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Hydrogen as a fuel additive in laminar premixed methane flames: Impact on the nucleation and growth of soot particles

Hong-Quan Do, Alessandro Faccineto, Luc-Sy Tran, Pascale Desgroux, Laurent Gasnot,
Abderrahman El Bakali*, Xavier Mercier*

*Univ. Lille, CNRS, UMR 8522 - PC2A - Physicochimie des Processus de Combustion
et de l'Atmosphère, F-59000 Lille, France*

Full-Length Article

Supplemental Material (SM) is available:

SM1: Additional information (PDF file)

SM2: Experimental data (Excel file)

* Corresponding authors:

Prof. Dr. Abderrahman El Bakali

Email: abderrahman.el-bakali@univ-lille.fr

Dr. Xavier Mercier

Email: xavier.mercier@univ-lille.fr

Abstract:

This work reports new experimental data regarding the impact of H₂ on slightly sooting methane flames ($\Phi=1.91$) characterized by the formation of soot particles undergoing growth processes. This study has been carried out in three atmospheric sooting premixed methane flames with added H₂ (2% of the total flowrate) or substituted (10% molar comparing to CH₄ fuel).

The mole fraction profiles of selected aliphatic and aromatic compounds (C₁-C₁₆) have been measured by Gas Chromatography and Jet-Cooled Laser-Induced Fluorescence. Concerning the soot particles, we have implemented for the first time an analytical methodology based on in-situ measurements by Laser-induced Incandescence and Cavity Ring-Down Spectroscopy coupled with ex-situ measurements by Scanning Mobility Particle Sizing (SMPS). This original approach allows to determine the soot volume fraction profiles and corresponding evolution of the particle number densities and particles size density function without requiring accurate knowledge of the dilution ratio during SMSP measurements.

The reported data highlight that the introduction of H₂ strongly influences the formation of aromatic species and soot depending on the operating conditions (H₂ addition or substitution). The impact of H₂ was evaluated on the nucleation step and the soot growth processes. In that context, we notably show that the H₂ substitution inhibits while the H₂ addition favors the formation of nascent soot particles, and furthermore the H₂ addition generates substantial modifications in the dynamic of the soot growth processes. This work also supports the idea that the onset of the particle nucleation might be controlled by specific concentration thresholds of aromatic precursors.

Keywords: soot, hydrogen, polycyclic aromatic hydrocarbons (PAHs), soot growth, premixed flame

1. Introduction

Reducing the emissions of soot and gaseous pollutants from the combustion of conventional hydrocarbon fuels is an ongoing challenge. Hydrogen (H_2) is well-known as a zero-carbon energy carrier with low ignition energy and high burning velocity [1–3]. However, the use of H_2 alone in real industrial systems is not yet optimal due to certain inherent handling difficulties and the necessary adaptations of industrial processes. Major safety issues arise from the wide flammability range and low ignition energy of H_2 [4–6]. In this context, H_2 -hydrocarbon blends, which are easier to implement in real combustion systems, have received increased attention due to different positive aspects notably related to their increased combustion efficiency and propensity to reduce soot and gaseous pollutant emissions. The local flame extinction, combustion stability and power output of CH_4 combustion have all been shown to be improved by H_2 enrichment [7,8], and the addition of small amounts of H_2 to methane has been demonstrated to increase the performances of gas powered spark-ignited engines [9]. Moreover, the presence of H_2 in synthetic natural gas flame has been shown to inhibit the formation of CO and CO_2 [10].

The impact of H_2 on the formation of soot precursors and soot particles has also been the subject of numerous experimental and modeling studies [11–35]. Regarding soot precursors, the impact of added H_2 (40% in CH_4) in a methane laminar premixed sooting flame (equivalence ratio relative to CH_4 $\Phi_C=2.2$) has notably been shown to enhance the formation of aliphatic C_1 - C_4 species as well as benzene and toluene [29]. Ezenwajiaku et al. [28] experimentally studied the impact of H_2 (20% in CH_4) on the formation of polycyclic aromatic hydrocarbons (PAHs) in a diffusion flame and concluded that H_2 addition to fuel decreased their concentration.

