flux at the wall.

1. Introduction

Most of the DNS of the turbulent channel flow performed with a passive scalar are based on an imposed temperature at the wall (Kasagi et al. 1992, Kawamura et al. 1998). When the temperature is imposed at the wall, there is a close similarity between thermal and momentum low-speed near-wall streaks (Abe et al. 2009).

In a small number of DNS, a constant heat flux is imposed at the wall (Tiselj et al. 2001). However, it is widely recognized that neither isothermal nor isoflux boundary conditions can realistically mimic the actual heat transfer in real life where the wall has a thickness, especially when the thermal diffusivity of the fluid and solid are of the same order of magnitude. When such a coupling is considered, it is referred as conjugate heat-transfer. To the authors' knowledge Tiselj et al. (2001) were the first to investigate by DNS the influence of the thermal boundary conditions with a direct comparison between conjugate heat transfer, imposed temperature and imposed heat flux at the wall.

In the present paper, the turbulent heat-fluxes, the temperature variance and the associated budgets obtained for three different boundary conditions (imposed temperature (isoT), imposed heat flux (isoQ), heat exchange coefficient (Robin)) and conjugate heat transfer (Conjug) are compared. In the present conjugate simulations, the ratio of thermal diffusivity and conductivity between the solid and the fluid can be equal to 2, 1 and 0.5: 9 conjugate simulations were performed (the heat flux is imposed at the outer wall of the solid domain).

2. Numerical setup

Present simulations are based on the open-source software Incompact3d (<https://code.google.com/p/incompact3d/>) developed at Université de Poitiers and Imperial College London by Laizet et al. (2011). The details of the numerical methods employed here are similar to the ones given in Flageul et al. (2014): high-order compact finite difference schemes in the fluid domain are combined with a mixed finite difference/spectral discretization in the solid domain. The number of computational cells is equal to 256x193x256 and the domain size is [25.6,2,8.52]. For the conjugate heat transfer cases, the solid domain is on top and bottom of the fluid one, as sketched figure 1. For such cases, the equation of evolution of the passive scalar reads

$$\begin{aligned}\partial_t T + \partial_j (Tu_j) &= \alpha_f \partial_{jj}^2 T \quad \text{in the fluid} \\ \partial_t T_s &= \frac{\alpha_f}{G_1} \partial_{jj}^2 T_s \quad \text{in the solid}\end{aligned}\tag{1}$$

$$T_f = T_s \text{ and } \partial_y T_f = G_2 \partial_y T_s \text{ at the interface}$$

where G_1 is the ratio of thermal diffusivities α_f/α_s and G_2 is the ratio of thermal conductivities λ_s/λ_f . Based on those dimensionless numbers, the thermal activity ratio K can be defined with $1/K = G_2 \sqrt{G_1}$ (Tiselj et al. (2012)). The ratio of thermal diffusivities and conductivities considered here lead to $K = [1/2\sqrt{2}; 1/2; 1/\sqrt{2}; 1; \sqrt{2}; 2; 2\sqrt{2}]$. Both for $K = 1/\sqrt{2}$ and $K = \sqrt{2}$, two simulations were performed: $(G_1, G_2) = (2, 1)$, $(G_1, G_2) = (1/2, 2)$ and $(G_1, G_2) = (1/2, 1)$, $(G_1, G_2) = (2, 1/2)$. Theoretical analysis shows that a very low (resp. high) thermal conductivity in the solid domain is equivalent to an imposed heat-flux (resp. imposed temperature) at the fluid boundary. Therefore, for a given G_1 , the lower G_2 , the higher K , the closer to the imposed heat flux case. Accordingly as illustrated in figure 1 for the temperature variance, the higher K , the closer "Conjugate" results move to the imposed heat flux case.

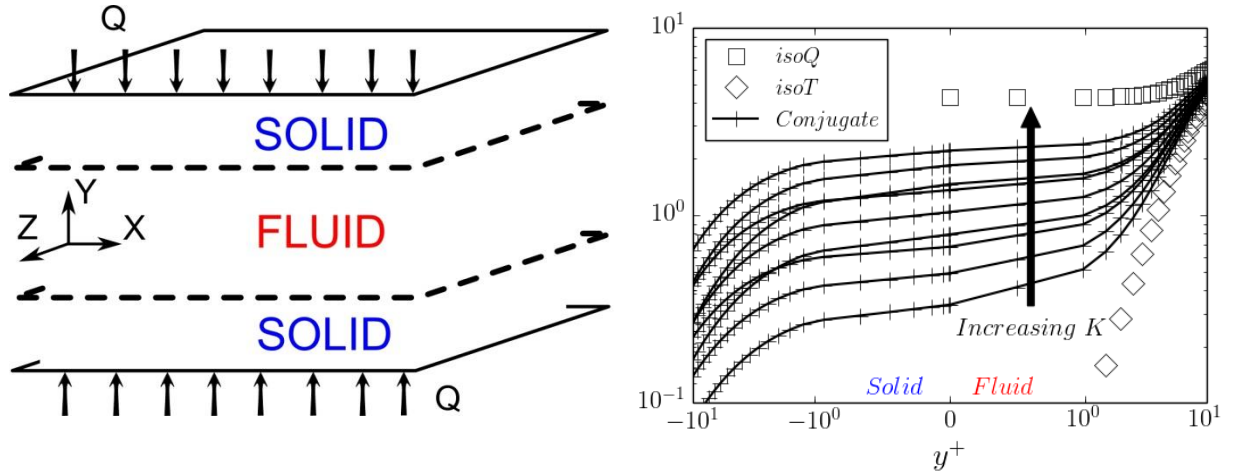


Figure 1: Left: Sketch of the configuration. Right: Temperature variance.

