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Mineral dissolution and precipitation under stress: model formulation and application to metamorphic reactions

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7	Key Points:
8	• model of reaction by dissolution-precipitation under stress providing new creep
9	laws for pressure solution and replacement reaction
10	• in the presence of fluid, dissolution-precipitation creep is the dominant deforma-
11	tion mechanism in the Earth's crust
12	• grain shape preferred orientation can only develop near thermodynamic equilib-
13	rium

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14 Abstract

Reactions in the Earth's crust occur through a dissolution-precipitation process in the 15 presence of fluid. Dissolution releases aqueous species which are transported to the lo-16 cus of precipitation. This replacement process generates creep deformation (i.e. dissolution-17 precipitation creep) due to volume change during reaction and stress-controlled mass re-18 distribution in the rock. Reaction under stress also modifies the rock microstructure and 19 the pressure record during metamorphism. A quantitative model for dissolution-precipitation 20 creep is developed here by considering both dissolution and precipitation at grain inter-21 faces to simulate replacement reactions under stress. A new creep law is obtained for pres-22 sure solution, allowing for the reaction- and the diffusion-controlled cases to be modelled 23 with a single expression. It is extended to replacement reactions by introducing volume 24 change during reaction. Deformation mechanism maps are generated with the new creep 25 law, indicating that, when fluid is present, dissolution-precipitation creep is the domi-26 nant deformation mechanism in the Earth's crust. Numerical model reveals that grain 27 shape preferred orientation only develops near thermodynamic equilibrium. This is con-28 sistent with measurements of porphyroblasts preferred orientation in rocks from the Nufe-29 nen Pass (Switzerland) having experienced prograde metamorphism. Kinetics play a key 30 role on the thermodynamic pressure of metamorphic reaction. Near the equilibrium, re-31 action is controlled by either σ_1 or σ_3 depending on the total volume change during re-32 action whereas it is controlled by the mean stress far from the equilibrium. 33

³⁴ 1 Introduction

Stylolites, pressure shadows or flattened pebbles are common observations in the 35 first 15 km of the Earth's crust (Gratier et al., 2013). They are markers of anisotropic 36 mineral dissolution and mass transfer. Dissolution occurs when fluid is undersaturated 37 with respect to equilibrium. As many mineral solubilities increase with pressure (Eugster 38 & Baumgartner, 1987; Dolejš & Manning, 2011), grain-to-grain surfaces under high nor-39 mal stress can locally dissolve. The dissolved aqueous species then diffuse and precip-40 itate at surfaces under low normal stress. This process of mass transfer called pressure 41 solution induces compaction by creep at large scale (Durney, 1972). In the presence of 42 fluid and at temperature below 500 $^{\circ}$ C, pressure solution is thought to be the dominant 43 deformation mechanism in Earth's crust (Rutter, 1976; Gratier & Gamond, 1990). Pres-44 sure solution theory is based on the presence at grain contacts of a thin aqueous film to 45 provide the dissolved aqueous species necessary for crystal growth and transmit the nor-46 mal stress across the grain contact (Rutter, 1976, 1983). The thinner estimates of aque-47 ous film thickness ranges from 1 to 100 nm (Renard et al., 1997; Dysthe et al., 2002; De-48 sarnaud et al., 2016). 49

The existing models of pressure solution consider three steps: dissolution at grain-50 to-grain contacts (source), diffusive transport in the thin aqueous film and precipitation 51 in the pore space (sink) (Rutter, 1976; de Meer & Spiers, 1999; Niemeijer et al., 2002; 52 Gundersen et al., 2002). They predict strain rate as a function of stress, dissolution and 53 precipitation rates, diffusivity and geometrical parameters. Three main diffusive path-54 way geometries are used (den Brok, 1998): a thin fluid film model with equally spaced 55 grain boundaries, an island model with fluid-filled channels surrounding grains in con-56 tact (Raj, 1982), and a micro-cracking model with complex fluid pathways continuously 57 transformed by stress-corrosion at grain boundaries (Gratz, 1991). These geometries play 58 a first-order role on the estimated strain rates (Xia & Platt, 2017). The pressure solu-59 tion models proved their efficiency in reproducing observations in natural samples (sed-60 imentary rocks) and in experiments (Gratier et al., 2009; Niemeijer et al., 2002). How-61 ever, they are not directly applicable to metamorphic or hydrothermal systems since they 62 consider a single phase. Observations in natural samples (A. Putnis & Austrheim, 2011) 63 and in experiments (C. Putnis et al., 2005; A. Putnis, 2009; Raufaste et al., 2011) in-64 deed indicate that reactions occur through a replacement process in which primary min-65

eral dissolution and secondary mineral precipitation are coupled at the mineral interface.
 A critical point to model dissolution-precipitation process in metamorphic rocks is thus
 to allow for precipitation at the stressed grain boundaries.

Structural features such as strain shadow, grain shape preferred orientation (GSPO) 69 and crenulation cleavage provide evidence for the occurrence of dissolution-precipitation 70 creep in metamorphic rocks. They are used to understand how deformation is accom-71 modated from the scale of a single fault or shear zone (Renard et al., 2000; Gratier et 72 al., 2011; McAleer et al., 2017) to the scale of a subduction zone (Shimizu, 1995; Wass-73 74 mann & Stöckhert, 2013b; Platt et al., 2018). The acquisition of GSPO during dissolutionprecipitation requires mass redistribution from highly to low stressed surfaces. It was 75 recognized in a variety of rocks including marble (Bestmann et al., 2004), amphibolite 76 (Imon et al., 2004; Stokes et al., 2012), serpentinite (Wassmann et al., 2011; Bial & Trep-77 mann, 2013) and micaschist (Wassmann & Stöckhert, 2013a). However, other processes 78 can lead to the acquisition of GSPO (Kretz, 1966; Means & Paterson, 1966; Willis, 1977; 79 Brady, 1983; Awad et al., 2000). The possible occurrence of all these mechanisms dur-80 ing metamorphism complicates the interpretation of GSPO in rocks and calls for a bet-81 ter understanding of the conditions required to form a GSPO during dissolution-precipitation. 82

Dissolution and precipitation under stress could play a fundamental role on the ther-83 modynamics of reactions in metamorphic environments. Wheeler (2014, 2018) proposes 84 that the reaction pathway followed during reaction by pressure solution does not allow 85 thermodynamic equilibrium in stressed environments to be defined. However, the sta-86 bility fields of the various mineralogical assemblages can still be determined and the re-87 action lines can be shifted by several hundreds of MPa under stress. These results are 88 debated in the metamorphic community (Fletcher, 2015; Hobbs & Ord, 2016; Moulas 89 et al., 2019) and developing a quantitative model able to reproduce the reaction path-90 way proposed in Wheeler (2014) would help determining the effect of stress on thermo-91 dynamic equilibrium. 92

Here we develop a model for reaction under stress by considering both reaction ki-93 netics and dissolved aqueous species transport. The model allows creep laws for pres-94 sure solution and dissolution-precipitation to be determined. These laws give insights 95 into the importance of dissolution-precipitation creep for deformation in the Earth's crust. 96 We also use the model to determine the conditions favouring the acquisition of GSPO 97 during metamorphism and to constrain the pressure controlling the metamorphic reac-98 tions observed in natural systems. The model predictions are compared to observations 99 in metasediments from the Nufenen Pass (Swiss Alps). 100

¹⁰¹ 2 Modelling replacement under stress

2.1 Theoretical framework

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Fluid promotes metamorphic reactions such as the quartz-coesite transition, the albite = jadeite + quartz geobarometer or the eclogitisation of the lower crust. We develop in the following a model to estimate the first-order effect of stress on such reactions. Parameters used in the model are listed in Table 1.

Let us consider a stressed porous rock matrix reacting at constant temperature un-107 der the simplified geometry of Figure 1. The elementary unit of the model is a cubic vol-108 ume initially composed of the reactant mineralogical assemblage engulfed in a porous 109 network. We study the deformation of this elementary unit during mass redistribution 110 and volume change associated with a replacement reaction under stress. The geometry 111 used here allows for calculations at small porosity and simple upscaling with a face-centered 112 cuboid packing. It differs from the face-centered cubic packing of equally sized spher-113 ical grains generally used in pressure solution studies (Yasuhara, 2003). This latter can-114 not be used below a critical porosity of 3.49% corresponding to the porosity of the densely 115



Figure 1. Geometry of the reaction under stress model. A: considered elementary unit. The reacting grain (light grey) is replaced on its stressed surfaces by reaction products (dark grey). The reactants and the products are separated on each face by an aqueous film in which dissolved aqueous species are transported by diffusion (the aqueous films are displayed in blue). Exchanges of dissolved aqueous species between the grain surfaces occur through the porous network occupying the edges and the corners of the cuboid. B: grain packing (left) and associated pore network (right) for an assemblage of 8 cuboids.

packed spheres when the faces of adjacent spheres touch. The fluid in this rock occupies 116 both the pores and the thin films at grain boundaries perpendicular to three stress com-117 ponents (σ_{α} such that $\alpha = 1, 2$ or 3) respecting the following inequality: $\sigma_1 > \sigma_2 > \sigma_2$ 118 σ_3 . The reference frame is defined by the stress components with coordinate axis vec-119 tors, $\vec{x_{\alpha}}$, parallel to each stress component having the same subscript. The fluid pres-120 sure is equal to a constant in the pores $(P_{f,0})$. In the aqueous film, thermodynamic cal-121 culations are performed by using the fluid pressure (Dahlen, 1992) which is equal to the 122 normal stress σ_{α} (Israelachvili, 1992). This implies that we use a thin film grain bound-123 ary model. For simplicity, the fluid pressure in each film is denoted in the following with 124 the stress it is equal to (σ_{α}) . 125

We decompose the replacement reaction in the dissolution and then the precipi-126 tation of two different mineralogical assemblages: the initially rock-forming mineral(s) 127 (denoted with subscript r in the following) and the reaction product(s) (denoted with 128 subscript p). At $P_{f,0}$, the initially rock-forming minerals are more soluble than the re-129 placing minerals and they will thus dissolve whereas the replacing mineral will precip-130 itate. The aqueous film is considered to be located in between the reacting and produced 131 mineralogical assemblages (Figure 1). The chemical compositions of the reacting and pro-132 duced mineral assemblages are identical in the model. (De-)volatilization reactions are 133 thus not taken into account here. The involved dissolved aqueous species are identical 134 for the reacting and precipitating phases. We also assume equal transport properties for 135 all the mineral assemblage components in the fluid. This is in line at first-order with the 136 calculations of Oelkers and Helgeson (1988) showing diffusivity of the same order of mag-137 nitude for ions in bulk fluid. However, this does not allow to distinguish single miner-138 als in each mineralogical assemblage. Such a level of complexity is considered in Wheeler 139 (1992) and Ford and Wheeler (2004) with more complex geometries involving several grains 140 but it cannot be modelled quantitatively due to the high uncertainty on diffusion coef-141 ficients. In summary, the aim here is to provide first-order quantitative estimates for re-142 placement under stress by focusing on mass redistribution in one single cuboid of our 143 model. This requires assuming constant chemical composition in the cuboid, the same 144

chemical composition for reactants and products, and the same diffusion coefficients for
 all the dissolved aqueous species.

For each mineralogical assemblage, the rate of dissolution/precipitation (in $mol.s^{-1}$) is modelled under stress σ_{α} with the kinetic law of Lasaga (2014):

$$\dot{\xi}_{\{r,p\},\alpha} = k_{\{r,p\}} S_{\{r,p\},\alpha} \left(1 - \exp \frac{-A_{\{r,p\},\alpha}}{RT} \right) = k_{\{r,p\}} S_{\{r,p\},\alpha} \left(1 - \frac{a_{\alpha}}{a_{e,\{r,p\},\alpha}} \right) \\
= k_{\{r,p\}} S_{\{r,p\},\alpha} \left(1 - \frac{c_{\alpha}}{c_{e,\{r,p\},\alpha}} \right)$$
(1)

where $k_{\{r,p\}}$ is a kinetic constant (with unit of $mol.m^{-2}.s^{-1}$), $S_{\{r,p\},\alpha}$ is the ge-149 ometrical reactive surface area of the considered mineralogical assemblage in the aque-150 ous film normal to σ_{α} , R is the gas constant and T is the temperature. $A_{\{r,p\},\alpha}$ is the 151 chemical affinity of reaction of dissolution or precipitation under stress σ_{α} . It is defined 152 at the fluid/solid interface as the difference of the chemical potentials of the minerals un-153 der their solid state $(\mu_{s,\{r,p\},\alpha})$ and of the minerals dissolved in the fluid as aqueous species 154 $(\mu_{f,\alpha})$: $A_{\{r,p\},\alpha} = \mu_{s,\{r,p\},\alpha} - \mu_{f,\alpha}$. $A_{\{r,p\},\alpha}$ is first expressed as a function of the activity of the minerals dissolved as aqueous species in the fluid (a_{α}) and of their activ-155 156 ity in the fluid at the equilibrium $(a_{e,\{r,p\},\alpha})$. Then activities are replaced by the con-157 centration of the dissolved minerals (c_{α}) by assuming that the activity coefficients do not 158 depend on concentration. $c_{e,\{r,p\},\alpha}$ is the concentration of the dissolving or precipitat-159 ing phases at the equilibrium under stress σ_{α} . The composition of the dissolved miner-160 als formed by dissolution or consumed during precipitation are identical. There is thus 161 no need to distinguish the activity (or concentration) of the dissolved minerals between 162 reactants and products, and a_{α} and c_{α} are not mineral-specific. 163

Dissolved aqueous species migrate in the thin aqueous film as a result of chemical 164 potential gradients between the aqueous film and the pores. The transport of dissolved 165 aqueous species in the planar thin film normal to $\vec{x_{\alpha}}$ is modelled by diffusion. The re-166 lease and consumption of aqueous species by dissolution or precipitation, respectively, 167 are modelled with two source terms for dissolution and precipitation occurring at the min-168 erals/fluid interfaces. These terms are obtained by dividing the reaction rate of equa-169 tion 1 by the volume of the thin aqueous film. We assume here that the reactive surface 170 area of the dissolving and precipitating phases in each fluid film are identical $(S_{r,\alpha} =$ 171 $S_{p,\alpha}$ and that the aqueous film thickness (w) is constant so the thin film volume is $S_{p,\alpha}w$. 172 The equation describing the diffusion of dissolved aqueous species and their release/consumption 173 by reaction is finally: 174

$$\frac{\partial c_{\alpha}}{\partial t} = D\left(\frac{\partial^2 c_{\alpha}}{\partial x_{\beta}^2} + \frac{\partial^2 c_{\alpha}}{\partial x_{\gamma}^2}\right) + \frac{k_r}{w}\left(1 - \frac{c_{\alpha}}{c_{e,r,\alpha}}\right) + \frac{k_p}{w}\left(1 - \frac{c_{\alpha}}{c_{e,p,\alpha}}\right) \tag{2}$$

where D is the diffusion coefficient of dissolved aqueous species in the aqueous film, $\beta \neq \gamma \neq \alpha = 1, 2 \text{ or } 3$, and the subscript α refers to the normal stress σ_{α} at which the concentrations are calculated.