Haynes et al. [25] found that H_2 addition (3% of total flame flowrate) to an ethylene flame operating at the soot inception C/O ratio promoted the formation of nascent soot. By

contrast, Liu et al. [30] and Xu et al. [31] investigated the effect of H₂ addition (up to 40% comparing to the base fuel) on soot formation in methane diffusion flames and found that the addition of H₂ in these cases strongly decreased the soot volume fraction. This tendency to decreasing the soot volume fraction in flames when adding amounts of H₂ (from 10 up to 50% H₂/fuel) has been observed in numerous works investigating flames stabilized with various fuels as ethane, ethylene, propane, butane [15,17,21,22,24,36,37].

Besides, De Iuliis et al. showed that the introduction of H₂ in an ethylene/air premixed flame [24] by a substitution procedure slowed down the soot growth process due to the decrease of the H/H₂ ratio. Choi et al. [16] investigated the effect of H₂ addition on the micro- and nano-structure of soot particles in an ethylene/air counter-diffusion flame. They highlighted that H₂ addition decreased the size of the soot microstructures and enhanced the formation of PAHs containing 5 carbon atom rings that induce the curvatures into the carbon lamella.

The effect of H₂ on the number density of soot particles has also been investigated in literature. Tesner et al. [14] found that H₂ addition (30% comparing to fuel) to a methane diffusion flame increased the number density of soot particles. Zhao et al. [22] mentioned that H₂ addition (20% comparing to fuel) and H₂ substitution (25% of ethylene by H₂) to an ethylene laminar diffusion flame decreased the number density of soot particles by 23% and 66% respectively, comparing to the reference flame. However, the H₂ effect was not only due to the dilution and chemical inhibition but also to the reduced number of carbon atoms in the initial mixture.

Hence, at the state of the art, the literature shows that the introduction of H₂ into sooting flames enhances or inhibits the formation of soot particles and their precursors depending on the operating conditions. We recently also showed that the introduction of H₂ in a nucleation methane flame ($\Phi_C=1.82$), i.e. a flame generating only nascent soot particles [32], drastically reduced or enhanced the formation of aromatic species and the soot volume fraction, depending

on the way of introducing H₂ (either by addition or substitution to the diluent). However, these flames did not allow studying the soot growth process and the impact of H₂ on the soot particles distribution and soot number density.

In the present work, as part of a continuing effort to improve the understanding of the impact of H₂ on soot formation, we investigated the impact of H₂ on a slightly richer methane flame ($\Phi_C=1.91$) characterized by the formation of soot particles undergoing growth processes. As demonstrated by [38], both nucleation and growth process happen simultaneously under fuel-rich flame conditions. These richer operating conditions allowed us to examine the effect of H₂ on both the nucleation and growth processes.

Similarly to our previous work [32], we employed two different approaches to introduce H₂ to the reference methane flame, consisting either in keeping constant (H₂ substitution) or slightly increasing (H₂ addition) the total gas flow rate. We implemented a large panel of experimental methods to record the most complete set of experimental data to gather information on the role of H₂ on these two specific soot formation steps. Hence, we measured the mole fraction profiles of gaseous species including selected aliphatic and aromatic compounds (C₁-C₁₆) in the different flames. Moreover, we determined the soot volume fraction profiles as well as the corresponding evolution of the soot particle size distribution and number density using a combination of complementary highly sensitive analytical tools. To this aim, we developed a new analytical method based on the coupling of laser induced incandescence (LII), cavity ring-down spectroscopy (CRDS) and scanning mobility particle sizing (SMPS) to determine the soot number density from the soot volume fraction and soot particle size distribution measured in the flame.

2. Experiment methods

2.1. Burner and flame conditions

Three atmospheric methane premixed flames were stabilized on a water-cooled McKenna burner equipped with a bronze porous disk (6 cm diameter). The system was already described previously [32]. In the present study, the water in the cooling circuit was kept at 296 K and a shield nitrogen flow, introduced in the co-annular section of the porous disk, was set to 1440 NLPH (normal liter per hour) to prevent perturbations induced by the surrounding air.