3. Compatibility condition for the non-conjugate cases

One considers a general boundary condition for the temperature at the wall $aT + b\partial_y T = c$. Furthermore, if one assumes the coefficients a , b and c are constant, one obtains:

$$aT + b\partial_y T = c \Rightarrow a\bar{T} + b\partial_y \bar{T} = c \text{ and } aT' + b\partial_y T' = 0 \quad (2)$$

The second condition in (1) can be multiplied by T' or $\partial_y T'$. The resulting 3 equations can be used to build a matrix:

$$\begin{pmatrix} \bar{T} & \partial_y \bar{T} & -1 \\ T'^2 & \partial_y (T'^2)/2 & 0 \\ \partial_y (T'^2)/2 & \partial_y T' \partial_y T' & 0 \end{pmatrix} \begin{pmatrix} a \\ b \\ c \end{pmatrix} = \begin{pmatrix} 0 \\ 0 \\ 0 \end{pmatrix} \Rightarrow 4T'^2 \times \partial_y T' \partial_y T' = \partial_y (T'^2) \times \partial_y (T'^2) \quad (3)$$

The determinant of the matrix must vanish to allow non trivial solutions. The resulting relation connects the values (at the wall) of the temperature variance, its derivative and the wall-normal part of the dissipation rate associated with the temperature variance. One can combine the second and the third lines of the matrix in (3) to obtain: $a^2/b^2 = T'^2 / \partial_y T' \partial_y T'$. Our Robin boundary condition for $(G_1, G_2) = (1, 1)$ was built using this relation with the temperature variance from the isoQ case and the wall-normal part of the dissipation rate from the isoT one. The Robin boundary condition for the other conjugate cases was obtained using cross-multiplication between the one at $(G_1, G_2) = (1, 1)$, and the ratio $T'^2 / \partial_y T' \partial_y T'$ of the conjugate cases.

4. Compatibility condition for the conjugate cases

Assuming the solid domain is semi-infinite in the wall-normal direction and the

case is stationary, one can apply Fourier and Laplace analysis to the solid heat diffusion equation:

$$ik_t \frac{\rho C_p}{\lambda} T = \partial_{yy}^2 T - [k_x^2 + k_z^2] T \xrightarrow{\text{Laplace}} T = \frac{sT_{y=0} + \partial_y T_{y=0}}{s^2 - (k_x^2 + k_z^2) - ik_t \frac{\rho C_p}{\lambda}} \quad (4)$$

The denominator can be written as $s^2 - S^2$ with $S^2 = k_x^2 + k_z^2 + ik_t \rho C_p / \lambda$. Applying an inverse Laplace transform leads to a compatibility condition between the wall-normal heat flux and the temperature at the wall: $\partial_y T_{y=0} \pm S T_{y=0} = 0$. The sign in the expression depends on the sign of the real part of S and on the orientation of the y -axis. This condition is a product in the spectral space, which is equivalent to a convolution in physical space. If one were to neglect the dependency of S on k_x , k_z and k_t , the quadratic norm of the compatibility condition would be $1/S^2 = T'^2 / \partial_y T' \partial_y T'$. As this ratio is used to define our Robin boundary condition, there is strong connection between the conjugate cases and the Robin ones. Using a Robin boundary condition with constant coefficients, one can imitate conjugate heat transfer but neglect the non-local effects (i.e. the convolution).

5. Results

In figure 2, the temperature variance obtained for the conjugate cases and the Robin ones are in between the isoT and the isoQ one. There is a remarkable agreement between the conjugate cases and the Robin ones. It is similar for the dissipation rate associated with the temperature variance, although the agreement between the Robin case and the conjugate ones is degraded for $y^+ \leq 7$. For the ratio of thermal properties considered in the present conjugate simulations, the temperature variance and the associated dissipation rate depends only on the thermal activity ratio K .

The one point correlation coefficient associated with the turbulent heat flux $\langle u'_j T' \rangle$ is $\langle u'_j T' \rangle / (u_{jRMS} T_{RMS})$. In figure 3, the one point correlation coefficient associated with the wall-normal turbulent heat flux obtained with conjugate heat transfer and a Robin boundary condition lies in between the isoT and isoQ cases. There is a good agreement between the Robin case and the conjugate ones, although the agreement is more qualitative for $y^+ \leq 3$. The one point correlation coefficient associated with the streamwise turbulent heat-flux obtained with conjugate heat transfer and a Robin boundary condition lies in between the isoT and isoQ cases. The Robin cases are however now very close to the isoT one. In addition, for a given thermal activity ratio, the one point correlation coefficient for the conjugate cases does not overlap (cases $K = 1/\sqrt{2}$ and $K = \sqrt{2}$).

