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T. Len, M. Bahri, O. Ersen, Y. Lefkir, L. Cardenas, et al.. Ultradispersed Mo/TiO₂ catalysts for CO₂ hydrogenation to methanol. Green Chemistry, 2021, 23, pp.7259-7268. 10.1039/d1gc01761f . hal-03339757

HAL Id: hal-03339757

<https://hal.science/hal-03339757>

Submitted on 28 Sep 2021

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Ultradispersed Mo/TiO₂ catalysts for CO₂ hydrogenation to methanol

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Abstract

Mo/TiO₂ catalysts with atomic dispersion of molybdenum appear active and stable in the gas-phase hydrogenation of CO₂. The comparison between various titania materials shows a crucial effect of the support surface structure on the methanol yield. Molybdenum supported at low coverage on rutile titania nanorods is the most active and methanol-selective system. From catalyst characterization by aberration-corrected scanning transmission electron microscopy, near-ambient pressure X-ray photoelectron spectroscopy, diffuse reflectance UV-vis spectroscopy, and temperature-programmed techniques, we suggest that the most active catalysts for methanol production involve atomically-dispersed oxomolybdate species with high reducibility and strong interaction with the rutile support.

Introduction

Due to environmental concerns, and following the European Commission climate strategies and targets,¹ the reduction of greenhouse gas emissions has become mandatory. In this context, promising approaches for the valorisation of CO₂ have been developed, allowing the synthesis of value-added chemicals such as urea, salicylic acid, cyclic carbonate and polypropylene carbonate at the laboratory scale.^{2–4} The most promising valorisation strategy – provided that electricity and hydrogen production costs are reduced^{5,6} – consists in the transformation of effluent CO₂ through catalytic hydrogenation,^{7–10} leading to valuable products such as carbon monoxide, hydrocarbons and oxygenates.^{11,12} Methanol, a platform chemical with high interest in the production of fuels and plastics,^{13,14} is industrially produced from syngas (CO and H₂) in the presence of a Cu/ZnO/Al₂O₃ catalyst at 5–10 MPa and 250–300 °C. Researches on CO₂ hydrogenation to methanol have mostly focused on this system, for understanding and optimising its catalytic performances.^{15–21} However, this catalyst is pyrophoric, and a serious threat exists in the next decades for zinc availability.²² Moreover, the

generation of water as a by-product of CO₂ hydrogenation induces ZnO agglomeration, Cu oxidation and sintering, leading to catalyst deactivation.^{23,24} Hence, it is desirable to find alternative catalysts with enhanced performances.^{25–27} This includes not only the catalyst stability but also its activity and selectivity to methanol.²⁸

Ultradispersed metal-based catalysts, *i.e.* single-atom catalysts (SACs) or subnanometric cluster-based catalysts,²⁹ are an attractive new class of materials which potentially offer maximum atom-efficiency and specific catalytic properties.^{30–33} A large fraction of SAC studies has focused on noble metals, with a view to cost reduction. Although some strategies have been proposed,^{34–37} the stabilization of single noble-metal atoms on oxides is challenging because of their tendency to aggregation.^{29,38–40}

Molybdenum-based catalysts are widely used in petroleum refining, and catalyze syngas conversion to alcohols.⁴¹ Mo has a half-filled d-electron shell and a variable valence state, which makes this oxophilic element suitable for tuning the catalytic performance through coordination engineering.⁴² Non-precious catalysts containing Mo-based species supported on TiO₂ (MoO_x/TiO₂, MoS₂/TiO₂, etc.) are well-known for photocatalysis,⁴³ as well as thermocatalytic oxidation^{44,45} and hydrodesulfurization^{46–48} reactions. When CO and CO₂ hydrogenation reactions were carried out over Mo/TiO₂,^{49–51} this system was found inefficient. Shimizu's group recently reported that the addition of a noble metal such as Pt is mandatory to activate a 30 wt% Mo/TiO₂-P25 sample for the CO₂-to-methanol reaction.⁵¹

Herein, we disclose the unexpected CO₂ hydrogenation performances of selected low wt% Mo/TiO₂ catalysts. A broad range of TiO₂ materials, Mo loadings and pretreatment conditions were studied to compare their impacts on CO₂ conversion activity and selectivity to methanol.

Experimental section

Catalyst preparation

The TiO_2 samples, the molybdenum precursor (Aldrich, 99.98% trace metals basis) and the reference $\text{Cu/ZnO/Al}_2\text{O}_3$ catalyst (Thermo Fisher) were used without specific treatment. For titania supports, DT51D (>99.5%) and PC500 (>85%) were obtained from Tronox, P25 and P90 (>99.5%) were purchased from Evonik Aeroxide, and RL11A (>99.5%) was purchased from Solvay.

In a typical preparation, 5 g of TiO_2 , an appropriate amount (depending on the target Mo loading) of $\text{Mo}_7\text{O}_{24}(\text{NH}_4)_6 \cdot 4\text{H}_2\text{O}$ and 60 mL of deionized water were stirred for 2 h in a round bottom flask. The mixture was dried in a rotary evaporator at 60 °C, and the resulting powder was treated in a flow fixed-bed reactor under H_2 (40 mL/min) for 2 h at 500 °C (5 °C/min).