To solve the differential equation 2, we use as boundary conditions the concentration of dissolved mineral in the pore (c_0) . Diffusion in the pore proceeds rapidly compared to diffusion at grain boundaries (Brady, 1983). Therefore, we assume no spatial variations of c_0 . In the following, c_0 is either fixed by assuming a connection with an infinite source of dissolved aqueous species or calculated by assuming closed system conditions:

$$\frac{\partial c_0}{\partial t} = -\frac{4Dw}{V_0} \sum_{\alpha=1,2,3; \beta \neq \alpha; \gamma \neq \alpha, \beta} \left(L_\beta \left. \frac{\partial c_\alpha}{\partial x_\alpha} \right|_{b\beta} + L_\gamma \left. \frac{\partial c_\alpha}{\partial x_\alpha} \right|_{b\gamma} \right) \\
+ \frac{k_r S_{0,r}}{V_0} \left(1 - \frac{c_0}{c_{e,r,0}} \right) + \frac{k_p S_{0,p}}{V_0} \left(1 - \frac{c_0}{c_{e,p,0}} \right)$$
(3)

where L is the length of the thin film, and the subscript 0 refers to the fluid pres-184 sure $P_{f,0}$ at which the concentrations are calculated. In the geometry used here, each 185 pore is shared between 8 elementary units (Figure 1) and each cuboid summit contains 186 a eight part of a pore. V_0 is therefore the volume of one pore, and $S_{0,r}$ and $S_{0,p}$ are the 187 reactive surface area in this pore of the reactants and the products, respectively. The 188 two last terms on the right hand side correspond to precipitation/dissolution in the pore. 189 The first term is the Fickian flux of matter from the thin films to the pores at bound-190 aries $b\alpha$, $b\beta$ and $b\gamma$ parallel to $\vec{x_{\alpha}}$, $\vec{x_{\beta}}$ and $\vec{x_{\gamma}}$, respectively. 191

¹⁹² 2.2 Analytical solution in one dimension

It is instructive to study an analytical solution of equations (2) and (3). The geometry is simplified to recover a solution at steady state in one dimension. The aqueous films are connected to pores in x = 0 and x = L with x the distance along the aqueous film, so that $c_{\alpha}(x = 0) = c_{\alpha}(x = L) = c_0$. The composition in the films only varies in one direction (infinitely long sheet-like films in the other direction). The solution of equation 2 at steady state in one dimension is:

$$c_{\alpha}(x) = c_{b,\alpha} + (c_0 - c_{b,\alpha}) \frac{\exp\left(Da_{\alpha}\frac{x}{L}\right) + \exp\left(Da_{\alpha}\left(1 - \frac{x}{L}\right)\right)}{1 + \exp\left(Da_{\alpha}\right)} \tag{4}$$

where $c_{b,\alpha} = \frac{k_r + k_p}{\frac{k_r}{c_{e,r,\alpha}} + \frac{k_p}{c_{e,p,\alpha}}}$ is the concentration at steady state in the plane normal to $\vec{x_{\alpha}}$ when diffusion is fast compared to reaction (i.e. the amount of dissolving min-

mal to $\vec{x_{\alpha}}$ when diffusion is fast compared to reaction (i.e. the amount of dissolving minerals is exactly balanced by the amount of precipitating minerals). Da_{α} is the Damköhler number defined here as:

$$Da_{\alpha} = \sqrt{\frac{\left(\frac{k_r}{c_{e,r,\alpha}} + \frac{k_p}{c_{e,p,\alpha}}\right)L^2}{Dw}} \tag{5}$$

 Da_{α} compares the timescales of the processes involved in the system, that is reaction and diffusion. It depends on stress as the reaction rates are stress dependent. At high Da_{α} , diffusion is slower than reaction and the system is thus controlled by diffusion. Conversely, the system is controlled by reaction at low Da_{α} .

Equation 4 reveals that dissolution and precipitation reactions release and consume dissolved aqueous species in order to reach a concentration of $c_{b,\alpha}$ in the aqueous film at which input by dissolution and output by precipitation are exactly balanced. However, this concentration is never reached due to diffusion from or towards the pores in x = 0 and x = L. The direction of diffusive transport depends on the relative values of c_0 and $c_{b,\alpha}$.

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The flux of concentration at boundary x = 0 can be derived from equation 4:

$$\left. \frac{\partial c_{\alpha}}{\partial x} \right|_{x=0} = \left(c_0 - c_{b,\alpha} \right) \frac{Da_{\alpha}}{L} \frac{1 - \exp\left(Da_{\alpha}\right)}{1 + \exp\left(Da_{\alpha}\right)} \tag{6}$$

It is the opposite at boundary x = L. This flux can then be introduced into the equivalent of equation 3 in one dimension under the assumptions of steady state to obtain an expression of c_0 :

$$c_0 = \frac{-8\sum_{\alpha} \left(c_{b,\alpha} Da_{\alpha} \frac{1 - \exp Da_{\alpha}}{1 + \exp Da_{\alpha}} \right) + c_{b,0} Da_0^2}{-8\sum_{\alpha} \left(Da_{\alpha} \frac{1 - \exp Da_{\alpha}}{1 + \exp Da_{\alpha}} \right) + Da_0^2}$$
(7)

where
$$Da_0 = \sqrt{\frac{\left(\frac{k_r}{c_{e,r,0}} + \frac{k_p}{c_{e,p,0}}\right)S_0}{Dw}}$$
 under the assumption that $S_0 = S_{0,r} = S_{0,p}$.

It is apparent from equations (4) and (7) that the concentrations are controlled by the Damköhler number, that is by the slowest process between diffusion and surface-controlled kinetics in the pores and in the thin aqueous films. Table 2 gives the borderline cases for c_{α} and c_0 . The variations of Da_0 compared to Da_{α} are mainly due to differences between the reactive surface area of the pores and the grain boundary, respectively.

223 **2.3 Expression of strain rate**

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Strain rate $(\dot{\epsilon}_{\alpha})$ allows the various deformation mechanisms in the Earth to be com-224 pared. As it is usually done in pressure solution studies, we derive in the following strain 225 rates for dissolution-precipitation creep when the system is controlled by diffusion $(\epsilon_{\alpha D})$ 226 and reaction $(\dot{\epsilon}_{\alpha R})$. We also introduce strain rate for a system controlled by volume change 227 during reaction $(\epsilon_{\alpha V})$, which is specific to replacement reactions. As in most pressure 228 solution studies, strain rate is calculated here as positive when the rock compacts and 229 it is calculated with the solution for mass transfer in one dimension (Gratier et al., 2013). 230 It can be directly recovered from the reaction rates in the thin films: 231

$$\dot{\epsilon_{\alpha}} = \frac{2k_r V_r}{L} \left(1 - \frac{c_{\alpha}}{c_{e,r,\alpha}} \right) + \frac{2k_p V_p}{L} \left(1 - \frac{c_{\alpha}}{c_{e,p,\alpha}} \right) \tag{8}$$

where V_r and V_p are the molar volumes of the replaced and replacing solid phases, respectively. These volumes are involved here since a replacement reaction can induce deformation through volume change. The presence of L in the denominator is related to the distribution of volume change in the considered volume.

At high Da_{α} , equation 4 leads to $c_{\alpha} = c_{b,\alpha}$ and equation 8 can thus be re-written as:

$$\dot{\epsilon_{\alpha V}} = -2\frac{\Delta_r V}{L}k_m \tag{9}$$

where $k_m = \frac{k_r k_p \left(1 - \frac{c_e, p, \alpha}{c_e, r, \alpha}\right)}{k_r \frac{c_e, p, \alpha}{c_e, r, \alpha} + k_p}$ and $\Delta_r V = V_p - V_r$ are, respectively, the overall reaction rate constant and the solid change in volume for the replacement reaction including both dissolution and precipitation. $\epsilon_{\alpha V}$ is thus the strain rate when the system is controlled by volume change during reaction. When the reaction rate is controlled by dissolution, the reaction rate constant of the dissolving phase is smaller than the one of the precipitating phase $(k_r \ll k_p)$, and $k_m = k_r \left(1 - \frac{c_e, p, \alpha}{c_e, r, \alpha}\right)$. When the reaction rate is controlled by precipitation $(k_p \ll k_r), k_m = -k_p \left(1 - \frac{c_e, r, \alpha}{c_e, p, \alpha}\right)$. In the case of isotropic stresses, equation 9 is equivalent to a kinetically-delayed change in solid volume.

 $c_{e,\{r,p\},\alpha}$ depends on stress (Paterson, 1973) as:

$$c_{e,\{r,p\},\alpha} = c_{e,\{r,p\},0} \exp\left(\frac{(\sigma_{\alpha} - P_{f,0}) V_{\{r,p\}}}{RT}\right)$$
(10)

where $c_{e,\{r,p\},0}$ is the concentration of the dissolved or precipitating minerals at the equilibrium at $P_{f,0}$. We obtain with equations 9 and 10 for $k_r \ll k_p$:

$$\dot{\epsilon_{\alpha V}} = -2\frac{k_r \Delta_r V}{L} \left(1 - \frac{c_{e,p,0}}{c_{e,r,0}} \exp\left(\frac{(\sigma_\alpha - P_{f,0}) \Delta_r V}{RT}\right)\right)$$
(11)

and for $k_p \ll k_r$:

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$$\dot{\epsilon_{\alpha V}} = 2 \frac{k_p \Delta_r V}{L} \left(1 - \frac{c_{e,r,0}}{c_{e,p,0}} \exp\left(-\frac{(\sigma_\alpha - P_{f,0}) \Delta_r V}{RT}\right) \right)$$
(12)

We consider in the following that equilibrium is achieved at $P_{f,0}$ ($c_{e,r,\alpha} = c_{e,p,\alpha}$ when $\sigma_{\alpha} = P_{f,0}$). By definition, the dissolving assemblage has a higher solubility than the precipitating one ($c_{e,r,\alpha} > c_{e,p,\alpha}$). These two latter statements as well as equation 10 imply that $V_r < V_p$ ($\Delta_r V > 0$) if $\sigma_{\alpha} < P_{f,0}$. Conversely, $\Delta_r V$ is negative when $\sigma_{\alpha} > P_{f,0}$. As a result, the product ($\sigma_{\alpha} - P_{f,0}$) $\Delta_r V$ is always negative in far from the equilibrium conditions and equations 11 and 12 tend towards $-\frac{k_{\{r,p\}}\Delta_r V}{L}$ when assuming equilibrium in the pores $c_{e,r,0} = c_{e,p,0}$.

Equations 9, 11 and 12 are derived at high Da_{α} but they indicate that processes are not controlled by diffusion but rather by volume change during reaction. Studying the diffusion controlled case at high Da_{α} requires assuming no change in volume during reaction, that is $V_r = V_p$. In these conditions, strain rate can be derived by summing the fluxes of matter at the aqueous film/pore interface and noticing that each mole of exported matter corresponds to a displacement of $\frac{V_r}{T^2}$:

$$\dot{\epsilon_{\alpha}} = 8D \left. \frac{\partial c_{\alpha}}{\partial x} \right|_{x=0} \frac{wV_r}{L^2} \tag{13}$$

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Equation 13 can then be combined with equation 6 to obtain:

$$\dot{\epsilon_{\alpha}} = \frac{8Da_{\alpha}DwV_r}{L^3} \left(c_0 - c_{b,\alpha}\right) \frac{1 - \exp\left(Da_{\alpha}\right)}{1 + \exp\left(Da_{\alpha}\right)} \tag{14}$$

At $Da_{\alpha} > 5$, $\frac{1-\exp(Da_{\alpha})}{1+\exp(Da_{\alpha})} \sim -1$ and equation 14 can be simplified to recover the strain rate for a diffusion-controlled system:

$$\dot{\epsilon_{\alpha D}} = -\frac{8Da_{\alpha}DwV_r}{L^3} \left(c_0 - c_{b,\alpha}\right) \tag{15}$$

At low Da_{α} (control by reaction), the strain rate can be retrieved from equation 8 by substituting c_{α} with the expression of c_0 for the different borderline cases (see Table 2).