Therefore, the turbulent heat fluxes depends both on K and G_1 , even if the temperature variance and the associated dissipation rate depends only on K .

In figure 4, the two-point streamwise autocorrelation of the temperature at the wall for the Robin cases is lower than the conjugate and isoQ ones. Oppositely, the two-point streamwise autocorrelation of the wall-normal heat flux at the wall for the Robin cases is higher than the conjugate and isoT ones. As the coefficients in the Robin boundary condition are constants, the autocorrelation of the temperature and wall-normal heat flux are identical. This is obviously not the case for conjugate heat transfer. This confirms the failure of a Robin boundary condition with constant coefficients to mimic the non-local aspects of conjugate heat transfer.

In figure 5, the two point spanwise autocorrelation of the temperature and wall-normal heat flux at the wall show a similar trend, although the impact of the thermal boundary condition is less severe.

In figure 2, the temperature variance in the fluid domain overlap for the simulations at $K=1/\sqrt{2}$ and $K=\sqrt{2}$. As shown figure 6, this is not the case in the solid domain. This leads to distinct second derivatives of the temperature variance in the solid domain (for a given thermal activity ratio K). In the budgets of the temperature variance in the solid domain, ε_θ balances the molecular diffusion. The small difference observed on θ^2 in the solid domain leads to a larger difference on $\varepsilon_{\theta,s}$.

The relative contribution to ε_θ of its wall-normal part is $\frac{\partial_y T' \partial_y T'}{\partial_i T' \partial_i T'}$. As shown figure 7 (left), in the fluid domain, the wall-normal part of $\varepsilon_{\theta,f}$ is dominant in the near-wall region for the conjugate, Robin and isoT cases. Therefore, in the vicinity of the wall, for the conjugate and Robin cases, the value of $\varepsilon_{\theta,f}$ is closer to the isoQ case while its anisotropy is closer to the isoT case. Using the continuity of temperature and heat-flux at the fluid-solid interface and the budgets of the temperature variance in the fluid and solid domains leads to the interface condition:

$$2\partial_y T'_f \partial_y T'_f \left(1 - \frac{\lambda_f^2}{\lambda_s^2}\right) = \partial_{yy} (T_f'^2) - \partial_{yy} (T_s'^2) = \frac{\varepsilon_{\theta,f}}{\alpha_f} - \frac{\varepsilon_{\theta,s}}{\alpha_s} \Leftrightarrow \frac{\partial_y T'_f \partial_y T'_f}{\partial_i T'_f \partial_i T'_f} \left(1 - \frac{1}{G_2^2}\right) = 1 - G_1 \frac{\varepsilon_{\theta,s}}{\varepsilon_{\theta,f}} \quad (5)$$

Assuming the wall-parallel contribution to $\varepsilon_{\theta,f}$ is negligible at the fluid-solid interface leads to:

$$\frac{\varepsilon_{\theta,s}}{\varepsilon_{\theta,f}} = \frac{1}{G_1 G_2^2} = K^2 \quad (6)$$

This is in good agreement with our results: the higher K , the higher $\frac{\varepsilon_{\theta,s}}{\varepsilon_{\theta,f}}$.

In figure 7 (right), the temperature variance in the solid domain near the

fluid-solid interface seems to overlap when the abscissa and ordinate axes are rescaled with G_2 and K respectively. However, the focus on the wall-value indicates large deviations.

The relative contribution of the wall-normal part of $\varepsilon_{\theta,f}$ at the wall as a function of K seems linear with a slope of -0.19 for the ratio of thermal properties considered in this study. However, there are few chances for this trend to be valid for ratio of thermal properties farther from unity as this relative contribution is bounded in $[0,1]$.

6. Discussion

On the one hand, our results show that a Robin boundary condition can imitate accurately conjugate heat-transfer: the temperature variance and the associated budgets are in good agreement. On the other hand, the one point correlation coefficient associated with the streamwise turbulent heat flux and the streamwise autocorrelations at the wall show that there remains a difference between conjugate and non-conjugate heat-transfer.

From section 4, in case of conjugate heat transfer, there is a compatibility condition that is a product in the spectral space, which is equivalent to a convolution in the physical space. Such a condition is non-local and cannot be imitated by a Robin boundary condition with constant coefficients. The theoretical failure of such a Robin boundary condition to mimic the non-local aspect of conjugate heat transfer is confirmed by our results.

The relatively high autocorrelation of the temperature at the wall for the conjugate cases at large separations may be explained by the periodicity and the limited streamwise extension of our domain, even if it is longer than the reference ones (Kasagi et al. 1992, Tiselj et al. 2001). Very large scale thermal structures may also be intrinsic to conjugate heat transfer: those are the only ones able to penetrate deep inside the solid domain. For instance, at $K = 1/\sqrt{2}$, the streamwise autocorrelation of the temperature at the wall at the largest separation is 0.19 for $(G_1, G_2) = (2, 1)$ and 0.14 for $(G_1, G_2) = (1/2, 2)$. The higher G_1 , the lower the thermal diffusion in the solid domain, the more important are very large scale thermal structures.