Catalytic testing

The catalytic tests were performed using a straight stainless-steel flow fixed bed reactor (internal diameter 7 mm), heated with a tubular oven. Gas flows were controlled by Brooks Instruments flowmeters and analyzed by an Inficon Fusion micro gas chromatograph equipped with molecular sieve and RT-Q-Bond modules. The temperature program for the RT-Q-Bond was 60 °C for 70 s, then 230 °C for 120 s (2.5 °C/min). The total pressure was set to 30 bar using a Tescom ER5000 electropneumatic PID controller driving a Tescom membrane backpressure regulator. A heating system was set up to keep the temperature above 70 °C in the gas lines in order to avoid condensation. Prior to catalytic tests the as-prepared catalysts were treated *in situ* in the catalytic reactor under H_2 (40 mL/min) for 2 h (5 °C/min) at atmospheric pressure in the 450-700 °C range (standard value 450 °C). The catalytic experiments were conducted with an $\text{H}_2/\text{CO}_2/\text{N}_2$ mixture (3:1:1 vol. fractions and 50 mL/min total molar flow rate) and 400 mg of catalyst, leading to a gas hourly space velocity (GHSV) of $7500 \text{ mL} \cdot \text{g}^{-1} \cdot \text{h}^{-1}$. The following standard temperature sequence was used for the catalytic tests: from RT to 200 °C at 5 °C/min, then 200 °C to 300 °C at 0.25 °C/min.

Conversion of CO₂ (χ_{CO_2}), selectivities to product P (S_P), methanol (MeOH) production turnover frequency (TOF_{MeOH}) and space-time yield (STY_{MeOH}) were calculated as follows, with $Q_{CO_2}^{in}$, Q_i^{out} , n_{Mo} , M_{MeOH} , and m_{cat} representing the molar flow rate of CO₂ at the reactor inlet, the molar flow rate of product i at the reactor outlet, the molar amount of Mo, the molar mass of methanol, and the catalyst mass, respectively. For TOF calculations, all Mo atoms were considered as exposed to the gas phase (100% dispersion).

$$\chi_{CO_2} = \frac{\sum_i Q_i^{out}}{Q_{CO_2}^{in}} \quad S_P = \frac{Q_P^{out}}{\sum_i Q_i^{out}} \quad TOF_{MeOH} = \frac{Q_{CO_2}^{in} \chi_{CO_2} S_{MeOH}}{n_{Mo}} \quad STY_{MeOH} = \frac{Q_{CO_2}^{in} \chi_{CO_2} S_{MeOH} M_{MeOH} \times 1000}{m_{cat}}$$

Catalyst characterization

Scanning transmission electron microscopy (STEM) with high-angle annular dark field (HAADF) detection was performed on a Jeol Cold FEG NeoARM (point-to-point resolution 0.78 Å, images in Figure 1) and a Jeol 2100F (point-to-point resolution 1.1 Å, all other images), both equipped with a Cs-corrected condenser at the probe level and operated at 200 kV. For sample preparation, the powder was crushed and dispersed in ethanol through ultrasonication, dropped onto a holey carbon-coated 200 mesh Cu grid, and dried by a lamp. To avoid contamination during analysis and remove any residual carbon, the samples were Ar plasma-cleaned for 20 s (Plasma Prep 5, GaLa Instrumente). No filtering was applied on the STEM images.

NAP-XPS analysis was conducted at the CIRCE beamline at ALBA synchrotron, using a NAPP endstation designed by SPECS GmbH in collaboration with CIRCE beamline. All spectra reported here were acquired combining UHV and H₂/CO₂ environments with the sample held at RT, 200 °C, 275 °C, and 350 °C while the catalyst run at 2 mbar with a 3/1 ratio of H₂/CO₂ mixture. Each sample was previously reduced *in situ* at 400 °C under 2 mbar of H₂. The catalyst in powder form was deposited onto an Ag foil previously cleaned to reduce charge effects and for XPS calibration purposes.⁵² The spectra are all referenced to the Ag Fermi level, measured after

every spectrum, to determine absolute binding energies. A Photon energy of 400 eV was used to probe Mo 3d core-level with high photoionization cross-section under NAP conditions. Sample degradation due to X-ray radiation was not observed. NAP-XPS analysis revealed a well-resolved Mo 3d core level. Each spectrum was decomposed into a combination of Voight functions, each with an overall full-width at half maximum (FWHM) of approximately 1.6 eV.

Hydrogen-assisted temperature programmed reduction (H_2 -TPR) was performed using a U-shaped quartz reactor (internal diameter 4 mm). Prior to the TPR, the catalyst (100 mg) was pretreated under He (30 mL/min) at 250 °C (15 °C/min) for 30 min. After returning to room temperature, the catalyst was heated at 15 °C/min to 850 °C under 30 mL/min of 1% H_2 /He. The outlet gas mixture was analyzed by an Omnistar mass spectrometer from Pfeiffer Vacuum. The baseline was subtracted to the resulting H_2 signal, which is quantified using 1% H_2 /He as reference value.

Diffuse reflectance ultraviolet-visible spectroscopy (DRUV) was performed with a Perkin Elmer Lambda 45 spectrometer equipped with a deuterium-halogen illumination source and an integrated sphere (RSA-PE-20 $\varnothing$ = 200 mm). Barium sulphate (Sigma-Aldrich, 99.99%) was used as a reference and a diluting powder for samples. In a typical sample preparation, 20 mg of catalyst were diluted in 1 g of $BaSO_4$, homogenized by grinding in an agate mortar and placed in a sample holder. Reflectance measurements were converted to absorption spectra using the Kubelka-Munk function (K-M).