As recently reported for nucleation flames [32], two different approaches have been used to introduce H₂ into the reference methane flame, consisting on either keeping constant or slightly increasing the total gas flow rate. The first method consisted of replacing a small amount of dilution nitrogen, equal to 10% of CH₄ flow rate with H₂, hence preserving a total constant flowrate. The corresponding flame is denoted Φ -1.91_H₂-S. The second method consisted of adding the same amount of H₂ directly to the cold gas supply, therefore leading to a slight increase (around 2%) of the total flowrate compared to the reference flame. The corresponding flame is denoted Φ -1.91_H₂-A. The introduction of such a small quantity of H₂ (< 2%) strongly limits its impact on the flame temperature which is an essential parameter in the soot particle formation processes. The experimental conditions of the flames are reported in Table 1.

	Flame		
	Φ -1.91	Φ -1.91_H ₂ -S	Φ -1.91_H ₂ -A
Φ_C	1.91	1.91	1.91
Φ_{C+H}	1.91	1.96	1.96
C/O	0.479	0.479	0.479
Total flow rate (NLPH)	690.6	690.1	704.5
x_{CH_4}	0.202	0.202	0.198
x_{O_2}	0.211	0.211	0.207
x_{N_2}	0.587	0.567	0.575
x_{H_2}	0	0.020	0.020
$T_{adiabatic}$ (K)	1806	1806	1787
$T_{uncorrected}$ (K)	1552	1569	1543
Flame velocities at 298 K and 1 atm (cm/s)	9.1	9.9	9.2

Table 1. Experimental conditions. Flame name: Φ -1.91: CH₄ flame; Φ -1.91_H₂-S: CH₄ substituted-H₂ flame; Φ -1.91_H₂-A: CH₄ added-H₂ flame. $T_{adiabatic}$: adiabatic temperature calculated using GASEQ program [39]. $T_{uncorrected}$: measured temperature by using a type B thermocouple without radiative heat loss correction. Flame velocities have been calculated using the GRI mechanism [40]. $\Phi_C = 2 x_{CH_4} / x_{O_2}$ and $\Phi_{C+H} = 2 x_{CH_4} / x_{O_2} + 0.5 x_{H_2} / x_{O_2}$

2.2. Experimental setup

In this work, several experiments were implemented to measure the flame temperature, the mole fraction profiles of combustion products (CO, CO₂, H₂, H₂O), aliphatic species (C₁-C₆), benzene, naphthalene, pyrene, soot volume fractions, number density of particles as well as particles size density functions (PSDFs) along the flame height.

2.2.1. Flame temperature measurement

The temperature profiles of the three studied flames were measured with a Pt/Rh(6%)-Pt/Rh(30%) type B thermocouple (diameter 100 μ m) along the centerline of the flame as a function of the height above the burner (HAB) from 0 mm to 16 mm. The thermocouple was coated with a ceramic layer of BeO-Y₂O₃ to reduce catalytic effects [41]. As the main objective of this measure was only to check whether the temperature profile was modified by the H₂

addition/substitution, no specific correction has been applied to the reported temperature profiles.

2.2.2. Measurement of gaseous species by GC, JCLIF and FTIR

The gaseous species formed in the sooting flames were extracted by a quartz sampling microprobe (350 μm orifice). As described in our previous work [32], gas chromatography (GC) was used to identify and quantify CO, H₂, aliphatic species and benzene. The uncertainty on the mole fraction of gaseous species measured by GC in this study is estimated to be < 5% for major species and < 10% for minor species. Naphthalene and pyrene concentration profiles were determined by jet cooled laser induced fluorescence (JCLIF) while CO₂ and H₂O were measured by Fourier-transform infrared spectroscopy (FTIR). The measurement uncertainty on all these species was estimated < 13%. The C, O and H atomic balances of the three studied flames were found to be close to 100% as detailed in Table S1 of the Supplemental Material 1 (SM1).