269 **2.4 Pressure solution**

Pressure solution models consider only one phase which dissolves at grain contacts. This corresponds to a model proposed here if only considering the reaction of dissolution. There is therefore no replacement reaction and the terms of the previous section with p subscript can all be dropped. Moreover, the geometry is slightly modified since the aqueous film needs to be shared between two elementary units. The strain rate of equation 14 needs thus to be divided by 2.

The strain rate expressed in equation 8 becomes:

$$\dot{\epsilon_{\alpha}} = \frac{2k_r V_r}{L} \left(1 - \frac{c_{\alpha}}{c_{e,r,\alpha}} \right) \tag{16}$$

This latter equation can be re-written with the limits given in Table 2 at low Da_{α} to express the strain rate for a system controlled by reaction:

$$\dot{\epsilon_{\alpha R}} = \frac{2k_r V_r}{L} \left(1 - \frac{c_0}{c_{e,r,\alpha}} \right) \tag{17}$$

The consideration of a one phase system also leads to $c_{b,\alpha} = c_{e,r,\alpha}$ which allows equation 14 to be re-written as:

$$\dot{\epsilon_{\alpha}} = -\frac{4k_r V_r}{L} \left(1 - \frac{c_0}{c_{e,r,\alpha}}\right) \frac{1}{Da_{\alpha}} \left(\frac{1 - \exp\left(Da_{\alpha}\right)}{1 + \exp\left(Da_{\alpha}\right)}\right) \tag{18}$$

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For a system controlled by diffusion (high Da_{α}), equation 18 becomes:

$$\dot{\epsilon_{\alpha D}} = \frac{4Da_{\alpha}c_{e,r,\alpha}DwV_r}{L^3} \left(1 - \frac{c_0}{c_{e,r,\alpha}}\right)$$
(19)

Equations 17 and 19 provide strain rates in the reaction-controlled and diffusioncontrolled cases, respectively. The only unknown is c_0 in these equations. We determine this unknown under two assumptions (small or large porosity) in the following.

Firstly, at small porosity $(Da_0 \ll Da_\alpha; \text{closed system})$, the concentration in the pores is $c_0 = \frac{\sum_\alpha c_{e,r,\alpha} Da_\alpha}{\sum_\alpha Da_\alpha}$ (Table 2). For non-hydrostatic stresses, grain surfaces normal to σ_1 will dissolve whereas phase precipitation will occur on the grain surfaces normal to σ_3 . The rate of this mass transfer at the grain scale can be quantified with equations 17 and 19.

Secondly, we can assume that pores are connected to a large sink/source of aqueous species buffering the system composition at an equilibrium value of $c_0 = c_{e,r,0}$. This is the assumption used in most pressure solution studies when open system conditions are considered. For the reaction-controlled case, combining equation 17 with equation 10 under the assumption $c_0 = c_{e,r,0}$ leads to:

$$\dot{\epsilon_{\alpha R}} = \frac{2k_r V_r}{L} \left(1 - \exp\left(\frac{-\left(\sigma_{\alpha} - P_{f,0}\right) V_r}{RT}\right) \right) \approx \frac{2k_r V_r^2 \left(\sigma_{\alpha} - P_{f,0}\right)}{RTL}$$
(20)

²⁹⁵ When the system is controlled by diffusion (high Da_{α}) under the assumption of ²⁹⁶ a large aqueous species reservoir, the strain rate is recovered from equation 19 with $c_0 =$ ²⁹⁷ $c_{e,r,0}$:

$$\dot{\epsilon_{\alpha D}} = -\frac{4Da_{\alpha}c_{e,r,0}DwV_r}{L^3} \left(1 - \exp\left(\frac{(\sigma_{\alpha} - P_{f,0})V_r}{RT}\right)\right) \approx \frac{4Da_{\alpha}c_{e,r,0}DwV_r^2\left(\sigma_{\alpha} - P_{f,0}\right)}{RTL^3}$$
(21)

298 2.5 Deformation mechanism maps

Equation 18 can be used to generate a deformation mechanism map, allowing pres-299 sure solution to be compared with other deformation mechanisms, that is dislocation and 300 diffusion creeps. The parameters needed to plot such a map are the diffusion coefficient, 301 D, the reaction rate, k_r , the aqueous film thickness, w, the grain size, L, and the con-302 centration at the equilibrium in the aqueous film, $c_{e,r,\alpha}$. Experiments of pressure solu-303 tion (van Noort et al., 2007, 2011), molecular dynamics simulations (Dysthe et al., 2002) 304 and theoretical studies (Revil, 2001) give estimates of D of $\sim 10^{-10} m^2 s^{-1}$, that is one 305 order of magnitude lower than diffusivity in bulk fluid (Oelkers & Helgeson, 1988). In 306 practice, we use in the following a diffusion coefficient depending on temperature such 307 as: 308

$$D = 1.2.10^{-9} \exp\left(-\frac{10.10^3}{RT}\right) \tag{22}$$

The dependency in temperature in this latter equation is derived from the diffu-309 sivity estimates of Oelkers and Helgeson (1988). We use an aqueous film thickness of w =310 $2.10^{-9}m$ based on the study of Dysthe et al. (2002). The grain size is fixed to L = 100311 $\mu m. c_{e,r,\alpha}$ is estimated with equation 10 including the aqueous species concentration at 312 the equilibrium at P_{f0} ($c_{e,r,0}$) calculated with Perple_X (Connolly, 2005) and the merged 313 high pressure databases of Sverjensky et al. (2014) and Holland and Powell (2011) for 314 dissolved aqueous species and solid phases, respectively. k_r is poorly constrained since 315 kinetic parameters are generally determined in a bulk fluid with experiments on pow-316 ders in batch reactors in which the reaction processes are probably strongly different than 317 in an aqueous film. The quartz indentation experiments of Gratier et al. (2009) provide 318 precise strain rate measurements at 350 °C in a NaOH-bearing fluid and at stress rang-319 ing from 25 to 350 MPa. Their experimental dataset was fitted with equation 18 to es-320 timate k_r (Figure 2 A). We obtained a value of $k_r = 3.10^{-5} mol.m^{-2}.s^{-1}$ which is four 321 orders of magnitude lower that the rate of quartz dissolution in a bulk fluid estimated 322 with the laws of Tester et al. (1994) and Worley et al. (1996) in the same conditions (k_{rbulk}) . 323 The experiments of Niemeijer et al. (2002) of quartz grain compaction can also be used 324 to compare k_r to the dissolution laws obtained with experiments on powders. They were 325 performed with stresses ranging from 50 to 150 MPa and at temperature comprised be-326 tween 400 and 600 °C. Estimating stress (and associated reaction progress) at grain con-327 tacts from the applied far-field stress in the experiments of Niemeijer et al. (2002) re-328 quires introduction of a stress concentration factor (B) (Dewers & Hajash, 1995) (see 329 details on the calculation in Appendix A). This factor decreases with porosity during 330 compaction as more grain contacts are formed (Figure 2 B). Therefore, estimates of re-331 action rate in the thin aqueous film are more indirect than with the dataset of Gratier 332 et al. (2009). They are at least one order of magnitude lower than in the bulk fluid (Fig-333 ure 2 B). 334

The fit of experimental data thus indicate k_r values below the one determined in 335 bulk fluid. Since the uncertainty on k_r is high (1 to 4 orders of magnitude below k_{rbulk}), 336 we investigated the influence of this parameter on strain rate prediction by determin-337 ing two deformation mechanism maps for quartz with either $k_r = k_{rbulk}$ or $k_r = k_{rbulk} / (10^4)$ 338 (Figure 3 C and D). The Damköhler number calculated with equation 5 and the param-339 eters given above are required to plot the deformation mechanism maps. It is displayed 340 in Figure 3 A and B for distinguishing between diffusion- and reaction-controlled pres-341 sure solution creep. The deformation mechanism maps are obtained by considering, in 342 addition to pressure solution, dislocation and diffusion creeps for which strain rates are 343 calculated with the laws given in Tokle et al. (2019) and Rutter and Brodie (2004), re-344 spectively (see Appendix B for details on these laws). 345



Figure 2. Fit of experimental data with equation 18 to determine k_r . A: Strain rate as a function of applied normal stress in the quartz indentation experiments of Gratier et al. (2009) (black dots). The black line corresponds to the best fit (k_r) $2.9.10^{-5} mol.m^{-2}.s^{-1}$). The = strain rate computed with the reaction rate determined in a bulk fluid $(k_r = k_{rbulk} = 0.43)$ $mol.m^{-2}.s^{-1}$) (Tester et al., 1994; Worley et al., 1996) is also displayed with a red line. k_r deduced from the fit of the experimental data is four of magnitude lower than k_{rbulk} . B: Strain rate as a function of the ratio between actual and initial porosities (ϕ/ϕ_0) . The data from Niemeijer et al. (2002) are displayed with dots and one colour for each experiment: blue, red, black, yellow, cyan, magenta and green for their experiments CPf3, CPf4, CPf5, CPf6, CPf7, CPf8 and CPf9, respectively. These experiments are performed at different temperature and effective pressure (see Niemeijer et al. (2002) for details). The lines correspond to the best fit of the data for which $k_r = k_{rbulk}/15$. Dashed lines correspond to the strain rates calculated with $k_r = k_{rbulk}$. The colors of the lines are identical to the color used for the experimental results (dots) when the stress and the temperature used for the computation are identical to those used in the experiments.

The distribution of the dominant deformation mechanisms is similar for the two 346 reaction rates used for calculating the deformation mechanism maps (Figure 3). Diffu-347 sion creep is not a dominant deformation mechanism in the investigated stress-temperature 348 domain. Dislocation creeps dominates at stress above $\sim 10^8 Pa$ and temperature above 349 $\sim 650^{\circ}C$ whereas pressure solution creep dominates elsewhere. The pressure solution creep 350 domain extends as the reaction rate increases. The strain rate calculated for pressure 351 solution are two orders of magnitude higher when calculated with $k_r = k_{rbulk}$ than with 352 $k_r = k_{rbulk}/(10^4)$, in agreement with equation 18. Pressure solution creep is controlled 353 by reaction at low temperature whereas it is controlled by diffusion at high temperature. 354 The temperature of transition from reaction- to diffusion-controlled pressure solution creep 355 is ~ 70°C and ~ 350°C for $k_r = k_{rbulk}$ and $k_r = k_{rbulk}/(10^4)$, respectively. 356

The pressure solution model proposed above assumes no precipitation in the aque-357 ous film. This does not allow dissolution-precipitation creep in small porosity rocks to 358 be modelled as it is commonly observed in hydrothermal and metamorphic systems. We 359 use in the following the equations of section 2.2 to extend our understanding of polymin-360 eralic assemblages by calculating first-order estimates of strain rate for dissolution-precipitation 361 creep. Such estimates allow to compute deformation mechanism maps including dissolution-362 precipitation creep (Figure 4). We consider as an example the metamorphic reaction of 363 muscovite + quartz $\langle = \rangle$ and a lusite + sanidine + H₂O. We assume isotropic stress and 364 small porosity $(Da_0 \rightarrow 0)$ so that equation 9 can be used to calculate strain rate at both 365 high and low Da_{α} . This strain rate corresponds to the strain rate associated with vol-366 ume change during reaction $(\epsilon_{\alpha V})$. The muscovite dehydration involves water exchange 367 between the solid and the fluid phases which is not considered in our model. However, 368 it is one of the few metamorphic reactions for which reaction rates estimates are avail-369 able as a function of pressure and temperature (Schramke et al., 1987). The use of this 370 reaction as a general kinetic model for metamorphic reactions is justified by the fact that 371 the kinetic data for many metamorphic reactions (including or not volatile species) can 372 be rather accurately fitted with a single rate law (Wood & Walther, 1983). Calculations 373 are performed by considering that and alusite + sanidine + H₂O react to produce mus-374 covite + quartz at temperatures lower than the equilibrium whereas the opposite reac-375 tion occurs at higher temperature. Equilibrium is thus never achieved in Figure 4 ex-376 cept on the reaction line and reaction rates progressively increase away from this line in 377 agreement with equation 1. This diagram is therefore only valid if disequilibrium con-378 ditions are achieved through changes in composition (e.g. fluid input) or in pressure and/or 379 temperature. We fitted the data of Schramke et al. (1987) with a kinetic law as follows: $k = k_{rbulk} \left(1 - \exp\left(\frac{-A_{t,\alpha,\beta}}{RT}\right)\right)^n$ where $k_{rbulk} = \lambda \exp\left(\frac{-Ea}{RT}\right)$ and $A_{t,\alpha,\beta}$ is the distance from the equilibrium defined as the difference between the chemical potential of the dis-380 381 382 solving minerals $(\mu_{s,p,\alpha})$ and the chemical potential of precipitating minerals $(\mu_{s,p,\beta})$: $A_{t,\alpha,\beta} =$ 383 $\mu_{s,r,\alpha} - \mu_{s,p,\beta}$. Two different fits are produced for hydration and dehydration. k_r and 384 k_p are assumed equal. There are no experimental data for dissolution-precipitation creep 385 which can be used to determine the relationship between k_r and k_{rbulk} as we did for pres-386 sure solution. We therefore used the same approach as for pressure solution and plot-387 ted deformation mechanism map with $k_r = k_{rbulk}$ and $k_r = k_{rbulk}/(10^4)$ (Figure 4). 388 The concentrations at the equilibrium $(c_{e,r,\alpha} \text{ and } c_{e,p,\alpha})$ are calculated with Perple_X 389 (Connolly, 2005) from the equilibrium constants of muscovite + quartz or andalusite + 390 sanidine + H₂O dissolution reactions written with $SiO_{2,aq}$, AlO_2^- , K^+ and H^+ as dis-solved aqueous species. The molar volumes are $162.68.10^{-6} m^3.mol^{-1}$ and $160.38.10^{-6}$ 391 392 $m^3 mol^{-1}$ for the assemblages muscovite + quartz and and a lusite + sanidine, respec-393 tively. The Damköhler number calculated with the above parameters for dissolution-precipitation creep is displayed in Figure 4 A and B. It is high in the investigated stress-temperature 395 domain except near the reaction line, where replacement is limited by the reaction rate 396 rather than by diffusion. 397

³⁹⁸ Dissolution-precipitation creep is the dominant deformation mechanism in most of ³⁹⁹ the investigated stress-temperature domain even for a low reaction rate $(k_r = k_{rbulk}/(10^4);$



Figure 3. Damköhler number and deformation mechanism maps for quartz as a function of stress and temperature. The calculations are performed with an aqueous film thickness of $2.10^{-9}m$, a grain size of $L = 100\mu m$, a diffusion coefficient given in equation 22, and a = wsolubility calculated with equation 10. Two different reaction rates are used: $k_r = k_{rbulk}$ (A and C) and k_r $k_{rbulk}/(10^4)$ (B and D). A and B: calculated Damköhler number. The contours = correspond to $log_{10}(Da_{\alpha})$. C and D: deformation mechanism maps. The contours correspond to $log_{10}(\dot{\epsilon})$. The domains where one of the four studied deformation mechanism (reaction- and diffusion-controlled pressure solution creep, dislocation creep and diffusion creep) dominates are displayed. The strain rates for dislocation and diffusion creeps are calculated with the equations given in Tokle et al. (2019) and Rutter and Brodie (2004), respectively. The strain rate for pressure solution creep is calculated with equation 18. Reaction- and diffusion-controlled domains correspond to $Da_{\alpha} < 1$ and $Da_{\alpha} > 1$, respectively.