CO_2 temperature-programmed desorption (TPD) measurements were conducted on a custom-made apparatus using a U-glass tubular reactor loaded with 100 mg of catalyst. After an *in situ* reduction for 2 h at 450 °C (5 °C/min) under 40 mL/min of H_2 , the powder was desorbed at 450 °C under N_2 (100 mL/min) for 4 h. After cooling down to 30 °C, the catalyst was exposed to 5% CO_2 in N_2 . Then, the reactor was flushed for 30 min under N_2 before the temperature was increased from 30 °C to 450 °C (5 °C/min) to desorb CO_2 . The outlet gases

were analyzed by infrared spectroscopy and the CO₂ quantity was determined from the asymmetric stretching bands at 2450-2100 cm⁻¹ using a calibration curve.

X-ray fluorescence (XRF) analysis was performed using an Epsilon 4 spectrometer from Malvern Panalytical. The generator was used at 50 kV and 60 µA under air atmosphere. Data were collected at the Mo Kα energy level (17.44 keV) using a 3-point calibration curve verified by inductively coupled plasma – optical emission spectroscopy (ICP-OES).

The specific surface areas were determined by N₂ volumetry through a 5-points BET method using a Micrometrics ASAP 2020.

Results and discussion

The catalysts were prepared by conventional wet impregnation followed by a reductive treatment (see Experimental section). The samples, listed in Table 1, are labelled as <Mo loading in wt%>Mo/<TiO₂ material name>-R<in situ reduction temperature>. For example, 3Mo/DT51D-R450 denotes a catalyst containing 3 wt% Mo supported on TiO₂ DT51D (anatase) and reduced *in situ* at 450 °C. This reduction temperature being the default one, “R450” is often omitted in the following. XRF measurements (Table 1) show that the Mo loadings were found close to the target values (0.1 to 10 wt%, standard loading 3 wt%) within a relative accuracy of 20%.

Table 1 – Characteristics of the as-prepared Mo/TiO₂ catalysts used in this study.

Sample name	Specific surface area (m ² /g) ^a	TiO ₂ phase composition (anatase/rutile) ^b	Mo loading (wt%) ^c
0.1Mo/DT51D	78	100%/0%	0.1
0.3Mo/DT51D			0.2
1Mo/DT51D			1.0
3Mo/DT51D			2.9
10Mo/DT51D			8.3
3Mo/PC500	148	100%/0%	3.4
3Mo/P90	105	90%/10%	3.3
3Mo/P25	61	80%/20%	2.8
3Mo/RL11A	12	0%/100%	2.6
1Mo/RNR	44	0%/100%	1.0
3Mo/RNR			2.9

^a Determined by N₂ volumetry through the BET method; ^b Supplier mass fraction values, except for RNR: determined from X-ray diffraction; ^c Determined by XRF spectroscopy (standard deviation 0.05 wt%).

Figure 1 displays representative STEM-HAADF micrographs of 3Mo/DT51D and 3Mo/RNR samples. The images suggest that Mo is atomically dispersed at the surface of TiO₂, i.e. it is present as a mixture of single-atoms and subnanometric clusters. The latter correspond to 2D oxomolybdate clusters, as previously reported in the literature.^{45,53–55} STEM micrographs of the other 3 wt% Mo/TiO₂ catalysts (Figure S1) show a similarly high dispersion of Mo. The color maps in Figures 1C and 1F highlight the relative intensities within the 2 nm² yellow squares represented in Figures 1B and 1E for anatase and rutile, respectively. Along these two imaging orientations, Mo atoms are seen to preferentially locate at the edges or within the dense layers of the titania lattice for both anatase and rutile. This is consistent with previous experimental and theoretical works on the epitaxial growth of Mo or MoO_x clusters or layers on anatase (101) or rutile (110) titania.^{54–58}