2.2.3. Determination of the soot volume fraction profiles by LII and CRDS

Soot volume fraction profiles were determined by laser induced incandescence (LII) measurements calibrated by cavity ring-down spectroscopy (CRDS) according to a procedure already described in previous papers from our group [32,42]. The same method has been employed and adapted to the present work. Hence, only the main details of the setup will be given here.

CRDS experiments were performed by using a Nd:YAG laser (Quantel) generating a laser pulse at 1064 nm. The cavity we used consisted of two identical 25-mm-diameter plano-concave mirrors (radius of curvature: 25 cm) coated to achieve a high reflectivity of $R = 99.96\%$ at 1064nm. The mirrors were separated by distance of 40 cm. The burner was

placed at the central position between these two mirrors. A laser pulse was injected inside the cavity with a specific optical system constituted of two lenses and a pinhole in order to preferentially match the TEM₀₀ modes of the cavity. The ring-down time characterizing the lifetime of the laser pulse inside the cavity was recorded thanks to a photomultiplier Hamamatsu R2257 (PMT). A longpass filter (RG-780) was placed in front of the PMT to limit the parasite light due to the flame emission. The lifetime of the laser pulse was then transformed into an extinction value according to a procedure already described elsewhere [32,42]. The measured extinction coefficient $K_{\text{ext}} = K_{\text{abs}} + K_{\text{sca}}$ (K_{abs} and K_{sca} being respectively the absorption and the scattering coefficients) was assumed to be equal to K_{abs} (K_{sca} being negligible).

LII experiments were also carried out by using 1064 nm laser excitation wavelength generating by the same laser used for CRDS experiments. The laser beam was expanded into a collimated horizontal plane using a specific optical system described in details in [32] to provide a top-hat irradiance profile at the position of the LII collection volume. The LII signal was collected at right angle of the laser axis by a system of lenses and a Hamamatsu R2257 PMT positioned behind an entrance slit (0.6 mm vertical \times 6 mm horizontal) and an interference filter centered at 532 ± 10 nm in order to limit parasite emission and scattering light from the flame. The LII signals recorded by the PMT were acquired and digitized by an oscilloscope Lecroy HDO - 4104A.

Basically, LII signals can be defined according to *Eq.1*:

$$S_{\text{LII}}(\lambda_{\text{em}}, T_p(t)) = E(m) \frac{48\pi^2 hc^2}{\lambda_{\text{em}}^6} \left[\exp\left(\frac{hc}{\lambda_{\text{em}} \cdot k_b \cdot T_p(t)}\right) - 1 \right]^{-1} f_v(t) \quad \text{Eq.1}$$

where $E(m)$ is the absorption function of the particles, T_p the temperature of the heated soot by the laser pulse, c the speed of light in vacuum, λ_{em} the emission wavelength, k_b the Boltzmann constant, h the Planck constant and f_v the soot volume fraction.

This equation shows a dependence on $E(m)$ and to T_p . In order to determine the LII profiles representative of the evolution of f_v , it is therefore important to consider the evolution of the value of $E(m)$ as well as the heated temperature T_p along the flame height. To this aim, we first determined the fluence curves characterizing the response of the LII signal to laser energy against the HAB in all studied flames. These fluence curves are reported in Fig.1.