Figure 4 D). The strain rate calculated for dissolution-precipitation creep are four orders of magnitude higher for $k_r = k_{rbulk}$ than for $k_r = k_{rbulk}/(10^4)$, in agreement with equation 9. The calculations do not predict diffusion creep to be a dominant deformation mechanism. The main difference with pressure solution (Figure 3) is observed near thermodynamic equilibrium (i.e. near the reaction line) where dislocation creep can dominate due to the low reaction rate calculated in this region.

⁴⁰⁶ 3 Numerical modelling of replacement under stress

The analytical solutions of the previous sections provide information at first-order 407 on the importance of dissolution-precipitation under stress for deformation. However, 408 they are difficult to directly connect to observations in metamorphic rocks. We develop 409 in the following a numerical model to predict the evolution of grain shape and overall 410 reaction progress during dissolution-precipitation under stress. The numerical model solves 411 equation 2 for the evolution of concentration in three aqueous fluid films of different ori-412 entations (normal to σ_1 , σ_2 and σ_3 ; Figure 5 A, B and C). We use the finite difference 413 method with an explicit scheme. The concentration in the pores is computed with equa-414 tion 3, providing an equation for the boundary conditions. At each time step, we extract 415 the volume of dissolved and precipitated minerals from the evolution of dissolved species 416 concentration. This allows the evolution of grain shape with time to be calculated (Fig-417 ure 5 D, E and F). The model geometry does not allow different rates in the same aque-418 ous film to be considered. The rates are thus averaged in each film to determine the to-419 tal volume of dissolving and precipitating minerals. These volumes are then converted 420 into changes in the length of the grain sides by solving for mass conservation with the 421 geometry provided in Figure 1. The simulations conserve mass within less than 1% af-422 ter total grain conversion. We use $D = 1.7.10^{-10}m^2 . s^{-1}$, $V_r = 140.10^{-6}m^3 . mol^{-1}$, $V_p = 180.10^{-6}m^3 . mol^{-1}$, $L = 100.10^{-6}m$, $w = 2.10^{-9}m$, $c_{e,r,0} = 0.195 mol . m^{-3}$, $c_{e,p,0} = 0.150 mol . m^{-3}$, $\sigma_1 = 150 MPa$, $\sigma_2 = 100 MPa$ and $\sigma_3 = 50 MPa$. The reac-423 424 425 tion rates $(k_r \text{ and } k_p)$ are equal and varied in-between simulations to investigate differ-426 ent Da_{α} . 427

We first validate the model by reproducing the analytical results presented above. 428 At low Da_{α} (~ 0.12), the model predicts a constant concentration in the whole system 429 (aqueous films and pores; $c_{\alpha} = c_0$) which can be approximately calculated with the equa-430 tion for concentration in the pores derived in one dimension (Table 2; Figure S1 A). The 431 strain rates derived analytically in one dimension at low Da_{α} are also reproduced with 432 a good precision (Equation 8; Figure S1 C). At high Da_{α} (~ 380), the calculated con-433 centration and strain rates are also approximately equal to the analytical solutions (Ta-434 ble 2 and Equation 9; Figure S1 B and D). 435

436

3.1 Grain shape preferred orientation

To better understand the acquisition of GSPO during replacement under stress, we numerically investigate the influence of Da_{α} on GSPO by running several simulations with different reaction rates. GSPO is quantified with the aspect ratio calculated after complete replacement and defined as the length of the grain side normal to σ_3 over the length of the grain side normal to $\sigma_1 \left(\frac{L_{tot3}}{L_{tot1}}\right)$. At $Da_{\alpha} > 100$, the aspect ratio is close to 1 and there is no change in shape during reaction (Figure 6). A strong change in GSPO occurs at $Da_{\alpha} < 10$ with an aspect ratio reaching 3.3 at $Da_{\alpha} = 0.282$ (Figure 6).

444

3.2 Pressure controlling the replacement process

⁴⁴⁵ The reaction rate depends on the distance from the equilibrium $(A_{t,\alpha,\beta};$ equation ⁴⁴⁶ 1). As the chemical potential depends on pressure, the reaction rates in two differently ⁴⁴⁷ oriented grain surfaces under different normal stresses are different. Reaction in one of



Figure 4. Damköhler number and deformation mechanism map for a system in which the replacement reaction of muscovite + quartz $\langle = \rangle$ and a lusite + sanidine + H₂O occurs. The = $2.10^{-9}m$, a grain size of calculations are performed with an aqueous film thickness of w $L = 100 \mu m$, a diffusion coefficient given in equation 22, and a solubility calculated with equation 10. Two different reaction rates are used: $k_r = k_{rbulk}$ (A and C) and $k_r = k_{rbulk}/(10^4)$ (B and D). A and B: calculated Damköhler number. The contours correspond to log_{10} (Da_{α}). C and D: deformation mechanism map. The strain rates for dislocation and diffusion creeps are calculated with the equations given in Tokle et al. (2019) and Rutter and Brodie (2004), respectively. The strain rate for dissolution-precipitation creep is calculated with equation 9, which is relevant for high Da_{α} and does not depend on differential stress (control by volume change during reaction). The reaction line where equilibrium is reached is shown in red and separates two fields in which we consider either hydration (left) or dehydration (right). The contours correspond to $log_{10}(\dot{\epsilon})$. The domains where one of the three studied deformation mechanism (dissolution-precipitation, dislocation and diffusion creeps) dominates are displayed. The yellow and orange areas correspond to the regions where prograde metamorphism and hydrothermal conditions are expected to occur, respectively.



Figure 5. Numerical modelling of replacement reaction under stress for $k_r = k_p = 1.10^{-10} mol.m^{-2}.s^{-1}$. A: concentration in the aqueous film normal to σ_1 at a reaction progress of $\xi = 10\%$. B: concentration in the aqueous film normal to σ_2 at $\xi = 10\%$. C: concentration in the aqueous film normal to σ_3 at $\xi = 10\%$. D: grain shape at $\xi = 10\%$ deduced from reaction rate calculated with the numerical model for concentration in the thin fluid film. The initially rock-forming mineral is displayed in yellow and the reaction products are displayed in green. The orientation of the stress components are indicated. E: grain shape at $\xi = 40\%$. F: grain shape at $\xi = 90\%$.



Figure 6. Aspect ratio after complete replacement as a function of the logarithm of Da_{α} . The aspect ratio is defined as the length of the grain side normal to σ_3 over the length of the grain side normal to $\sigma_1 \left(\frac{L_{tot,3}}{L_{tot,1}}\right)$. Each dot corresponds to one simulation. The differential stress $(\sigma_1 - \sigma_3)$ is of 100 MPa $(\frac{L_{tot,3}}{L_{tot,1}})$ would be equal to 1 if the grain would grow under isotropic stress).



Figure 7. Proportion of the overall reaction progress on each group of mineral faces with the same orientation as a function of the distance from the equilibrium. The faces normal to σ_1 , σ_2 and σ_3 are displayed with black, red and blue dots, respectively. We modify the distance from the equilibrium by increasing the difference between σ_3 and the equilibrium pressure (P_{eq}) . The simulations are performed at high Da with $k_r = k_p = 1.10^{-6} mol.m^{-2}.s^{-1}$ and fixed differential stresses $\sigma_2 - \sigma_3$ and $\sigma_1 - \sigma_3$ of 50 and 100 MPa, respectively.

the thin aqueous film can thus dominate the replacement process, leading to a control of the reaction by the stress normal to this film.

To quantitatively investigate this process, we run simulations to determine the contribution of each face of the cuboid to the overall reaction progress as a function of the distance from the equilibrium (Figure 7). The distance from the equilibrium increases with pressure in the simulations $(A_{t,1,1} > A_{t,2,2} > A_{t,3,3})$. This is equivalent to consider that the reaction involves a negative change in volume ($\Delta_r V = V_p - V_r < 0$; left side of the reaction line for a reaction with a positive Clapeyron slope or right side for a reaction with a negative Clapeyron slope). We run several simulations with an increasing difference between σ_3 and the equilibrium pressure (P_{eq}) while the differential stresses, $\sigma_2 - \sigma_3$ and $\sigma_1 - \sigma_3$, are fixed to 50 and 100 MPa, respectively.

At low Da_{α} , diffusion proceeds more rapidly than reaction and mass is redistributed between the aqueous films with precipitation which can occur in a different aqueous film than dissolution. The simulations are thus run at $Da_{\alpha} > 1$ to be able to isolate the contribution of each face to reaction. Most of grain conversion occurs on the face normal to σ_1 near the equilibrium (Figure 7). The pressure controlling reaction is thus σ_1 . For reactions with $\Delta_r V > 0$, the pressure controlling reaction is σ_3 . Far from the equilibrium, reaction is equally distributed among the faces (Figure 7) and the thermodynamic pressure is thus the mean stress.

467 4 Grain shape preferred orientation in natural samples from the Nufe-468 nen pass area

Here we present an application of the model developed above to evaluate GSPO 469 data from a regional metamorphic terrain. The Mesozoic sedimentary cover of the Got-470 thard massif is well exposed in the Nufenen pass area (Swiss Central Alps). We collected 471 along the road of the Griessee intensively foliated graphite-rich schists. We focused on 472 two different types: one has garnet porphyroblasts (0.6 to 8 mm in diameter), the other 473 one has plagioclase porphyroblasts (1 to 10 mm diameter). The peak metamorphic con-474 ditions were estimated by Klaper and Bucher-Nurminen (1987) and Kamber (1993) at 475 450-500 °C and 0.5 GPa. In addition to plagioclase and garnet, the rock contains quartz, 476 carbonates, muscovite, biotite, clinozoisite, ilmenite and carbonaceous matter. Garnet 477 and plagioclase are often slightly oval, and visual investigation of the direction of the long 478 axis of the porphyroblasts show that they are not aligned in the pronounced schistos-479 ity visible in the field (Figure 8). The schistosity is defined by mica. The stratigraphy, 480 deformation and metamorphism were studied in detail for this area by Liskay-Nagy (1965); 481 Leu (1985); Klaper and Bucher-Nurminen (1987); Kamber (1993). A detailed review of 482 the different nomenclature and tectonic interpretations made by these authors is beyond 483 interest of this study. Nevertheless, we agree with the observations of these authors, that 484 in the profile studied here the peak metamorphic minerals plagioclase and garnet grew 485 after the second folding phase (D2, following the nomenclature of Liskay-Nagy (1965)), 486 which was responsible for the major schistosity in the area. The final deformation phase 487 (D3) did in places result in a rotation of the blasts, visible in a rotation of the schistos-488 ity. This was not observed in the samples presented here. 489

The 3D orientation of the porphyroblasts is determined in seven plagioclase-bearing 490 and six garnet-bearing samples by X-ray microtomography (μ cT) with a Skyscan 1172 491 device at the University of Lausanne. Different settings are used for the two types of schists 492 since garnet and plagioclase have higher and comparable X-ray attenuation than the rock 493 matrix, respectively. Garnet-bearing samples were analysed at 130 kV and 60 μ A with 494 a resolution comprised between 20 and 25 μm and a brass filter. Plagioclase-bearing sam-495 ples are analysed at 70 kV and 114 μ A with a resolution comprised between 11 and 16 496 μm and an aluminium filter. 3D images are generated from transmission images with 497 the NRecon software. They are then segmented with blob3D (Ketcham, 2005) by con-498 sidering three phases: the porphyroblast, ilmenite and the matrix. We fit an ellipsoid 499 to each segmented grain to determine the grain aspect ratio (length of the longest axis 500 over length of the shortest axis), the orientations of the main elongation axis and of the 501 main shortening plane. Spherical orientation data are projected in 2D and statistically 502 analysed using Bingham axial distribution with the Stereonet software (Cardozo & All-503 mendinger, 2013). Porphyroblasts at the edge of the core and/or coalescing with other 504 grains were excluded from the analysis. Ilmenite grains are elongated in the foliation; 505



Figure 8. Field pictures of the schists samples at the Nufenen pass. (A) and (B) Garnetporphyroblast (Grt) bearing micaschist. Garnets are more reflective than the surrounding matrix. (C) Plagioclase-porphyroblast (Pl) bearing schist. Plagioclases are mainly form at the lithological contacts. The main elongation axis is displayed with white dashed lines for some porphyroblasts.