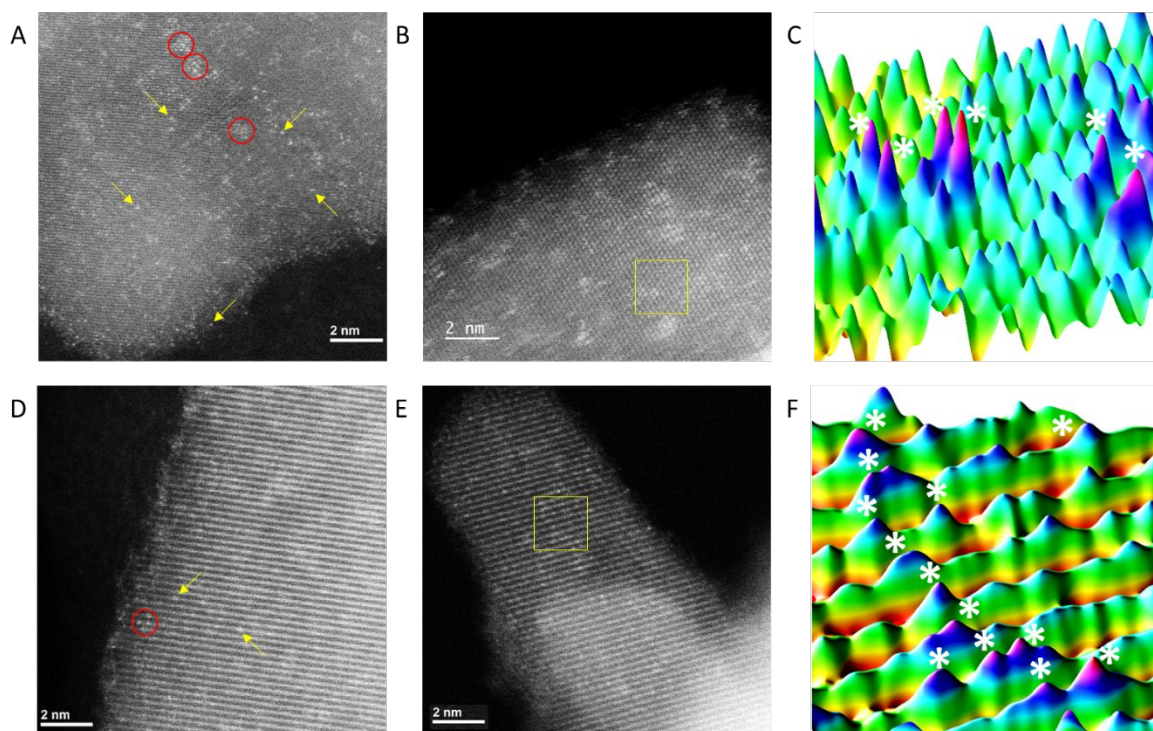


Figure 1 - Representative aberration-corrected STEM-HAADF micrographs. A, B: 3Mo/DT51D; D, E: 3Mo/RNR. Arrows and circles in A and D show single Mo atoms and Mo clusters, respectively. C, F: Color-map representation of the intensity in the 2 nm² yellow square represented in B and E, respectively. The white stars indicate the Mo atoms.

A summary of catalytic properties for the whole set of samples is presented in Table 2. In order to compare the different materials, conversion, selectivity as well as methanol TOF and STY were determined as described in the Experimental section.

Table 2 - CO₂ hydrogenation performances of Mo/TiO₂ samples at 275 °C under 30 bar of H₂/CO₂/N₂ (3/1/1), GHSV = 7500mL.g⁻¹.h⁻¹.

Sample ^a	CO ₂ conversion (%)	CH ₄ selectivity (%) ^b	MeOH selectivity (%) ^b	DME selectivity (%) ^b	MeOH TOF (mol _{MeOH} . mol _{Mo} ⁻¹ .h ⁻¹)	MeOH STY (g _{MeOH} . kg _{cat} ⁻¹ .h ⁻¹)
DT51D	0.2	-	-	-	-	-
0.1Mo/DT51D	0.9	5.2	4.8	4.8	2.81	0.94
0.3Mo/DT51D	3.0	5.9	5.1	2.5	3.20	3.20
1Mo/DT51D	5.2	12.0	10.2	3.2	3.57	11.31
3Mo/DT51D as prepared	1.7	5.1	23.3	5.9	0.88	8.22
3Mo/DT51D	4.8	8.7	6.6	3.2	0.71	6.84
3Mo/DT51D -R600	10.8	6.1	5.7	1.6	1.33	12.89
3Mo/DT51D -R700	3.8	3.2	15.1	0.7	1.24	12.00
10Mo/DT51D	3.3	9.5	4.9	2.2	0.12	3.41
3Mo/PC500	< 0.1	-	-	-	-	-
3Mo/P90	4.0	10.5	3.7	1.0	0.28	3.09
3Mo/P25	2.6	10.0	5.4	3.1	0.32	3.01
3Mo/RL11A	1.5	4.4	17.8	0	0.57	5.68
1Mo/RNR	7.6	23.1	10.5	1.1	5.16	16.87
3Mo/RNR	6.8	9.3	24.2	1.3	3.61	34.95
50Cu/ZnO/ Al ₂ O ₃	20.7	0	32.3	0	0.56	141.06

^a The samples were prereduced in situ at 450 °C, except when mentioned otherwise; ^b CO represents the complement to 100%.

From these data, it appears that titania supports without Mo are inactive whereas all the samples with Mo are active for CO₂ hydrogenation, except Mo/PC500 for which the support collapsed upon the catalyst preparation (specific surface area of 150 m²/g instead of 350 m²/g initially). The main product is always CO (along with water, which cannot be accurately

quantified), followed by methane or methanol depending on the support oxide, then dimethyl ether (DME). Thus, the main reaction pathway on molybdenum-based catalysts remains CO₂ reduction to CO through the reverse water-gas shift reaction as described by several groups using molybdenum carbide, MoO_x/Ti₃AlC₂ or molybdenum doping Fe/Al₂O₃ and Cu/FAU.^{59–63}

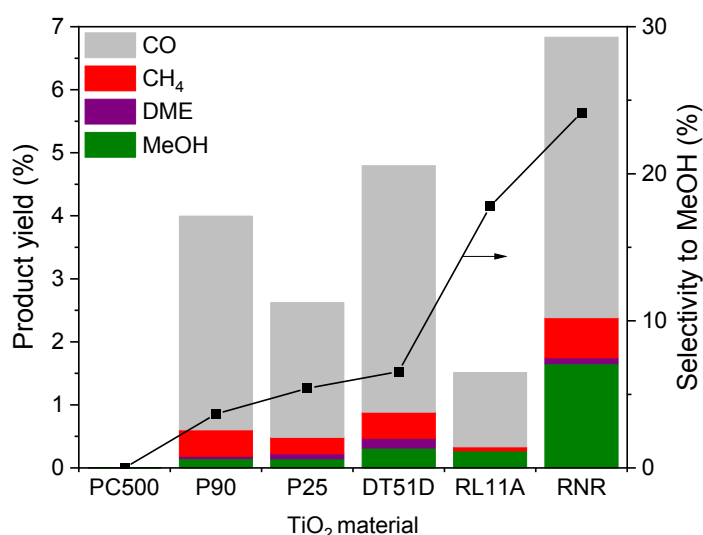


Figure 2 - Effect of TiO₂ nature on product yields and methanol selectivity for 3Mo/TiO₂ catalysts at 275 °C under 30 bar of

H₂/CO₂/N₂ (3/1/1), GHSV = 7500 mL.g⁻¹.h⁻¹.