7. Conclusion

From a RANS perspective, a Robin boundary condition with constant coefficients seems able to mimic conjugate heat transfer: the second moments and their budgets are satisfactorily reproduced (fig. 2). From a LES perspective, this is no longer the case, as shown by the streamwise autocorrelations of the temperature

and wall-normal heat-flux at the wall (fig. 4).

Those conclusions may not be valid for ratio of thermal properties farther from unity than the ones considered here. When the Prandtl number is 0.01, the temperature variance at the wall depends both on K and G_1 (Tiselj et al. (2012)).

Following the analysis developed in section 4, a Robin boundary condition with varying coefficient could offer a better potential to mimic conjugate heat-transfer. However, the coefficients should depend on values of the temperature and wall-normal heat flux at the wall in a non-local fashion: both previous time-steps and surrounding nodes should be considered to mimic the convolution accurately.

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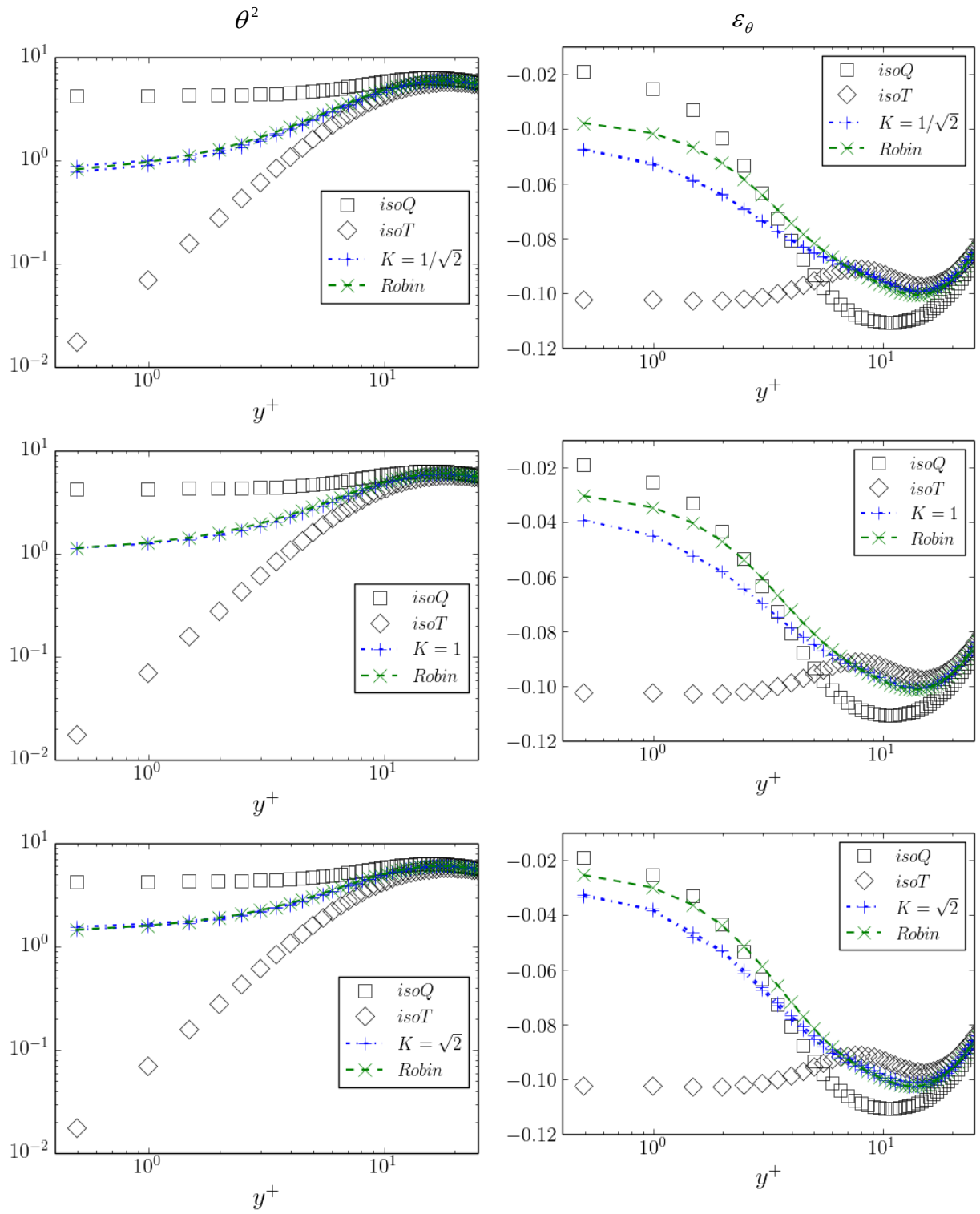


Figure 2. Left: Temperature variance. Right: Associated dissipation rate. Top: $K = 1/\sqrt{2}$. Middle: $K = 1$. Bottom: $K = \sqrt{2}$. +: Conjugate. x: Robin.