Figure 9. Plagioclase and garnet porphyroblasts orientation for the Nufenen pass area on an equal area lower hemisphere projection. The schistosity measured in the field is in green, the foliation measured with ilmenite orientation in black and the mean porphyroblast shortening plane in red. When the sedimentary layering (S0) is different from the schistosity, it is displayed in blue (samples LB_2018_1, LB_2018_2, LB_2018_3 and LB_2018_3.2). The white dots are the principal elongation axes of the porphyroblasts. The dot density is contoured. Sample LB_2018_10 was not collected in place and orientations are thus given relative to an arbitrary plane chosen as the planar bottom of the core.

their main shortening plane thus gives foliation orientation. The results of statistical analysis are given in Figure 9 and Table 3.

We determine the orientation and the aspect ratio of 13 to 42 plagioclases in 7 dif-508 ferent cores and 40 to 96 garnets in 6 different cores (Table 3). Ilmenite crystals outline 509 the orientation of the foliation. This orientation is similar to the schistosity measured 510 in the field for garnet-bearing samples whereas plagioclase-bearing samples collected near 511 a fold hinge display different schistosity and foliation orientations (Table 3 and Figure 512 9). Garnets have an ellipsoidal shape whereas plagioclases are only elongated in one di-513 rection (Figure 10). The mean aspect ratios are 2.3 ± 0.5 and 1.8 ± 0.5 for plagoclase 514 and garnet, respectively (Figure S2). Their elongation axis is oblique to the sedimen-515 tary layering (S0) (Figure 9). Plagioclases appear as elongated in the foliation even though 516 the dispersion of the data does not provide a precise estimate of their orientation. Gar-517 nets are flattened along a plane oblique to the schistosity/foliation at an angle between 518 15 and 39 ° (Table 3 and Figure 9), confirming the field observations. Garnets contain 519 numerous inclusions of quartz, epidote and ilmenite. These inclusions do not appear to 520 be preferentially elongated (Figure S2). In each core except plagioclase-bearing sample 521 LB_2018_4 , the orientations of the elongation or of the flattening of the porphyroblasts 522 are similar, indicating a GSPO at the centimetre scale (Table 3). Plagioclase orienta-523 tion data are more scattered than garnet orientation data at this scale but also at the 524 outcrop scale (Figure 9). Garnet-bearing cores have indeed similar GSPO with a main 525 shortening axis ranging from 158/88 to 169/73 (Azimuth/Dip). The orientation of the 526 main shortening axis of plagioclase varies between 5/62 and 325/80, indicating a vari-527 ation of the GSPO at the tens of centimetre to the metre scale. These results are in agree-528 ment with the observations made in the field, showing that the foliation and the main 529 orientation of plagioclase progressively rotate over a distance of several tens of centime-530 tres (Figure 8 C). There is no relationship between the main orientation of plagioclases 531 and their aspect ratio. 532



Figure 10. 3D images of segmented cores. A: plagioclase-bearing sample (LB_2018_3_2). B: garnet-bearing sample (LB_2018_6). Garnet, plagioclase and ilmenite are displayed in yellow, green and blue, respectively. The ilmenite crystals serve to determine the orientation of the foliation.

533 5 Discussion

The model proposed here implements two processes which were not considered in 534 the previous models of pressure solution: the possibility for mineral precipitation in the 535 thin aqueous films, that is at grain boundary, and a reaction rate depending on the dis-536 tance from the equilibrium. These two features lead to new laws for pressure solution 537 and dissolution-precipitation creeps. Moreover, they allow to predict the acquisition of 538 GSPO and to discuss the pressure controlling metamorphic reactions. We discuss in the 539 following the changes brought by these new laws for modelling reaction-driven deforma-540 tion in the Earth's crust. 541

542

5.1 Comparison with previous creep laws for pressure solution

Equation 18 is a general creep law for pressure solution. It is obtained by solving 543 for mass transfer in a thin aqueous film in one dimension, like in previous studies on pres-544 sure solution (Rutter, 1976; Niemeijer et al., 2002; X. Zhang et al., 2010). The grain size 545 (L) does not evolve during reaction with this approach. Equation 18 is thus only valid 546 if incremental deformation is assumed. Estimating the error associated with this assump-547 tion requires to solve for grain shape evolution during dissolution-precipitation. This is 548 done with the numerical model where the strain rate is shown to decrease with time (Fig-549 ure S1). This decrease is limited to less than one order of magnitude for a reaction progress 550 of less than 0.9. The incremental deformation assumption thus provides valid first-order 551 strain rate estimates for a large range of reaction progresses. 552

Equation 18 is valid for all Da_{α} values and thus allows strain rate to be calculated in both the reaction- and the diffusion-controlled cases. At low Da_{α} (reaction-controlled regime), equation 18 can be approximated with equation 20, equivalent, at low stress $((\sigma_{\alpha} - P_{f,0}) V_r \ll RT)$, to the strain rate determined in reaction-controlled conditions in Raj (1982); Niemeijer et al. (2002); X. Zhang et al. (2010). However, at large stress, equation 20 tends to-

wards $\frac{k_r V_r}{L}$. This is consistent with the transition state theory predicting reaction rate independent from the force driving reaction $(A_{\{r,p\},\alpha})$ when $A_{\{r,p\},\alpha} \gg 0$ (Lasaga, 2014). 558 559 The expression generally used in the literature for strain rate in the reaction-controlled 560 case (Raj, 1982; Niemeijer et al., 2002; X. Zhang et al., 2010) does not follow the tran-561 sition state theory since it depends on effective stress as $\left(\exp\left(\frac{(\sigma_{\alpha}-P_{f_0})V_r}{RT}\right)-1\right)$ and thus 562 tends towards infinity at large stress. For the pressure solution of quartz under a stress 563 of 100 MPa, the ratio between the strain rates calculated with the expression found in the literature and with equation 20 is 1.6. This ratio exponentially increases with stress 565 since it is 10 at 500 MPa. It could therefore lead to strong change in theoretical estimates 566 especially when stress concentration occurs as it is the case in compacting rock aggre-567 gates (Niemeijer et al., 2002). 568

569

At high Da_{α} (diffusion-controlled regime), equation 18 can be approximated with equation 21. This latter equation can be compared to the one generally obtained in pres-570 sure solution studies (Rutter, 1976) which can be expressed for the geometry and the 571 formalism used here as (see Appendix C for a detailed derivation): 572

$$\dot{\epsilon_{\alpha S}} = -\frac{24c_{e,r,0}DwV_r}{L^3} \left(1 - \exp\left(\frac{(\sigma_\alpha - P_{f,0})V_r}{RT}\right)\right) \approx \frac{24c_{e,r,0}DwV_r^2\left(\sigma_\alpha - P_{f,0}\right)}{RTL^3} \quad (23)$$

This equation is the same as the one generally used for strain rate in the diffusion-573 limited case with the exception of the geometric factor 24 associated with the cubic ge-574 ometry used here (Rutter, 1976; Gratier et al., 2013). Its derivation requires two main 575 assumptions (Appendix C): a constant reaction rate and thermodynamic equilibrium in 576 the thin aqueous film (Rutter, 1976). These assumptions may seem contradictory since 577 the driving force for reaction is disequilibrium in the thin aqueous film, and the reaction 578 rate should thus be zero and not a constant at the equilibrium. The assumption of a con-579 stant reaction rate leads to a parabolic equation for aqueous species concentration (Ap-580 pendix C) whereas we derive in equation 4 an hyperbolic cosine function by using a re-581 action rate depending on the distance from the equilibrium. The assumption of thermo-582 dynamic equilibrium in the aqueous film is responsible for the main difference between 583 $\dot{\epsilon}_{\alpha D}$ and $\dot{\epsilon}_{\alpha S}$, that is the absence of the Da_{α} factor in equation 23 compared to equa-584 tion 21 (Appendix C). The strain rate is underestimated by one order of magnitude at 585 $Da_{\alpha} = 100$ with equation 23 compared to equation 21 (Figure 11). The dependency 586 of $\dot{\epsilon}_{\alpha D}$ on Da_{α} indicates that the strain rate depends on reaction rate (k_r) even if the 587 system is controlled by diffusion. An increase in reaction rate indeed leads to a higher 588 dissolved aqueous species concentration in the aqueous film. As the gradient in concen-589 tration between the aqueous film and the pores drives diffusion, the transport rate in-590 creases leading to a higher strain rate. 591

The new laws provided here have thus not only different mathematical forms than 592 the previous creep laws but they also lead to orders of magnitude differences in the es-593 timated strain rates. This has to be considered when discussing the importance of pres-594 sure solution for deformation in the Earth's crust. 595

596

5.2 Dominant deformation mechanism in the Earth's crust

Figures 3 C and D and 4 C and D provide new deformation mechanism maps in-597 cluding the pressure solution and dissolution-precipitation creep laws determined here. 598 As shown above, these creep laws involve less assumptions than the previous formalisms. 599 Moreover, equation 18 encompasses all Da_{α} values allowing strain rate to be computed 600 without an a priori assumption on the process controlling deformation (diffusion or re-601 action). Plotting deformation mechanism maps requires quantitative estimates of the pa-602 rameters used in the creep laws. Significant efforts have been devoted to the determi-603 nation of the thickness of the aqueous film and the diffusion coefficient (Revil, 2001; Niemei-604



Figure 11. Strain rate as a function of the Dahmköhler number (Da_{α}) in the aqueous film. The black plain line corresponds to the general expressions for strain rate (equation 18). The black dash-dot and dashed lines are the borderline cases when considering non-constant rates for low Da_{α} (equation 20) and high Da_{α} (equation 21), respectively. The red plain line is the strain rate generally used for diffusion-controlled system. It is derived with constant reaction rate and a condition for thermodynamic equilibrium in the aqueous film (equation 23). The calculations are performed for a typical grain size of $L = 100 \ \mu m$, $\sigma_{\alpha} = 100 \ MPa$, the molar volume of quartz $V_r = 22.10^{-6}m^3.mol^{-1}$, $w = 2.10^{-9}m$, $D = 10^{-10}m^2.s^{-1}$, $c_{e,r,0} = 1mol.m^{-3}$ and T = 573K. Strain rates are calculated for different Da_{α} by varying k_r from 10^{-13} to $10^{-5} \ mol.m^{-2}.s^{-1}$ based on the range given in the works of Tester et al. (1994) and Worley et al. (1996).

jer et al., 2002; Dysthe et al., 2002; Gratier et al., 2009; van Noort et al., 2007, 2011). 605 However, the reaction rate in the aqueous film, k_r , is poorly constrained. Previous stud-606 ies generally assume that the reaction rate determined on unconfined surfaces (bulk fluid) 607 can be used. However, the presence of catalytic dissolved aqueous species (Rimstidt, 2015) 608 or the decrease in water activity (Schott et al., 2009; Lamadrid et al., 2017; Rubie, 1986) 609 can modify the reaction rate in the aqueous film by several orders of magnitude com-610 pared to rates measured in bulk fluid. We fit here strain rate data from Niemeijer et al. 611 (2002) and Gratier et al. (2009) with equation 18 to estimate k_r . The determined val-612 ues are one to four orders of magnitude lower than the reaction rates measured in the 613 bulk fluid. We therefore plot two deformation mechanism maps for pressure solution (Fig-614 ure 3 C and D) and dissolution-precipitation (Figure 4 C and D) with reaction rates equal 615 or four orders of magnitude smaller than the one determined in the bulk fluid. For quartz, 616 the transition from reaction- to diffusion-controlled pressure solution is predicted to oc-617 cur between ~ 70 °C ($k_r = k_{rbulk}$; Figure 3 C) and ~ 350 °C ($k_r = k_{rbulk}/(10^4)$; Fig-618 ure 3 D). This is consistent with the previous temperature estimate of $\sim 150 \ ^{\circ}C$ for this 619 transition (Gratier et al., 2013). The computed maps indicate orders of magnitude lower 620 strain rates for pressure solution and dissolution-precipitation with $k_r = k_{rbulk} / (10^4)$ 621 than with $k_r = k_{rbulk}$ (Figures 3 C and 4 C). The distribution of the dominant defor-622 mation mechanisms is similar for the two reaction rates. However, it is different from the 623 deformation mechanism map proposed by Rutter (1976) in which diffusion creep dom-624 inates at temperatures higher than $\sim 600 \ ^{\circ}C$. The use of equation 18 instead of equa-625 tion 23 plays a key role in this switch from a map with three possible deformation mech-626 anism to a map where pressure solution dominates. Indeed, recovering with equation 18 627 a deformation mechanism map similar to Rutter (1976) requires a reaction rate eleven 628 orders of magnitude smaller than the one measured in a bulk fluid $(k_r = 10^{-16} mol.m^{-2}.s^{-1})$ 629 for quartz at 350 $^{\circ}C$). Figures 3 and 4 thus provide robust distributions of the defor-630 mation mechanisms even though the absolute strain rate values will probably need to 631 be re-evaluated when disposing of better constraints on reaction rate. These maps in-632 dicate that pressure solution and dissolution-precipitation creeps are the main deforma-633 tion mechanisms in the Earth's crust. 634