Figure 2 allows comparing the titania supports in terms of CO₂ hydrogenation activity and selectivity to methanol at a constant Mo loading of 3 wt%. The CO₂ conversion at 275 °C varies from less than 0.1% for PC500 to 6.8% for RNR. The products distribution also strongly depends on the TiO₂ nature. In particular, the selectivity to methanol ranges from 3.7% for P90 to 24.2% for RNR. As a result, the STY reaches 35 g of methanol per kg of catalyst per hour, versus 141 g_{MeOH}.kg_{cat}⁻¹.h⁻¹ for the highly Cu-loaded (50 wt%) Cu/ZnO/Al₂O₃ commercial methanol-synthesis catalyst evaluated in the same conditions (Figure S2).

The results of typical experiments at variable temperature are reported in Figure S3 for 3Mo/RNR and 3Mo/DT51D, the two most active systems. CO₂ conversion as well as selectivities to CH₄ and CO increase with the temperature, whereas the selectivity to methanol decreases.

While the 3Mo/RNR catalyst reaches a methanol selectivity of 50% at 200 °C, a maximum of 23 % is obtained at 220 °C on 3Mo/DT51D, with CO as the main by-product for the two catalysts. These two catalysts exhibit stable catalytic performance for 40 h (Figure S4).

Notably, these performances correlate neither with the specific surface area of TiO₂ (Figure S5), nor with the titania phase composition as anatase-pure DT51D and rutile-pure RNR are the supports that promote the highest activities. A same TiO₂ phase can be synthesized by different preparation methods – including sol-gel methods, hydrothermal treatments (RNR), and flame pyrolysis (P25, P90) – that produce crystalline powders with substantially different exposed facets with different reactivities.⁶⁴

Synchrotron-based NAP-XPS was performed to tentatively clarify the atomic origins of the support-dependent performances in terms of Mo oxidation state. The experiments were carried out on 3Mo/RNR, 3Mo/P25, and 3Mo/DT51D under conditions of *in situ* reduction (H₂, 400 °C) and reaction (75 vol% H₂ + 25 vol% CO₂, 200-350 °C) at 2 mbar total pressure. As an example, Figure 3A shows Mo 3d core-level spectra for 3Mo/DT51D and 3Mo/RNR under H₂-CO₂ mixture at 275 °C. The XPS results obtained for all the samples and conditions are presented in Figure S6 and Table S1, and synthesized in Figure 3B. A clear impact of the nature of the TiO₂ support on the Mo oxidation states distribution is observed. As a matter of fact, Mo is more reduced on rutile (RNR) than on anatase (DT51D), the dominant states being Mo^V and Mo^{VI}, respectively. Mixed-phase P25 exhibits an intermediate Mo^V/Mo^{VI} ratio. Whereas the state of Mo on DT51D hardly changes, an overall oxidation of Mo occurs on RNR and P25 when switching from reduction to reaction conditions. This is ascribed to CO₂ and/or H₂O acting as oxidizing agents,^{65–67} and to the more labile oxygen environment of Mo on rutile than on anatase, which may relate to the higher reducibility of the rutile surface with respect to anatase.⁶⁸ Under NAP-XPS reaction conditions, Mo/RNR is the only catalyst containing Mo^{IV} species. The latter may be at the origin of the significant methanol production activity exhibited by Mo/RNR. However, the oxidation state of Mo/P25 comprised between those of DT51D and

RNR counterparts though its catalytic performance is the lowest (Figure 2). Moreover, the NAP-XPS pressure conditions (2 mbar total pressure in all cases) are obviously not representative of those employed in the laboratory catalytic reactor (1 bar of H_2 for reduction, and 18 bar H_2 + 6 bar CO_2 for reaction). Thus, the measured Mo state differences between the supports should be considered qualitatively, and they are not sufficient to explain the catalytic data.