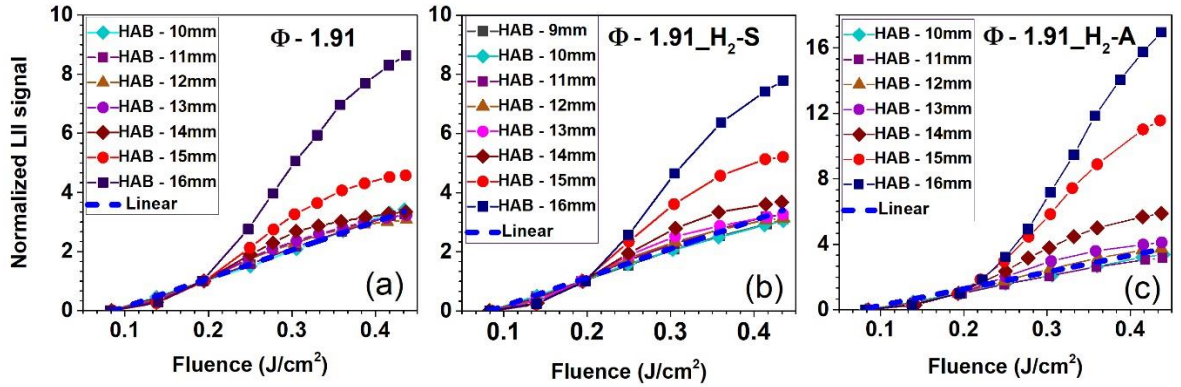


Fig.1: Normalized fluence curves at 0.2 J/cm² obtained in three studied flames. Φ -1.91: CH₄ sooting reference flame; Φ -1.91_H₂-S: CH₄ substituted-H₂ flame; Φ -1.91_H₂-A: CH₄ added-H₂ flame.

We arbitrary chose to normalize the LII fluence curves reported in Fig.1 at 0.2 J/cm². From this figure, it appears that the evolution of the normalized fluence curves with HAB is relatively similar in the three sooting flames. Hence, we observe that the fluence curves determined at the lowest heights ($HAB \leq 12$ mm), show for the three flames a similar quasi-linear evolution over the fluence range accessible with our laser. It has been shown that this behavior is typical of nascent soot particles which are characterized by low $E(m)$ values and require therefore much higher fluence to reach the sublimation threshold [43,44]. Based on

recent characterization of optical properties and fluence curves of such particles [42] we used the constant value $E(m) = 0.250 \pm 0.025$ for the soot particles identified as nascent soot particles in our flames, i.e. for HAB up to 12 mm.

At higher HAB, the fluence curves are characterized by a more classical S-shape strongly depending on T_p with an inflexion point appearing around 0.4 J cm^{-2} characteristic of the sublimation threshold of more mature soots [45]. This evolution denotes a change of the optical properties of the detected soot particles correlated with an increase of $E(m)$. The value of $E(m)$ is indeed well known to vary with the soot maturity in flame [46–50]. Values from 0.2 to 0.4 are usually considered in the literature to characterize particles from the nucleation step to the fully mature graphite-like particle [51–53]. The determination of the evolution of the $E(m)$ value with soot maturity along the flame height was beyond the scope of this work and has not been carried out. Based on the literature, we rather chose to consider a constant value $E(m) = 0.300 \pm 0.030$ as proposed by Yon *et al.* [54] for the more mature soot particles formed from 12.5 mm to 16 mm for all studied flames.

All the recorded LII profiles have been measured by using a laser fluence just below the soot sublimation threshold energy determined from these experimental fluence curves to minimize the influence of T_p on the measured LII signal [55]. Based on these considerations, this laser fluence has been defined equal to 0.359 J cm^{-2} for the three flames studied in this work.

Finally, LII profiles were calibrated in f_v profiles according to the method already detailed in previous works [32,42] and relying on the measurement of the extinction coefficient K_{ext} carried out by CRDS. This coefficient, defined by the well-known Eq.2, has been determined at 16 mm HAB as described in [32,42].

$$K_{ext} = \frac{6\pi E(m)}{\lambda} f_v \quad \text{Eq.2}$$

Where λ corresponds to the excitation wavelength (1064 nm) used for the extinction measurement.

2.2.4 Characterization of the particles size density functions (PSDFs) by SMPS

To measure the particle size distributions, we used a nano-SMPS system (TSI Inc.) as presented in SM1 (Fig. S1) which is capable of measuring size distributions from 1 to 30 nm, coupled to a sampling system based on dilutive microprobe extraction specifically designed for this SMPS experiments.

Soot particles were extracted from the flames by using a microprobe made of two co-annular quartz tubes, the outer tube ending with a long thin tip with a 250 μm orifice. This probe was positioned vertically and inserted into the flame throughout the burner stabilization plate. The outer tube was used to send a cold nitrogen flow (6 L min⁻¹) enabling a fast dilution of the sampled material from the flame directly at the entrance of the microprobe. The dilution ratio was estimated in the range 500-3000. The inner tube was connected to a pump system allowing the sampling of the diluted flow of particles from the flame. A 2 L buffer volume interposed between the probe and the nano-SMPS was required to stabilize the pressure in the sampling line. This system has been implemented in order to avoid post-sampling chemical reactions as well as coagulation and/or aggregation of the sampled particles.