One has to keep in mind the limitations of the model when using the deformation 635 mechanism maps. First, we use a simple geometry with all the minerals dissolving or pre-636 cipitating in the same cuboid, and we consider that dissolved aqueous species are trans-637 ported at similar rates. We can thus not reproduce the complex distribution of miner-638 als in natural samples, and transport distances can be underestimated by several times 639 the grain size. These are second-order issues regarding uncertainties in quantitative mod-640 elling which are mainly due to the variation in reaction rate estimates by several orders 641 of magnitude. Moreover, other models are available to understand mineral distribution 642 or to compare the deformation of monomineralic and polymineralic assemblages (Wheeler, 643 1992; Ford & Wheeler, 2004). Mineral distribution can become a first-order process to 644 take into account only if it strongly modifies diffusivity or reaction rate. Greene et al. 645 (2009) measure an increase in quartz dissolution rate when it is in contact with mica rather 646 than with another quartz crystal. The role of sheet minerals is not fully understood but 647 is related to a change in electrical potential. These experimental results are consistent 648 with observations in natural samples showing the activation of pressure solution by the 649 presence of sheet silicates (Heald, 1955; Engelder & Marshak, 1985). Mineral distribu-650 tion could thus be a key process to be introduced in further model development but this 651 would require to better capture the physics underlying the catalytic effect of sheet sil-652 icates. 653

Secondly, we assume that free fluid is available in the system during deformation.
Fluid is probably not commonly present in the Earth's crust explaining why quartz commonly deforms by dislocation creep in natural settings at temperatures above 300 °C (Stipp et al., 2002; Trepmann & Stöckhert, 2003; Kilian et al., 2011). Similarly, diffusion creep is expected to occur at high temperature if fluid availability is low. These observations

combined with predictions of our model suggest that large sections of the Earth's crust 659 are dry or at least not wet enough to allow for pressure solution. It is critical to estimate 660 the range of fluid content necessary to activate pressure solution. This first requires to 661 better constrain the geometry of the fluid pathways involved in pressure solution. Evidence for dissolution-precipitation creep are mainly collected in metasediments contain-663 ing hydrous minerals (Stöckhert et al., 1999; Wassmann & Stöckhert, 2013a; Xia & Platt, 664 2017). Fluid availability can be transient for example in metamorphic environments where 665 fluid expelled during dehydration is transported towards the surface (Connolly, 1997; Om-666 lin et al., 2017). Fluid transport mechanisms over several kilometres involve large fluid 667 pathways whereas the stress sustained by the rock can only be transmitted to the fluid 668 in nanometre-size aqueous films (Israelachvili, 1992). High fluid availability may there-669 fore not favour pressure solution but the quantification of this effect requires estimation 670 of pore distribution up to the nanoscale. 671

⁶⁷² Finally, dissolution-precipitation creep is a transient mechanism since it occurs while
⁶⁷³ reaching equilibrium. It thus requires a driving force for reaction which can be a change
⁶⁷⁴ in temperature, pressure or chemistry.

675

5.3 Acquisition of GSPO by dissolution-precipitation creep

The observation of a GSPO is commonly used as a marker of dissolution-precipitation 676 creep in rocks (Gratier et al., 2013; Wassmann & Stöckhert, 2013a). The formation of 677 a GSPO requires that minerals form with an anisotropic shape and that the shapes of 678 the grains are orientated similarly. Several mechanisms can lead to a GSPO: 1) the tor-679 tuosity is lower for a diffusion path parallel rather than perpendicular to the schistos-680 ity leading to an anisotropic growth if the mineral grows by diffusion. The long axis of 681 the crystals is in the schistosity (Brady, 1983); 2) the grain growth kinetics depend on 682 crystallographic orientation (Awad et al., 2000); 3) the interfacial energies at the con-683 tact between the growing and the surrounding minerals can systematically vary due to 684 a crystallographic preferred orientation of the surrounding minerals (Kretz, 1966). This 685 leads to a growth preferred orientation inherited from the host mineral or matrix; 4) the 686 grains can rotate and/or plastically elongate for a significant finite strain of the matrix 687 (Willis, 1977; Means & Paterson, 1966); 5) as demonstrated here with numerical mod-688 elling or in experiments (Gratier et al., 2015), dissolution-precipitation under stress can 689 also favour grain shape preferred orientation. A combination of these mechanisms will 690 promote GSPO as shown for example with a positive feedback between pressure solu-691 tion and crystallographic preferred orientation (Bons & den Brok, 2000). 692

We document a pronounced GSPO for garnet and plagioclase in the samples from the Nufenen Pass area with aspect ratios ranging from 1.6 to 2.6 and a similar orientation at the centimetre scale.

Garnet grows isotropically, hence its crystallographic orientation cannot lead to the 696 observed formation of ellipses. Since maximum temperatures never exceeded 500 $^{\circ}C$, gar-697 net elongation by plastic deformation is very unlikely (Karato et al., 1995). Moreover, 698 the ellipses are obliquely oriented with respect to the schistosity and they all have a sim-699 ilar orientation (Figures 9 and 10 and Table 3). The variation of the diffusion coefficient 700 (Brady, 1983) and/or of the interfacial energy (Kretz, 1966) with the orientation rela-701 tive to the schistosity are thus not responsible for the aspect ratios measured here. This 702 suggests a formation after the main foliation event (D2), consistent with the conclusions 703 of Klaper and Bucher-Nurminen (1987) based on textural observations. The most probable mechanism for the acquisition of GSPO is thus growth under stress. Garnet defor-705 mation by pressure solution has already been observed in metamorphic rocks (Bell & Rube-706 nach, 1983; Hara et al., 1984; Bell et al., 1986; Duebendorfer & Frost, 1988; Álvarez-Valero 707 et al., 2005; Smit et al., 2011; Wassmann & Stöckhert, 2013a). 708

Plagioclase commonly develops a GSPO. The growth and dissolution rates of this 709 mineral depends on crystallographic orientation (Arvidson et al., 2004). However, anisotropic 710 reaction rates are not sufficient to produce a GSPO since the grains also need to have 711 the same orientation at the centimetre scale. GSPO in plagioclase can develop as a re-712 sult of plastic deformation (Stünitz et al., 2003), at temperature as low as 500 °C (Shigematsu 713 & Tanaka, 2000; Rosenberg & Stünitz, 2003). At low metamorphic grades, plagioclase 714 does not deform by plastic deformation but rather by dissolution-precipitation (Shelley, 715 1989). The maximum temperature estimate in the Nufenen pass area is ~ 500 °C (Kamber, 716 1993), that is close from the temperature at which plastic deformation can occur in pla-717 gioclase. However, there is no evidence for rotation in the studied samples, suggesting 718 that elongation is not associated with plastic deformation. The plagioclases collected in 719 the Nufenen pass area are elongated in the foliation, suggesting that GSPO is acquired 720 during or after the main deformation event D2 (Klaper & Bucher-Nurminen, 1987). Pla-721 gioclases are found in a fold at the contact between a massive carbonate strata and a 722 finely-grained schist (Figure 8 C). This may explain the variation of the GSPO observed 723 at the outcrop scale due to the refraction of schistosity during D2. As the plagioclases 724 are oriented in the foliation, the mechanism responsible for GSPO acquisition is more 725 difficult to determine than for garnet. It could be mass transfer during a dissolution-precipitation 726 process but also anisotropic diffusion or growth in the foliation. There is no relationship 727 between the orientation of the plagioclases and their aspect ratio (Table 3). If the mech-728 anism responsible for GSPO is stress-driven mass transfer, this indicates that the dif-729 ferential stress is rather constant throughout the outcrop during reaction even though 730 the orientation of the main stress components significantly varies at the centimetre scale. 731

The Dahmköhler number can be calculated with the fluid composition at the equilibrium, the reaction rate, the grain size, the diffusion coefficient and the aqueous film thickness (equation 5). There are some uncertainties associated with these parameters, in particular regarding the reaction rate which can vary over several orders of magnitude (see above). Taking into account these uncertainties, Da_{α} is above 1 at T > 300 °C for the muscovite + quartz <=> andalusite + sanidine + H₂O reaction, except near the reaction line (Schramke et al., 1987) (Figure 4).

The acquisition of GSPO is not expected from numerical modelling at high Da_{α} , 739 that is in most of the investigated stress-temperature domain except near the reaction 740 line (Figure 6). The dissolution-precipitation process is indeed controlled by diffusion 741 in most of the stress-temperature domain. This implies that mass transfer between the 742 faces is slow compared to reaction, leading to a precipitation of the secondary phases where 743 the primary phases are dissolved. Thus, the lack of GSPO in rocks does not necessary 744 indicate low stresses but rather suggests that reaction took place at high Da_{α} , in far from 745 the equilibrium conditions. Interestingly, rocks reacting in these conditions (e.g. hydrother-746 mal alteration, contact metamorphism) do not generally display GSPO (Roselle et al., 747 1997; Gerdes et al., 1999). Hydrothermal alteration of peridotite at mid-ocean ridges forms 748 rocks with a mesh texture without GSPO (Malvoisin et al., 2017). Such a reaction oc-749 curs in environments where stresses can be high as expected near detachment faults along 750 which mantle rocks are exhumed (Olive & Behn, 2014). Examples of reaction in far from 751 the equilibrium conditions also exist during regional metamorphism. Moore et al. (2019) 752 describe a primary mineralogical assemblage out of equilibrium reacting to form two dif-753 ferent secondary mineral assemblages with one stable at higher pressure (A1) than the 754 other (A2). A1 and A2 form under different orientations and have a similar thickness, 755 leading to a limited GSPO. This indicates reaction at high Da_{α} , which is consistent with 756 the high differential stress of 0.2 GPa calculated in Moore et al. (2019) (Figures 4 A and 757 B). 758

⁷⁵⁹ Low Da_{α} can only be reached at low temperature (T < 150 °C) or near thermo-⁷⁶⁰ dynamic equilibrium where reaction rates significantly decrease (Figure 4). Figure 6 in-⁷⁶¹ dicates that GSPO can only be formed at low Da_{α} . Diffusion indeed proceeds faster than

reaction, allowing mass to be transported from one face to the other before precipita-762 tion. The metasediments of the Nufenen pass area continuously dehydrate during the 763 prograde path in Barrovian metamorphism. At the same time, temperature increases lead-764 ing to the overstepping of metamorphic reactions. This overstepping is limited since the rock rapidly reacts by a dissolution-precipitation process in the presence of fluids. As 766 a result, prograde metamorphic reactions are thought to take place close to the equilib-767 rium line (Wood & Walther, 1983). When fluid is no longer present, the reaction stops 768 leaving a mineralogical assemblage which can be used to retrieve the pressure-temperature 769 conditions of metamorphism (Spear, 1993). Plagioclase and garnet in the metasediments 770 of the Nufenen pass area precipitate during or after the main foliation event (D2), that 771 is close to the peak metamorphism conditions (Klaper & Bucher-Nurminen, 1987). They 772 have thus undergone prograde metamorphism in the presence of fluid during the Alpine 773 collision. We thus interpret GSPO in these samples as the result of replacement under 774 stress near thermodynamic equilibrium. This interpretation is consistent with the results 775 of numerical modelling provided here, showing that the distance from the equilibrium 776 is the key parameter controlling the acquisition of GSPO in rocks. 777

The acquisition of a GSPO during dissolution-precipitation requires the presence 778 of fluid serving as a transport medium for the dissolved minerals. GSPO is observed here 779 in volatile-rich rocks (Bestmann et al., 2004; Imon et al., 2004; Wassmann et al., 2011; 780 Stokes et al., 2012; Bial & Trepmann, 2013; Wassmann & Stöckhert, 2013a) and could 781 be used as a marker for fluid presence during metamorphism. In addition, our numer-782 ical simulations clearly show that GSPO can only be formed near thermodynamic equi-783 librium. This suggests that GSPO could be used to probe the distance from the equi-784 librium during metamorphism. The distance from the equilibrium plays a key role on 785 the kinetics of reaction (Lasaga, 2014) but also, as shown below, on the barometric record 786 during metamorphism. 787

788

5.4 Pressure controlling metamorphic reactions

Determining the pressure of metamorphic reactions is crucial for interpreting ob-789 servations in natural samples, thermodynamic calculations and numerical models (Moulas 790 et al., 2019). It serves as a basis in the metamorphic petrology community to reconstruct 791 the geodynamic history of the rocks collected in the field (Spear, 1993). In the presence 792 of fluid, experiments (Llana-Fúnez et al., 2012), theoretical studies (Dahlen, 1992) and 793 field data (Holdaway & Goodge, 1990) suggest that fluid pressure is the relevant pres-794 sure for determining thermodynamic equilibrium. Fluid pressure in the aqueous film varies 795 at grain boundary due to interactions with solid surfaces (Israelachvili, 1992). It is equal 796 to the normal stress in thin fluid films leading to strong pressure gradients at the mi-797 crometre scale between differently oriented mineral surfaces (Gratier et al., 2013). Moore et al. (2019) document an orientation dependence for precipitation at grain boundary 799 during metamorphism. Wheeler (2014) proposes to calculate the affinity between dif-800 ferently oriented grain boundaries (reaction pathway) to estimate the effect of stress on 801 thermodynamic equilibrium. Mineral stability fields shift by several hundreds of mega-802 pascals with this approach. However, Fletcher (2015) indicates that one cannot freely 803 select a reaction pathway without taking into account reaction kinetics and diffusion. The 804 model proposed here considers these two processes and can thus be used to estimate the 805 effect of stress on pressure record during metamorphism. 806

The effect of stress on reaction can first be evaluated by trying to conceptually reproduce the approach of Wheeler (2014) with our model. Wheeler (2014) considers an incongruent pressure solution pathway to estimate the displacement of reaction line with stress. This is equivalent to consider that dissolution and precipitation occur in the aqueous film normal to σ_1 and σ_3 , respectively (low Da_{α}). The reaction line is defined as the zero chemical affinity curve ($A_{t,1,3} = 0$ or $c_{e,r,1} = c_{e,p,3}$ with our formalism). By definition, the dissolving phases have a higher solubility than the precipitating phases at the