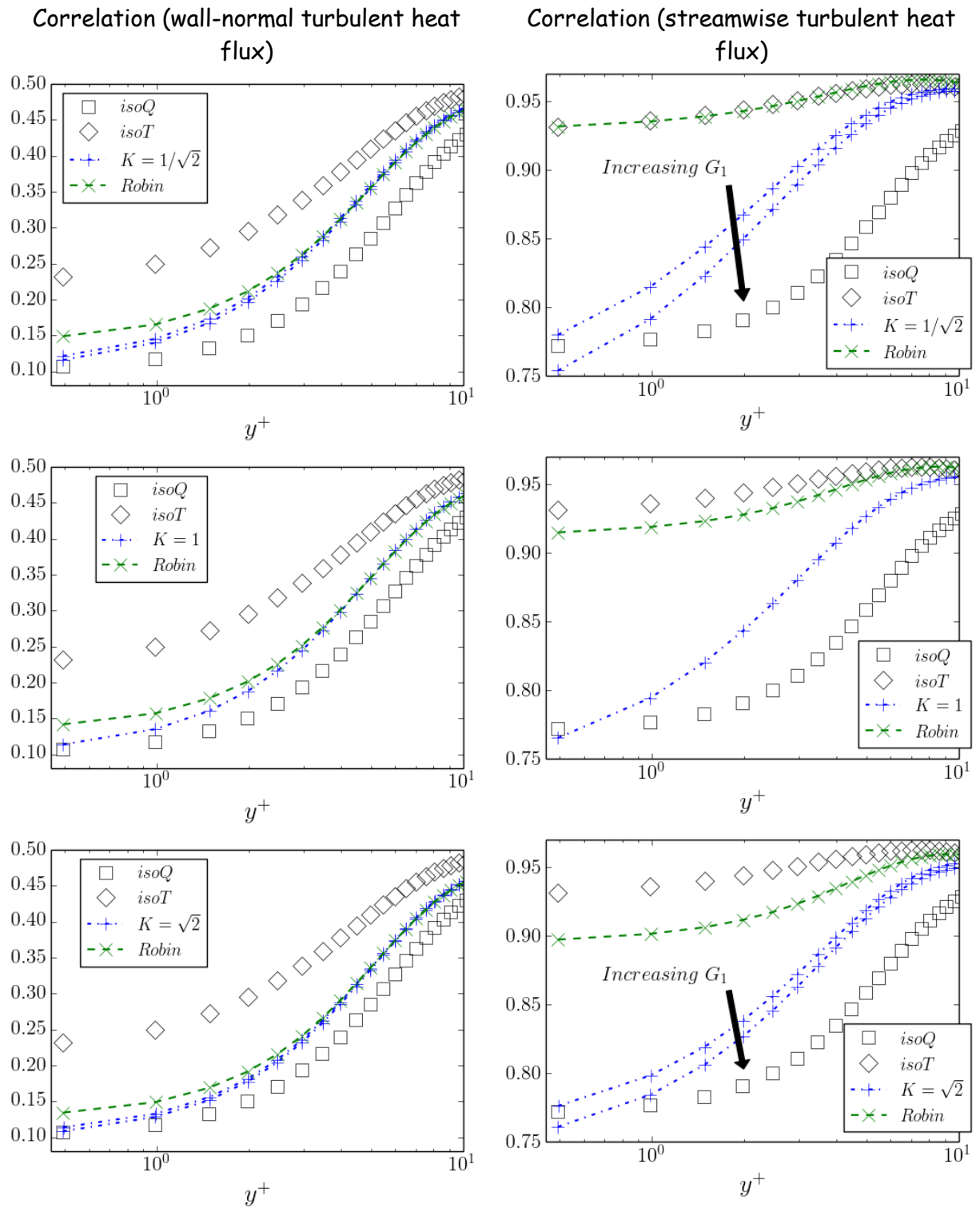


Figure 3: One point correlation coefficient associated with the turbulent heat flux. Left: Wall-normal turbulent heat flux. Right: Streamwise turbulent heat flux. Top: $K = 1/\sqrt{2}$. Middle: $K = 1$. Bottom: $K = \sqrt{2}$. +: Conjugate. $\times$: Robin.