The polydisperse aerosol was injected in the TSI nano-SMPS consisting, in the order, of: (1) a soft X-ray neutralizer model 3088 to reach a known particle charge distribution function; (2) a differential mobility analyzer (DMA) model 3086 operating over the size range 1-30 nm and controlled by an electrostatic classifier model 3082; (3) a nano-enhancer model 3757 that pre-activates the smallest particles in an environment supersaturated in diethylene glycol, and finally (4) a standard n-butanol condensation particle counter (CPC) model 3570 [56]. To minimize diffusion losses, the highest total flow 2.5 L min⁻¹ was used in all experiments and

the sampling line was optimized for minimal distance (<2 m) between the probe and the nano-SMPS [57].

3. Determination of the profiles of the soot particle number densities

To determine the soot particle number density along the flame HAB, we used an original methodology relying on the coupling of the data obtained by SMPS and LII/CRDS measurements. Basically, the SMPS system was used to determine the normalized PSDFs against HAB for the studied flames. The PSDFs were then calibrated into absolute number densities with the soot volume fraction profiles determined by LII and CRDS, according to the analytical procedure explained below. This procedure provides the advantage of not requiring accurate knowledge of the dilution ratio during SMSP measurements, which remains a strong limitation for ex-situ measurements.

It is to be noted that comparisons between f_v deduced from the measurement of the soot PSDFs by SMPS with direct *in situ* extinction measurements have already been reported in the literature and showed very good correlation [58]. The main uncertainty, according to this comparison, has been attributed to the potential variations of the soot refractive index. In our work, the studied flames have been shown to produce soot particles characterized by fluence curves indicating a slight evolution of the optical properties all along the flame height, limiting therefore this issue.

3.1. Theory

The particle size distribution function (PSDF) of soot in the flame sampled volume can be expressed as a function of the particle number density N and the particle diameter D_p as:

$$\frac{dN}{d \log D_p} = \sum_{i=1}^2 N_i \left(\frac{dN}{d \log D_p} \right)_i \quad \text{Eq. 3}$$

308 The sum of functions in Eq. 3 is necessary to account for the bimodal structure observed
 309 at some HAB. N_i is the (partial) particle number density of each mode. The total particle number
 310 density is given by:

$$N_{\text{tot}} = \int_0^{\infty} \frac{dN}{d \log D_p} d \log D_p = N_1 + N_2 \quad \text{Eq. 4}$$

311 $\left(\frac{dN}{d \log D_p} \right)_i$ is well represented, as it will become clear in the experimental section, by
 312 lognormal distributions having median diameter $\bar{D}_{p,i}$ and geometric standard deviation $\sigma_{g,i}$ [59–
 313 64]:

$$\left(\frac{dN}{d \log D_p} \right)_i = \frac{1}{\sqrt{2\pi} \log \sigma_{g,i}} \exp \left[-\frac{(\log D_p - \log \bar{D}_{p,i})^2}{2(\log \sigma_{g,i})^2} \right] \quad \text{Eq. 5}$$

314 It is important to notice that in this work we chose the normalized number density $\frac{dN}{d \log D_p}$
 315 over $\frac{dN}{dD_p}$ since the former is independent of the instrument resolution and therefore particularly
 316 useful when intercomparing data from different instruments. In the explored D_p range (1.5–
 317 15 nm), soot particles are spherical and isolated [55], and the shift between the two
 318 representations $\frac{dN}{d \log D_p}$ and $\frac{dN}{dD_p}$ is always verified to be < 0.1 nm and thus considered as
 319 negligible.