Figure 12. Sketch showing the thermodynamic pressure for metamorphic reactions under stress in a pressure-temperature domain. The plain line is the reaction line where equilibrium between reactant and products is achieved. Far from the equilibrium, the thermodynamic pressure is the mean stress (σ_{mean}). Near the equilibrium, the thermodynamic pressure depends on the total volume change during reaction. It is σ_1 for $\Delta_r V < 0$ and σ_3 for $\Delta_r V > 0$.

same stress, so that $c_{e,r,1} > c_{e,p,1}$ and $c_{e,r,3} > c_{e,p,3}$. Moreover, solubilities always in-814 crease with pressure except near the critical point of water leading to $c_{e,r,1} > c_{e,r,3}$ and 815 $c_{e,p,1} > c_{e,p,3}$. Combining these four latter inegalities lead to $c_{e,r,1} > c_{e,p,3}$, which is 816 not compatible with the condition for zero chemical affinity. As a result, the incongru-817 ent pressure solution pathway used in Wheeler (2014) cannot be reproduced with our 818 pressure solution model and pressure solution is thus not expected to significantly mod-819 ify thermodynamic equilibrium. The only way to reproduce Wheeler (2014)'s approach 820 is to consider that dissolution and precipitation occur in the aqueous film normal to σ_3 821 and σ_1 , respectively $(c_{e,p,1} = c_{e,r,3})$. This requires a mechanism generating a large su-822 persaturation under σ_3 before transport and precipitation under σ_1 . Such a mechanism 823 is known as force of crystallisation (Steiger, 2005). 824

The model proposed here also provides a way to quantitatively estimate the effect 825 of stress on equilibrium. Mass transfer between differently oriented grain surfaces can 826 only occur at low Da_{α} (fast diffusion compared to reaction). The estimates of Da_{α} in 827 Figure 4 are high except near the reaction line. Moreover, the reaction rate does not de-828 pend on stress at high $A_{t,\alpha,\beta}$ (equation 1). Differential stress is thus not expected to have 829 an effect on thermodynamics in far from the equilibrium conditions (Figure 12). The nu-830 merical simulations performed here indicate that, near the equilibrium, reaction is af-831 fected by differential stress. σ_1 controls the reaction if $A_{t,\alpha,\beta}$ increases with pressure ($\Delta_r V <$ 832 0). σ_3 controls the reaction otherwise ($\Delta_r V > 0$). These results are in agreement with 833 the experiments performed by Richter et al. (2016), showing that the quartz to coesite 834 transition $(\Delta_r V < 0)$ depends on σ_1 . Thermodynamic equilibrium recorded in miner-835 alogical assemblages is thus strongly dependent on the relationship between reaction rate 836 and $A_{t,\alpha,\beta}$. 837

6 Conclusion

We propose here a model for pressure solution and dissolution-precipitation creeps. 839 This model provides revised deformation mechanism maps for pressure solution. The pre-840 vious deformation mechanism maps were not incorporating the effect of concentration 841 changes in the aqueous film on reaction rate. We show the critical role of this dependency 842 for estimating strain rates. We also propose new deformation mechanism maps and creep 843 laws for dissolution-precipitation creep. Dissolution-precipitation creep is the main de-844 formation mechanism in the Earth's crust provided that fluid is available and disequi-845 librium is achieved. The refinement of these deformation mechanism maps requires a de-846 tailed investigation of the dependence of reaction rate on pressure and water activity in 847 thin fluid films. We also use numerical modelling to gain insights on the acquisition of 848 GSPO during metamorphism and the pressure controlling metamorphic reactions. We 849 show here that the distance from the equilibrium plays a key role for these two topics. 850 The model is indeed controlled by diffusion in far from the equilibrium conditions, lead-851 ing to limited mass transfer between the reacting mineral faces. As a result, GSPO does 852 not develop and the effect of stress on thermodynamic pressure is small. In close from 853 the equilibrium conditions, significant differences in reaction rate occur between the min-854 eral faces, leading to a control of the reaction by σ_1 or σ_3 . Moreover, the mineral grains 855 change of shape and a GSPO is formed, in agreement with observations in samples from 856 the Nufenen pass area. These results can serve as a basis to interpret GSPO and baro-857 metric record in metamorphic rocks. 858

Appendix A Fit of the experiments of quartz compaction

We determined k_r by fitting with equation 18 the dataset of Niemeijer et al. (2002) for quartz grains compaction in pure water under stresses ranging from 50 to 150 MPa and at temperature comprised between 400 and 600 °C. Strain rate data are reproduced from their figure 4.

 k_{rbulk} ranges from $3.3.10^{-6} mol.m^{-2}.s^{-1}$ at 400 °C to $1.4.10^{-4} mol.m^{-2}.s^{-1}$ at 600 864 $^{\circ}$ C (Tester et al., 1994). The grain sizes are given in their Table 1. The experiments are 865 loaded with sands and the grain contacts thus evolve during compaction. To take into 866 account grain contact evolution, a stress concentration factor depending on porosity $(B(\phi))$ 867 is introduced in the equations in front of the $(\sigma_{\alpha} - P_{f,0})$ term (Dewers & Hajash, 1995). 868 This factor theoretically tends towards infinity at the beginning of the compaction even 869 though a small elastic distortion occurs leading to finite grain contact (X. Zhang et al., 870 2010). B is modelled here by using a body centered cubic packing of spherical grains for 871 which: 872

$$B(\phi) = \frac{d(\phi)^2}{\pi \left(\left(\frac{L}{2}\right)^2 - \left(\frac{d(\phi)}{2}\right)^2 \right)}$$
(A1)

where d is the diameter of the grain-to-grain contact determined by numerically solving:

$$\frac{8}{3}\pi \left(\frac{L}{2}\right)^3 - \frac{4}{3}\pi \left(L-d\right)^2 \left(L+\frac{d}{2}\right) - (1-\phi)\left(\frac{2d}{\sqrt{3}}\right)^3 = 0$$
(A2)

B is approximately 40 for a ratio between actual porosity and initial porosity of
0.9. This corresponds to an effective pressure of 4 GPa at grain contact for an effective
pressure of 100 MPa applied on the sample. The reaction rate constant theoretically varies
with pressure as (Schott et al., 2009):

r p σ_{α} $P_{f,0}$ $\vec{x_{\alpha}}$ $\xi \{r,p\},\alpha$ $k_{\{r,p\}}$ k_{m} k_{rbulk} a_{α} $a_{e,\{r,p\}\alpha}$ c_{α} $c_{e,\{r,p\}\alpha}$ c_{0} $c_{e,\{r,p\},\alpha}$ c_{0} $c_{b,\alpha}$ D $S_{\{r,p\},\alpha}$ $S_{0,\{r,p\}}$ w r L	Subscript referring to the dissolving phases Subscript referring to the precipitating phases Stress component α with $\alpha = 1, 2$ or 3 and $\sigma_1 > \sigma_2 > \sigma_3$ Pore pressure Axis vector parallel to σ_{α} Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration the equilibrium of dissolved aqueous species in the pores Concentration in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Liength of the grain boundary in 1D Diameter of the grain boundary in 1D	Pa Pa $mol.s^{-1}$ $mol.m^{-2}.s$ $mol.m^{-2}.s$ $mol.m^{-2}.s$ $none$ $none$ $mol.m^{-3}$
$D = \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} $	Subscript referring to the precipitating phases Stress component α with $\alpha = 1, 2$ or 3 and $\sigma_1 > \sigma_2 > \sigma_3$ Pore pressure Axis vector parallel to σ_{α} Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration of dissolved aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$. Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D Diameter of the grain boundary in 1D	Pa Pa $mol.s^{-1}$ $mol.s^{-2}.s$ $mol.m^{-2}.s$ $mol.m^{-2}.s$ $mol.m^{-3}$
$ \begin{array}{l} F_{\alpha} \\ F_{f,0} \\ \overline{c}_{\alpha} \\ \{r,p\},\alpha \\ \overline{c}_{r,p},\alpha \\ \overline{c}_{r,p} \\ \overline{c}_{m} \\ \overline{c}_{rbulk} \\ la_{\alpha} \\ \overline{c}_{e,\{r,p\}\alpha} \\ \overline{c}_{\alpha} \\ \overline{c}_{e,\{r,p\}\alpha} \\ \overline{c}_{\alpha} \\ \overline{c}_{e,\{r,p\}\alpha} \\ \overline{c}_{e,\{r,p\},\alpha} \\ \overline{c}_{b,\alpha} \\ D \\ \overline{c}_{b,\alpha} \\ $	Stress component α with $\alpha = 1, 2$ or 3 and $\sigma_1 > \sigma_2 > \sigma_3$ Pore pressure Axis vector parallel to σ_{α} Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D Diameter of the grain boundary in 1D	$\begin{array}{c} Pa\\ Pa\\ m\\ mol.s^{-1}\\ mol.m^{-2}.s\\ mol.m^{-2}.s\\ mol.m^{-2}.s\\ none\\ none\\ mol.m^{-3}\\ mol.m^$
$P_{f,0}$ F_{α} $F_$	Pore pressure Axis vector parallel to σ_{α} Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration of dissolved aqueous flow equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain boundary in 1D	$\begin{array}{c} Pa \\ m \\ mol.s^{-1} \\ mol.m^{-2}.s \\ mol.m^{-2}.s \\ mol.m^{-2}.s \\ none \\ none \\ mol.m^{-3} \\ mol.m^{-$
$\sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{i=1}^{n} \sum_{i=1}^{n} \sum_{i=1}^{n} \sum_{i$	Axis vector parallel to σ_{α} Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain boundary in 1D Diameter of the grain boundary in 1D	$ \begin{array}{c} {\rm m} \\ mol.s^{-1} \\ mol.m^{-2}.s \\ mol.m^{-2}.s \\ mol.m^{-2}.s \\ none \\ none \\ mol.m^{-3} \\ mol.m^{-$
$\begin{cases} r, p \}, \alpha \\ \{r, p \}, \alpha \\ \{r$	Reaction rate in the aqueous film normal to $\vec{x_{\alpha}}$ Reaction rate constant Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D Diameter of the grain to react defined in equation A2	$mol.s^{-1}$ $mol.m^{-2}.s$ $mol.m^{-2}.s$ none none $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$
$\begin{cases} (r,p), \alpha \\ \delta \{r,p\}, \alpha \\ \delta \{r,p\} \\ \delta \\ \delta \\ m \\ \delta \\ r bulk \\ l_{\alpha} \\ l_{e}, \{r,p\}\alpha \\ \delta \\ c_{\alpha} \\ c_{$	Reaction rate constant defined below equation 9 Reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$ \begin{array}{c} mol.m^{-2}.s\\ mol.m^{-2}.s\\ mol.m^{-2}.s\\ mol.m^{-2}.s\\ none\\ none\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ m^2.s^{-1}\\ m^2\\ m\\ m\\ m\\ m\\ m\\ m\\ \end{array} $
$\{r,p\}$ im i	Mean reaction rate constant defined below equation 9 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$ \begin{array}{c} mol.m^{-2}.s\\ mol.m^{-2}.s\\ mol.m^{-2}.s\\ none\\ none\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ m^2.s^{-1}\\ m^2\\ m\\ m\\ m\\ m\\ m\\ m\\ \end{array} $
$\sum_{k=1}^{m} \sum_{k=1}^{m} \sum_{k$	Reaction rate constant defined below equation 5 Reaction rate constant in the bulk fluid Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D Diameter of the grain boundary in 20	$ \begin{array}{c} mot.m^{-3}.s\\ mol.m^{-3}.s\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ mol.m^{-3}\\ m^2.s^{-1}\\ m^2\\ m\\ m\\ m\\ m\\ m\\ m\\ \end{array} $
$rbulk$ l_{α} $l_{e,{r,p}\alpha}$ $c_{e,{r,p}\alpha}$ $c_{e,{r,p},0}$ $c_{e,{r,p},0}$ $c_{e,{r,p},\alpha}$ $c_{e,{r,p},\alpha}$ $c_{e,{r,p},\alpha}$	Activity of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Liength of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	none none $mol.m^{-3}$
L_{α} $L_{e,\{r,p\}\alpha}$ L_{a} $L_{e,\{r,p\}\alpha}$ $L_{e,\{r,p\}\alpha}$ $L_{e,\{r,p\},\alpha}$ D D D D D D D D	Activity of dissolved aqueous species in the aqueous min normal to x_{α} Activity at the equilibrium of dissolved aqueous species in the film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D	none none $mol.m^{-3}$ mo
$be, \{r, p\} \alpha$ $c \alpha$ $c \alpha$ $c e, \{r, p\} \alpha$ c 0 $c e, \{r, p\}, 0$ $c b, \alpha$ D $b (r, p), \alpha$ D $c 0, \{r, p\}, \alpha$ c 0 $c 0, \{r, p\}, \alpha$ $c 0, \{r, p\}, \alpha$ c	Activity at the equilibrium of dissolved aqueous species in the him normal to \vec{x}_{α} Concentration of dissolved aqueous species in the aqueous film normal to \vec{x}_{α} Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to \vec{x}_{α} Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to \vec{x}_{α} . Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to \vec{x}_{α} Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D	none $mol.m^{-3}$ $mol.m^{-$
α a b c , { r,p } α c c , { r,p }, 0 c c c c c c c c	Concentration of dissolved aqueous species in the aqueous him normal to x_{α} Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Diameter of the grain boundary in 1D	$mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $m^{2}.s^{-1}$ m^{2} m^{2} m m m
$e_{i} \{r, p\} \alpha$ $e_{i} \{r, p\}, 0$ $e_{i} \{r, p\}, 0$ $e_{i} \{r, p\}, \alpha$ $f_{i} \{r, p\}$	Concentration at the equilibrium of dissolved aqueous species in the aqueous film normal to $\vec{x_{\alpha}}$ Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $m^2.s^{-1}$ m^2 m^2 m m m m
c_0 $c_{e,\{r,p\},0}$ $c_{b,\alpha}$ D $S_{\{r,p\},\alpha}$ $S_{0,\{r,p\}}$ v c_{L}	normal to x_{α} Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $m^2.s^{-1}$ m^2 m^2 m m m m
$S_{e,\{r,p\},0}$ $S_{e,\{r,p\},\alpha}$ $S_{\{r,p\},\alpha}$ $S_{0,\{r,p\}}$ v r	Concentration of dissolved aqueous species in the pores Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$mol.m^{-3}$ $mol.m^{-3}$ $mol.m^{-3}$ $m^2.s^{-1}$ m^2 m^2 m m m m
$E_{e}, \{r, p\}, 0$ $E_{b, \alpha}$ D D $\{r, p\}, \alpha$ D $S_{0}, \{r, p\}$ v c C	Concentration at the equilibrium of dissolved aqueous species in the pores Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$mol.m^{-3}$ $mol.m^{-3}$ $m^2.s^{-1}$ m^2 m^2 m m m m
$\mathcal{S}_{t,p}, \alpha$ $\mathcal{S}_{t,p}, \alpha$ $\mathcal{S}_{0,\{r,p\}}$ v	Concentration when balance between the amounts of dissolving and precipitating minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$mol.m^{-3}$ $m^2.s^{-1}$ m^2 m^2 m m m
$\sum_{\{r,p\},\alpha} \sum_{\{r,p\},\alpha} \sum_{\{v,p\}} \sum_{i=1}^{N} \sum_{j=1}^{N} \sum_{i=1}^{N} \sum_{i=1}^{N} \sum_{i=1}^{N} \sum_{i=1}^{N} \sum_{i=1}^{N} \sum_{i=1$	minerals in the aqueous film normal to $\vec{x_{\alpha}}$. Defined below equation 4. Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$m^2.s^{-1}$ m^2 m^2 m m m
$D = \{r,p\}, \alpha$ $D = \{r,p\}, \alpha$ $D = \{r,p\}$ $U = \{r,p\}$	Diffusion coefficient in the aqueous fluid film Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$m^2.s^{-1}$ m^2 m^2 m m m
$\sum_{i=1}^{n} \{r,p\}, \alpha$ $\sum_{i=1}^{n} \{r,p\}$	Reactive surface area in one aqueous film normal to $\vec{x_{\alpha}}$ Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$egin{array}{c} m^2 \ m^2 \ m \ m \ m \ m \end{array}$
0,{ <i>r</i> , <i>p</i> }	Reactive surface area in one pore Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	${m^2 \over m} {m \over m}$
	Thickness of the aqueous film Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	$egin{array}{c} m \ m \ m \end{array}$
;	Length along the grain boundary in 1D Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	${m \atop m}$
- 	Length of the grain boundary in 1D Diameter of the grain-to-grain contact defined in equation A2	m
-	Diameter of the grain-to-grain contact defined in equation A2	
,		m
Da_{α}	Damköhler number in the aqueous film normal to $\vec{x_{\alpha}}$. Defined in equation 5.	none
Da_0	Damköhler number in the pores. Defined below equation 7.	none
/(m m)	Molar volume	$m^{3}.mol^{-1}$
$\{r,p\}$	Change in volume during reaction $(V_{\rm c} - V_{\rm c})$	$m^3 mol^{-1}$
<u> </u>	Volume of one pore	m^3
VV^*	Activation volume used in equation A^3	$m^{3} mol^{-1}$
	Porosity during compaction experiments	nt
ba	Initial porosity during compaction experiments	none
0	Chamical potential of the minoralogical components dissolved in the fluid	$Imol^{-1}$
$f_{f}(r,p),\alpha$	Chemical potential of the colid minoralogical components dissolved in the huid	J.mol
$s, \{r, p\}, \alpha$	Chemical of the dissolution on presinitation reactions in the acusous film	J.mol $I \approx cl^{-1}$
$A_{\{r,p\},\alpha}$	Chemical amily of the dissolution of precipitation reactions in the aqueous $\lim_{n \to \infty} \frac{1}{n}$	J.mol -
	normal to x_{α} $(\mu_{s,\{r,p\},\alpha} - \mu_{f,\{r,p\},\alpha})$	T 1_1
$A_{t,\alpha,\beta}$	Chemical affinity of the replacement reaction $(\mu_{s,r,\alpha} - \mu_{s,p,\beta})$	$J.mol^{-1}$
R	Gas constant	$J.K^{-1}.mo$
	Temperature	K_{1}
α	Strain rate in direction $\vec{x_{\alpha}}$	s^{-1}
αV	Strain rate in direction $\vec{x_{\alpha}}$ when control by volume change during reaction	s^{-1}
αD	Strain rate in direction $\vec{x_{\alpha}}$ when control by diffusion	s^{-1}
αR	Strain rate in direction $\vec{x_{\alpha}}$ when control by reaction	s^{-1}
αS	Strain rate in direction $\vec{x_{\alpha}}$ derived in a similar way to Rutter (1976)	s^{-1}
\dot{dis}	Strain rate for dislocation creep defined in B1	s^{-1}
dif	Strain rate for diffusion creep defined in B2	s^{-1}
3	Stress concentration factor defined in equation A1	none
4	Pre-exponential factor in the experimental fit of k_r	$mol.m^{-2}$.
Ξa	Energy of activation in the experimental fit of k_r	$J.mol^{-1}$
Adia	Material parameter for dislocation creep	$Pa^{-n}.s^{-1}$
-ars Eadin	Energy of activation for dislocation creep	$Jmol^{-1}$
- ~uis	Stress exponent for dislocation creep	none
fuec	Water fugacity for dislocation creep	none
н20 э	Water fugacity exponent for dislocation green	none
и Л. н. а	Pro exponential factor for diffusion croop	$m^2 D_a - 1$
∎dif E a	Frenze of estimation for diffusion encorp	$111 \cdot r^{-1} - 1$