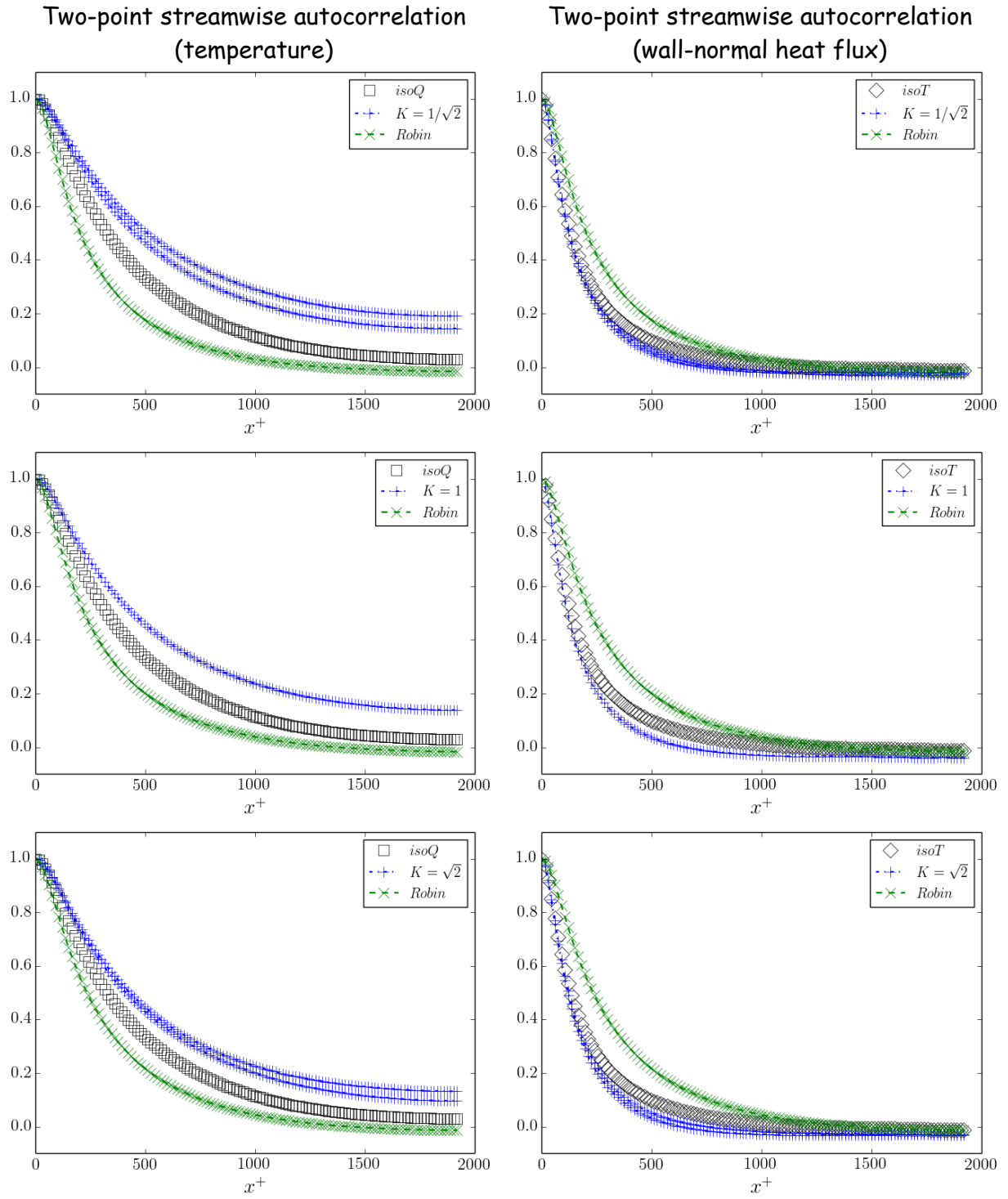


Figure 4: Two-point streamwise autocorrelation at the wall. Left: Temperature. Right: Wall-normal heat flux. Top: $K = 1/\sqrt{2}$. Middle: $K = 1$. Bottom: $K = \sqrt{2}$. +: Conjugate. x: Robin.