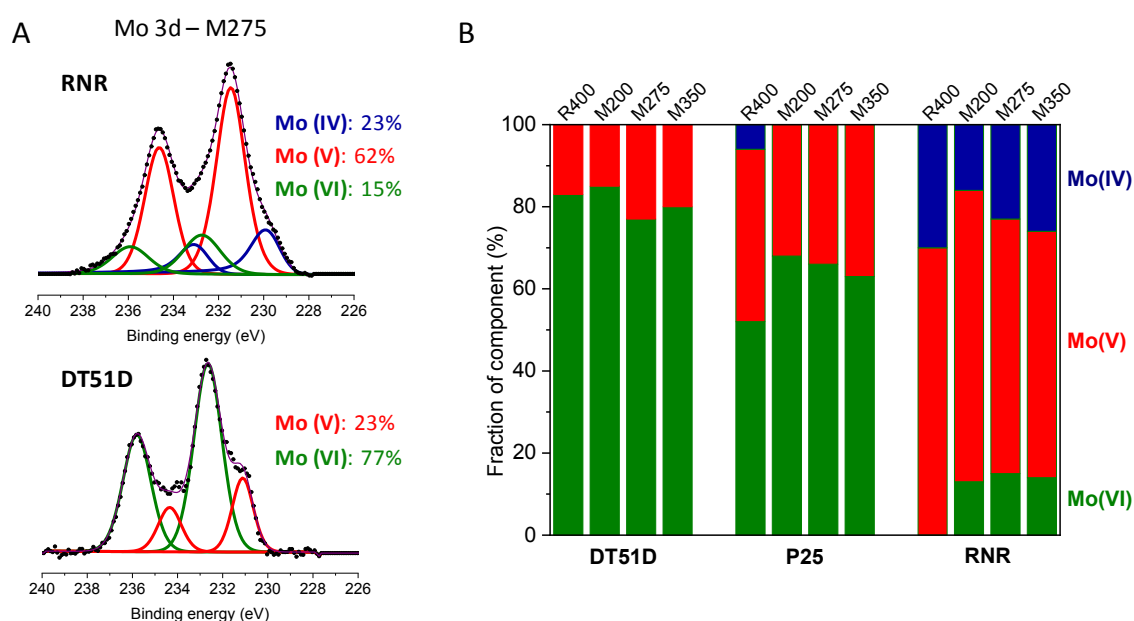


Figure 3 – A: Mo 3d NAP-XPS analysis at 275 °C under 2 mbar of a 3/1 H_2/CO_2 mixture on 3Mo/RNR (top) and 3Mo/DT51D (bottom). B: Mo oxidation state distribution in 3 wt% Mo supported on DT51D, P25 and RNR TiO_2 determined from NAP-XPS (Mo 3d), during in situ reduction at 400 °C (R400), and exposure to CO_2/H_2 reactant mixture (3/1) at 200 °C (M200), 275 °C (M275) and 350 °C (M350).

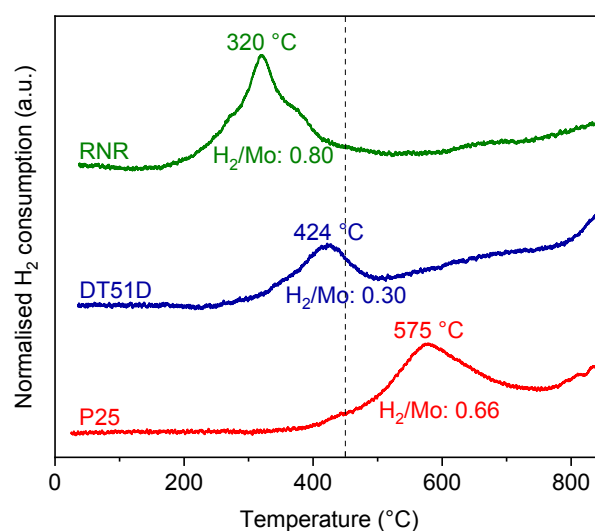


Figure 4 – H_2 -TPR profiles for 3 wt% Mo supported on RNR, DT51D and P25 titania. The temperatures of maximum consumption and the H_2 -to-Mo molar ratios, i.e. area of the TPR peak normalised over the amount of Mo, are indicated. The temperature of in situ reduction pretreatment employed for catalytic tests (450 °C) is displayed with a vertical dotted line.

In order to gain insight into the reducibility of molybdenum on these three TiO_2 supports, H_2 -TPR experiments were carried out, as shown in Figure 4. Two types of hydrogen consumption features can be distinguished: a fast main one identifiable by a TPR peak, and a slower and continuous one at higher temperature. Regarding the main feature, on the one hand the amount of H_2 consumed per Mo atom increases with the fraction of rutile phase (i.e. from DT51D to RNR), consistently with the NAP-XPS data showing the lowest overall oxidation state for Mo on RNR. On the other hand, the TPR peak position varies from 320 °C to 424 °C and 575 °C for RNR, DT51D and P25, respectively. This peak can be assigned to the reduction of well-dispersed octahedral Mo^{VI} species.^{69–71} The last reduction event occurring above 800 °C for anatase-containing samples can be attributed to tetrahedral Mo^{VI} species.⁷² As no significant H_2 consumption was observed for the bare supports, the continuous TPR feature occurring after the main reduction event can be explained by the slow reduction of polymeric oxomolybdate species.⁷⁰ In addition, molybdenum species can promote the partial reduction

of titanium to Ti^{3+} in the near-surface region,⁷³ and the structural similarity of rutile TiO_2 and MoO_2 phases may maximize their interaction.

Overall, key factors for methanol productivity may not only be the lower Mo oxidation state (XPS) but also its higher reducibility at low temperature (TPR), both depending on the nature of the TiO_2 surface and being favored on RNR.