$\begin{array}{ c c c }\hline Da_0\\ Da_\alpha \end{array}$	0	∞
0	$c_{0} = \frac{4\sum_{\alpha} (c_{b,\alpha} D a_{\alpha}^{2}) + c_{b,0} D a_{0}^{2}}{4\sum_{\alpha} (D a_{\alpha}^{2}) + D a_{0}^{2}} c_{\alpha} = c_{0}$	$c_0 = c_{b,0}$ $c_\alpha = c_0$
∞	$c_0 = \frac{\sum_{\alpha} c_{b,\alpha} D a_{\alpha}}{\sum_{\alpha} D a_{\alpha}}$ $c = c_{b,\alpha}$	$c_0 = c_{b,0}$ $c_\alpha = c_{b,\alpha}$

Table 2. Borderline cases for c_{α} and c_0 as a function of the Da numbers in the pore (Da_0) and in the aqueous film (Da_{α}) .

Sample	Porphyroblast	S1(field)	n_{ilm}	F(ilmenite)	n_{pb}	MEA	MSP	F/MSP (°)	F/MEA (°)	Aspect ratio
LB_2018_1	Plagioclase	348/73	1126	140/74	32	156/41	5/62	62	1	2.0 ± 0.4
LB_2018_2	Plagioclase	348/73	1417	150/90	40	181/66	169/86	20	12	2.2 ± 0.4
LB_2018_3	Plagioclase	337/81	1182	112/85	40	266/67	222/70	72	5	2.4 ± 0.6
LB_2018_3_2	Plagioclase	337/81	814	304/85	25	326/79	216/78	87	1	2.0 ± 0.5
LB_2018_4	Plagioclase	138/89	839	279/87	13	270/59	247/81	32	7	2.3 ± 0.7
LB_2018_5	Plagioclase	138/89	1539	108/90	17	282/86	227/86	61	0	2.4 ± 0.7
LB_2018_11	Plagioclase	131/89	991	312/83	42	350/68	325/80	13	7	2.6 ± 0.4
LB_2018_6	Garnet	352/78	1822	356/76	75	330/76	158/88	24	19	1.8 ± 0.4
LB_2018_7	Garnet	352/81	1480	352/83	67	207/63	169/73	25	22	1.6 ± 0.3
LB_2018_7_2	Garnet	352/81	1471	354/84	96	236/77	158/77	25	18	1.8 ± 0.4
LB_2018_8	Garnet	350/79	1374	342/82	40	200/79	165/84	15	15	2.1 ± 0.5
LB_2018_9	Garnet	350/79	1364	348/79	40	197/80	171/85	16	15	2.3 ± 0.9
LB_2018_10	Garnet	NA*	654	$126/30^{*}$	65	$132/11^{*}$	$5/15^{*}$	39	7	1.7 ± 0.2

Table 3. Results of the statistical analysis for porphyroblasts orientation (values are given as Azimuth/Dip). S1(field), F(ilmenite), MEA and MSP refer to the trend/plunge of the Schistosity measured in the field, the Foliation measured with the ilmenite main shortening plane, the Mean main Elongation Axis of the porphyblast and the Mean main Shortening Plane of the porphyroblast, respectively. The mean orientations are determined with Bingham distribution. n_{ilm} and n_{pb} are the number of analyzed ilmenite and porphyroblast grains, respectively. F/MSP is the angle between the foliation orientation measured with ilmenite and the main shortening axis. F/MEA is the angle between the foliation orientation measured with ilmenite and the main elongation axis. *: sample LB_2018_10 was not collected in place and orientations are thus given relative to an arbitrary plane chosen as the planar bottom of the core.

$$\left. \frac{\partial lnk_r}{\partial P} \right|_T = -\frac{\Delta V^* \left(\sigma_\alpha - P_{f,0} \right)}{RT} \tag{A3}$$

where ΔV^* is the volume of activation (volume of the activated complex minus volume of the reactant). ΔV^* is approximately - 1.5 $cm^3.mol^{-1}$ at 200-300°C and several tens of megapascals (R. Zhang et al., 2015). Using this volume of activation, the reaction rate of quartz dissolution should increase with pressure by a factor ~ 1.7, ~ 13 and ~ 3.10⁴ for stresses of 200 MPa, 1 GPa and 4 GPa, respectively. Equation A3 allows to correct reaction progress for the effect of pressure.

Appendix B Dislocation and diffusion creeps for the deformation mechanism maps

Dislocation creep is modelled following Tokle et al. (2019) as:

$$\epsilon_{dis} = A_{dis} \left(\sigma_{\alpha} - P_{f,0} \right)^n f_{H2O}^h \exp\left(-\frac{Ea_{dis}}{RT}\right) \tag{B1}$$

with A_{dis} a material parameter, n is a stress exponent, f_{H2O} is the water fugacity, h is the water fugacity exponent and Ea_{dis} is the activation energy for dislocation. We used the parameters from the extrapolated fits of Tokle et al. (2019) (their Table 1). We take into account the change of stress exponent in the flow law (from n = 4 to n =3) when stress increases. We use a linear transition from one flow law to the other between 100 and 400 MPa. Water fugacity is calculated with the Pitzer and Sterner (1994)'s equation of state.

⁸⁹⁵ Diffusion creep is modelled following Rutter and Brodie (2004):

$$\epsilon_{dif} = \frac{A_{dif} \left(\sigma_{\alpha} - P_{f,0}\right) \exp\left(-\frac{Ea_{dif}}{RT}\right)}{L^2} \tag{B2}$$

where A_{dis} is a material parameter and Ea_{dif} is the activation energy for diffusion creep.

Appendix C Creep law for pressure solution with a derivation similar to Rutter (1976)

We derive in the following a creep law in the diffusion-controlled case in a similar way to Rutter (1976) but with the formalism and the geometry adopted here. The two main assumptions used in Rutter (1976) are that the reaction rate is constant ($\dot{\xi}_{r,\alpha} = k_r S_{r,\alpha}$) and that thermodynamic equilibrium is achieved in the thin aqueous film ($c_{\alpha} = c_{e,r,\alpha}$).

The assumption of constant reaction rate simplifies equation 2 at steady state in one dimension as:

$$D\frac{\partial^2 c_{\alpha}}{\partial x^2} + \frac{k_r}{w} = 0 \tag{C1}$$

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which can be solved to express c_{α} as a parabolic function:

$$c_{\alpha}\left(x\right) = c_{0} + c_{e,r,\alpha} \frac{Da_{\alpha}^{2}}{2} \left(\frac{x}{L} - \left(\frac{x}{L}\right)^{2}\right)$$
(C2)

An other equation for concentration is generally considered by assuming the achieve-908 ment of thermodynamic equilibrium in the aqueous film by integrating equation 10 over 909 the aqueous film length (equation 3 from Rutter (1976)): 910

$$\int_{0}^{L} c_{\alpha}(x) dx = c_{e,r,\alpha} L \tag{C3}$$

Equations C2 and C3 deal with the same single variable, $c_{\alpha}(x)$. They are gener-911 ally combined to express one of the model parameters (usually the reaction rate, k_r) as 912 a function of the others: 913

$$k_r = 12 \frac{c_{e,r,0} Dw}{L^2} \left(\exp\left(\frac{\left(\sigma_\alpha - P_{f,0}\right) V_r}{RT}\right) - 1 \right)$$
(C4)

Introducing the derivative of equation C2 at x = 0 into equation 13 and replac-914 ing k_r with equation C4 provide the following equation for strain rate : 915

$$\dot{\epsilon_{\alpha S}} = -\frac{24c_{e,r,0}DwV_r}{L^3} \left(1 - \exp\left(\frac{(\sigma_\alpha - P_{f,0})V_r}{RT}\right)\right) \approx \frac{24c_{e,r,0}DwV_r^2\left(\sigma_\alpha - P_{f,0}\right)}{RTL^3} \quad (C5)$$

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The mathematical model can be reproduced following derivations specified in the text 918

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