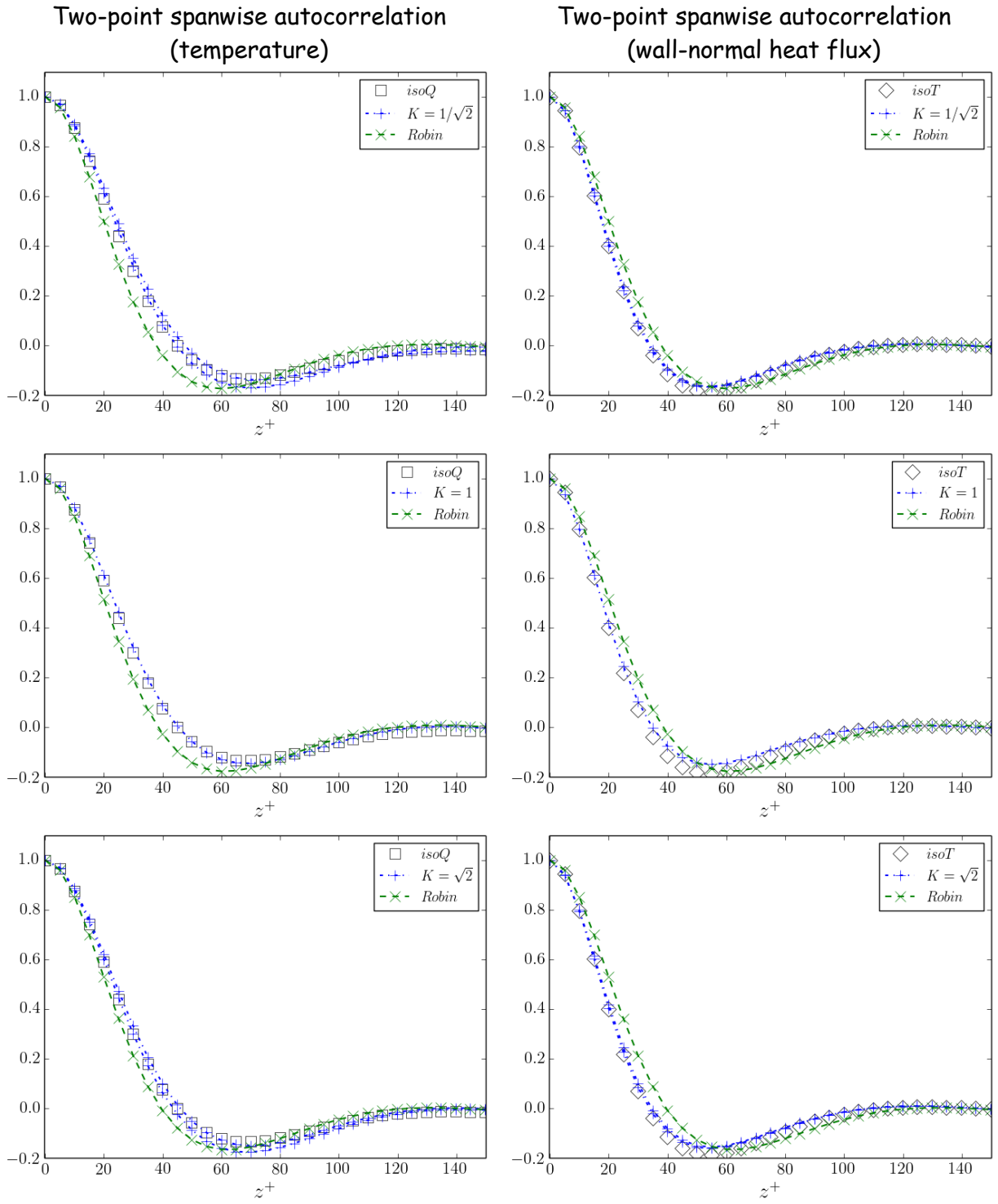


Figure 5: Two-point spanwise autocorrelation at the wall. Left: Temperature. Right: Wall-normal heat flux. Top: $K = 1/\sqrt{2}$. Middle: $K = 1$. Bottom: $K = \sqrt{2}$. +: Conjugate. x: Robin.