In an attempt to better understand the influence of the Mo oxidation state on the catalytic performance, the effect of the *in situ* reduction temperature (450-700 °C) was investigated for 3Mo/DT51D. Figure S7 shows that the catalyst is already slightly active in the absence of *in situ* pretreatment. After *in situ* reduction at 450 °C, CO_2 conversion is much higher, and it presents a maximum after treatment at 600 °C. However, the selectivity to methanol shows an opposite behavior, i.e. a minimum for the R600 sample. The increase in conversion being superior to the decrease in selectivity, the methanol TOF (1.4 h^{-1}) is maximal after reduction at 600 °C. As shown by the STEM images in Figure S8, 3Mo/DT51D seems structurally stable at 450 °C, with no obvious effect of the *in situ* treatment on Mo dispersion. However, Mo sintering occurred for the R600 sample, as revealed by the presence of MoO_x nanoparticles of $2.0 \pm 0.5 \text{ nm}$ in size. The stability of these particles, even after re-exposure to ambient air, can be related to the epitaxial growth of the partially reduced Mo oxide on TiO_2 .^{54–58} This sintering could lead to a change of active site from the MoO_x - TiO_2 interface to the MoO_x surface. A reducing treatment at 700 °C induces the formation of even larger MoO_x particles ($2.7 \pm 0.5 \text{ nm}$) and the sintering of titania (Figure S9), which loses part of its specific surface area (from $78 \text{ m}^2/\text{g}$ for R450 catalysts to 58 and $20 \text{ m}^2/\text{g}$ for their R600 et R700 counterparts, respectively). These phenomena could explain the significant drop in activity after treatment at 700 °C.⁷⁴ Overall, these results indicate that the formation of stable nanoparticles with a lower oxidation state of Mo is favorable to the CO_2 conversion rate, but not to methanol selectivity. Note that this observation as well as the heterogeneity of the dispersed Mo phase induced by reducing

pretreatments at temperatures higher than 500 °C led us to select 450 °C as the standard prereduction temperature for all catalysts.

Finally, the impact of the Mo loading (0.1-10 wt%) on the catalytic performance was investigated for Mo/DT51D-R450. The STEM images in Figure 5A show that Mo remains well-dispersed on titania without the formation of stable 3D nanoparticles even at high coverage, though Mo oxide clusters (polymeric oxomolybdates) gradually replace single Mo atoms (monomeric oxomolybdates) as the Mo coverage increases. At 10 wt% Mo, the cluster size determined from STEM is 0.8 ± 0.2 nm. In the literature, polymeric^{75–80} and monomeric^{81–84} oxomolybdate species are described as the most active species depending on the studies. DRUV spectroscopy was performed to further characterise molybdate species in catalysts with different loadings. The two contributions of TiO₂ centred at *ca.* 255 and 310 nm are clearly observable in Figure S10. A close view of the 350-800 nm range (Figure 5B) reveals two broad contributions associated with oxomolybdates species. While the one located in the 400-500 nm range (explaining the yellow colour of the samples) for all catalysts corresponds to Mo⁶⁺, the contribution above 550 nm (blue colour) for highly loaded catalysts is attributed to Mo⁵⁺.⁸⁵ Moreover, Mo⁵⁺ can be associated to polymolybdates.^{86,87} Thus, consistently with STEM, the low-loaded catalysts (< 3 wt% Mo) are covered with ultradispersed oxomolybdate species, whereas the highly loaded catalysts (> 3 wt% Mo) also exhibit larger Mo oxide clusters. The 3Mo/DT51D sample shows an intermediate state. In addition, 3Mo/P25 and 3Mo/RNR catalysts behave similarly as 3Mo/DT51D, as shown by Figure S11.

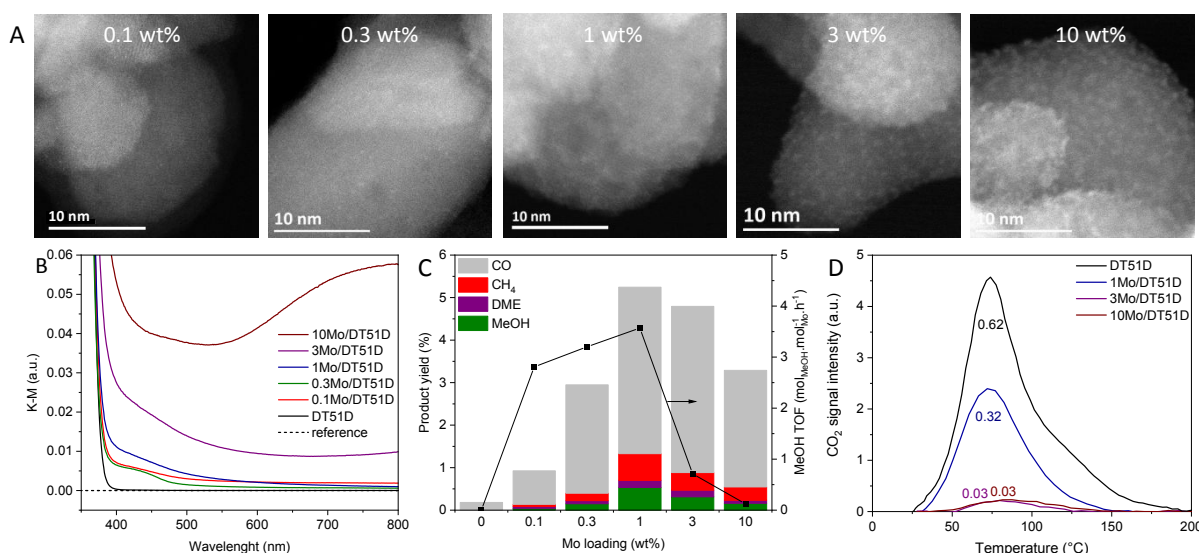


Figure 5 - A: Representative aberration-corrected STEM-HAADF micrographs of 0.1-10 wt% Mo/DT51D catalysts. B: Diffuse reflectance UV-vis spectra of 0-10 wt% Mo/DT51D samples in the 350-800 nm range. C: Effect of Mo loading on CO/MeOH/CH₄/DME yields and methanol STY for 0-10 wt% Mo/DT51D-R450 at 275 °C under 30 bar of H₂/CO₂/N₂ (3/1/1), GHSV = 7500 mL.g⁻¹.h⁻¹. D: CO₂-TPD profiles for 100 mg of 0-10 wt% Mo/DT51D samples. The total amount of desorbed CO₂ in $\mu\text{mol}/\text{m}^2$ is indicated.

Figure 5C shows an optimum in CO₂ conversion (5.2%) and methanol selectivity (10.2%) for 1 wt% Mo at 275 °C. This corresponds to a maximal methanol TOF of 3.6 h⁻¹. The decrease in CO₂ conversion below 1 wt% Mo is ascribed to a limiting number of active sites. However, the MeOH TOF remains nearly stable in the 0.1-1 wt% Mo loading range. This is assigned to the presence of mainly isolated oxomolybdate species on these three catalysts, which is in accordance with the DRUV spectra. Note also that in this “single atom” state, the length of the MoO_x-TiO₂ interface accessible to reactants is maximized. As the coverage increases and polymeric oxomolybdates form, some Mo atoms are no longer in contact with the accessible surface of titania. Thus, dual MoO_x-TiO₂ sites may be essential to methanol productivity, as the Cu-ZnO sites are for the classical Cu/ZnO/Al₂O₃ methanol-synthesis catalyst.⁸⁸

The CO₂-TPD curves in Figure 5D show that the amount of CO₂ – adsorbed on the catalyst at RT and desorbed in the RT-450 °C range – decreases as the Mo loading increases, and vanishes to almost zero for 3 wt% Mo and above. Consistently with the previous hypothesis, we attribute

the impact of the Mo loading on the catalytic properties to a balance between the number of basic sites on TiO_2 available for CO_2 adsorption⁸⁹ and that of Mo centers enabling H_2 activation and CO_2 conversion at the exposed $\text{MoO}_x\text{-TiO}_2$ interface. A similar methanol activity tendency is observed for Mo/RNR with a MeOH TOF at 275 °C reaching 5.2 h^{-1} for the 1 wt% Mo catalyst (Figure S12). Again, we ascribe this behavior to the higher methanol production performance of isolated oxomolybdate species.

Conclusion

In conclusion, we have demonstrated the possibility to obtain efficient catalysts based on titania-supported ultradispersed molybdenum species for CO_2 hydrogenation, here performed under gas-phase conditions at 3 MPa. The main products are CO, methane and methanol. The TiO_2 support type, as well as the Mo loading and the reductive pretreatment temperature, substantially impact the catalytic activity and selectivity.

From a combination of characterization techniques such as aberration-corrected STEM, NAP-XPS, DRUV and temperature-programmed methods, we reach the following conclusions. A low Mo coverage corresponding to ca. 1 wt% Mo provides an optimal compromise, in terms of methanol yield, between the number of active sites and their isolation. The most active sites for methanol production are associated to Mo oxo species, either isolated on titania or located at the periphery of polymolybdate clusters. In these dual $\text{MoO}_x\text{-TiO}_2$ sites, molybdenum ideally exhibits labile and partial oxidation states – possibly Mo^{IV} . The presence of these sites appears to strongly depend on the titania surface structure. The highest performance was measured for a titania support consisting of rutile nanorods, with a methanol STY of $35 \text{ g}_{\text{MeOH}} \cdot \text{kg}_{\text{cat}}^{-1} \cdot \text{h}^{-1}$ at 275 °C.

Forthcoming studies on the Mo/ TiO_2 system will rely on advanced *operando* investigations and theoretical modelling, with the aim of understanding how the Mo atom coordination and oxidation state, as well as the titania surface structure and acid-base properties (including the

presence of TiO₂ vacancies^{90,91}), affect the catalytic properties. A better knowledge of the structure-function relationships will enable further improvement of the catalysts reported herein.

Authors contributions

LP conceptualized the study, acquired the funding, and managed the project; TL and NP prepared the catalysts; TL carried out routine materials characterization, temperature-programmed experiments, and catalytic tests; MB, OE, and YL performed the STEM analyses; LC, IJVG, VPD and JL performed the NAP-XPS experiments; LC analysed the NAP-XPS data; EP performed the DRUV experiments and analysed the data; PA prepared the TiO₂ RNRs; RC set up the catalytic bench; LP, FM, PA and NP supervised the PhD thesis of TL; TL, LP and FM wrote the original draft; All the authors reviewed the paper.

Conflicts of interest

There are no conflicts of interest to declare.

Acknowledgment

A. Nassereddine (IRCELYON) is acknowledged for preliminary catalysis experiments. Y. Lefkir & S. Reynaud (Laboratoire Hubert Curien) and M. Aouine (IRCELYON) are acknowledged for their support in STEM analysis. CLYM is acknowledged for access to the FEI Titan and Jeol NeoARM microscopes. N. Bonnet & P. Mascunan (IRCELYON) are acknowledged for XRF and BET analyses. Agence Nationale de la Recherche (UltraCat project, ANR-17-CE06-0008) is acknowledged for financial support. JL is a Serra Húnter Fellow and is grateful to the ICREA Academia program and projects MICINN/FEDER RTI2018-093996-B-C31 and GC 2017 SGR 128.

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