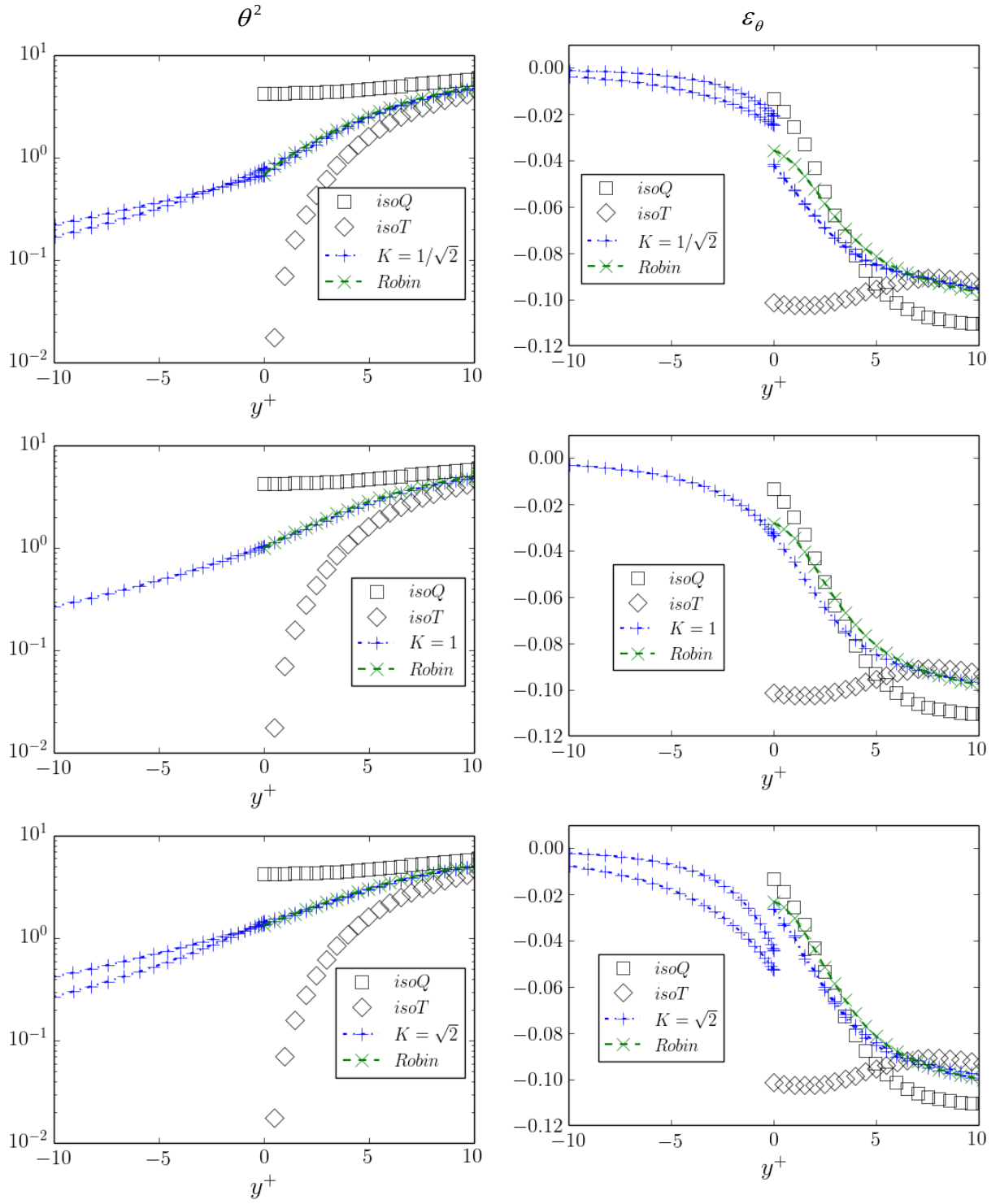


Figure 6: Left: Profile of θ^2 around the fluid-solid interface. Right: Profile of ε_θ around the fluid-solid interface.

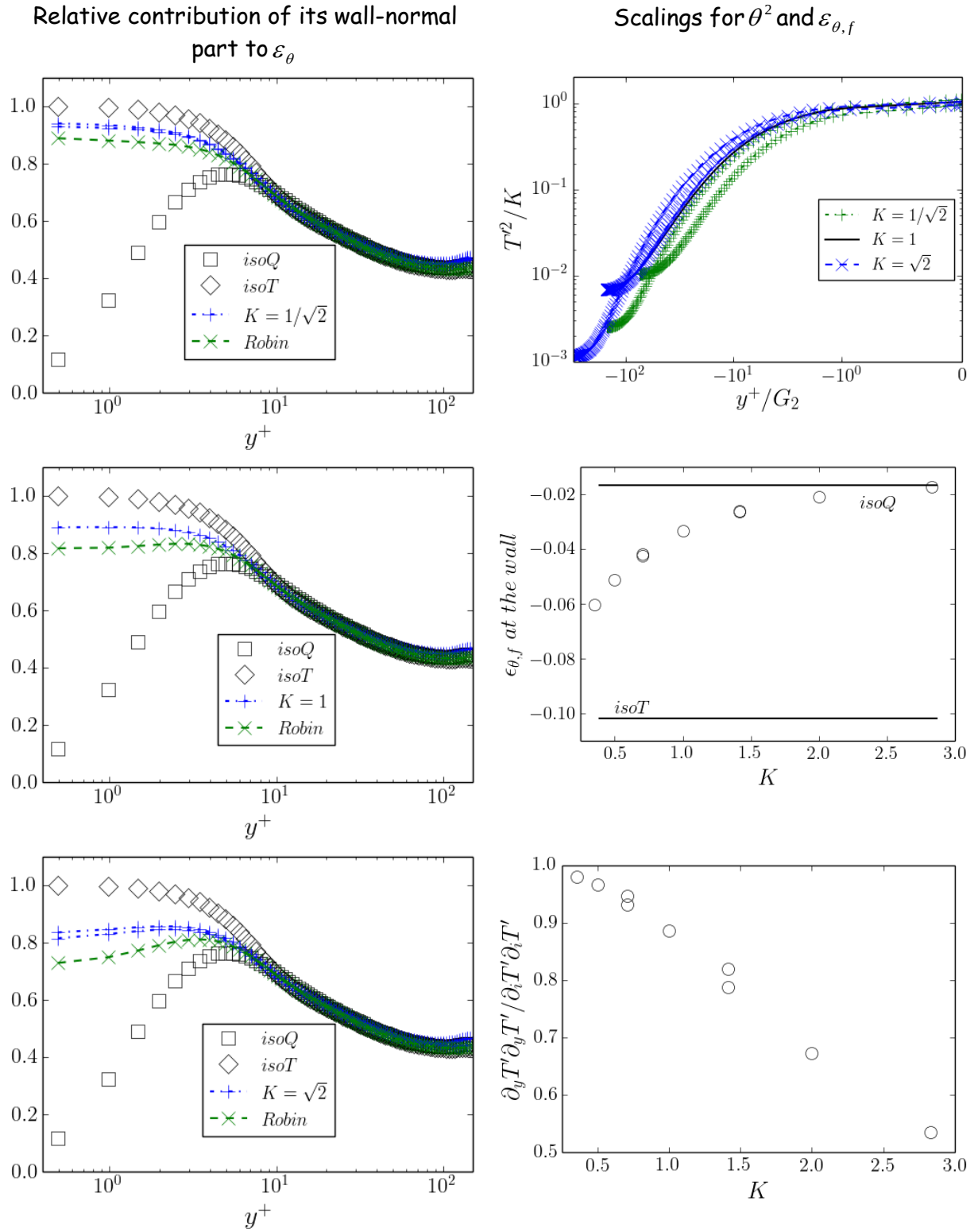


Figure 7: Left: Relative contribution to ε_θ of its wall-normal part. Right: Scaling for θ^2 in the solid domain and for $\varepsilon_{\theta,f}$ and its wall normal contribution to at the fluid-solid interface.