320 CRDS (in-situ) measures the soot volume fraction f_v without giving access to any
 321 information on the PSDF that is hidden in the integral:

$$f_v = \frac{\pi}{6} \int_0^{\infty} D_p^3 \frac{dN}{d \log D_p} d \log D_p \quad \text{Eq. 6}$$

On the other hand, SMPS (online) accesses the electrical mobility size distribution $\left(\frac{dN}{d \log D_p}\right)_{\text{SMPS}}$, but cannot provide a reliable measurement of the in-situ total particle number density that is biased by the sampling:

$$\frac{dN}{d \log D_p} = K(D_p) \left(\frac{dN}{d \log D_p}\right)_{\text{SMPS}} \quad \text{Eq. 7}$$

Here, the function $K(D_p)$ folds in all sampling-related effects that include the probe and dilution effects during sampling and the particle losses during transport in the probe, in the sampling line and in the SMPS due to diffusion, and depends on a number of factors including D_p .

In this work, the same probe and dilution flow were used in all experiments. The uncertainty due to the HAB-dependent temperature on the probed flame volume is small and therefore included in the calculation of the total uncertainty of the particle number density. In order to avoid post-sampling coagulation, preliminary SMPS scans were performed at each HAB by decreasing the differential pressure (thus increasing the dilution ratio) until the particle number density was sufficiently low that no shift of the PSDF to higher D_p could be observed in the time required for the data acquisition. All the PSDFs discussed in this work have been acquired with a dilution ratio equal or higher than this limit.

The quantitative estimation of the particle losses due to diffusion during transport is difficult and well beyond the scope of this paper. In this work, a rough estimation was performed by following the theoretical approach proposed by Kulkarni *et al.* [65] to calculate the transport efficiency function $\eta_{\text{tube,diff}}$ against D_p . The calculated $\eta_{\text{tube,diff}}$ has the highest slope between 2-3 nm, and is roughly twice as large at 5 nm than 2 nm. While experimental estimations of the particle losses for $D_p < 10$ nm exist in the literature [66,67], they are typically determined for very specific experimental conditions or subject to large uncertainty, and thus

often regarded as tricky to generalize. For this reason, and to avoid introducing further uncertainty in the interpretation of the measurements, we decided to discuss the uncorrected SMPS output, thus de facto neglecting the effect of the particle losses due to diffusion that will be instead the object of a future dedicated investigation.

Under these assumptions, $K(D_p) \approx K$ can effectively be treated as a calibration factor for the given experimental conditions. In conclusion, the relationship between f_v from *in-situ* extinction (CRDS) and $\left(\frac{dN}{d \log D_p}\right)_{\text{SMPS}}$ from online electrical mobility (SMPS) can be approximated as:

$$f_v = \frac{\pi}{6} K \int_0^{\infty} D_p^3 \left(\frac{dN}{d \log D_p} \right)_{\text{SMPS}} d \log D_p \quad \text{Eq. 8}$$

3.2. Application of the method

A practical example of the fitting procedure applied to the PSDF measured in the sooting flame Φ -1.91 at 12 mm HAB is shown in Fig. 2.

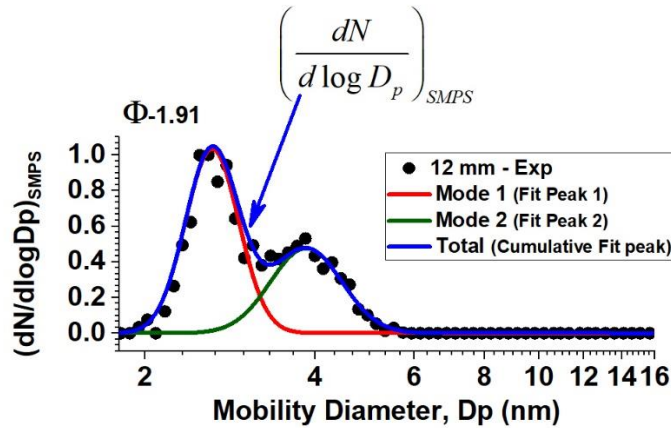


Fig. 2: Result of the fitting procedure by using two lognormal functions at the onset of the bimodality of size distribution at 12 mm HAB in sooting flame Φ -1.91.

360

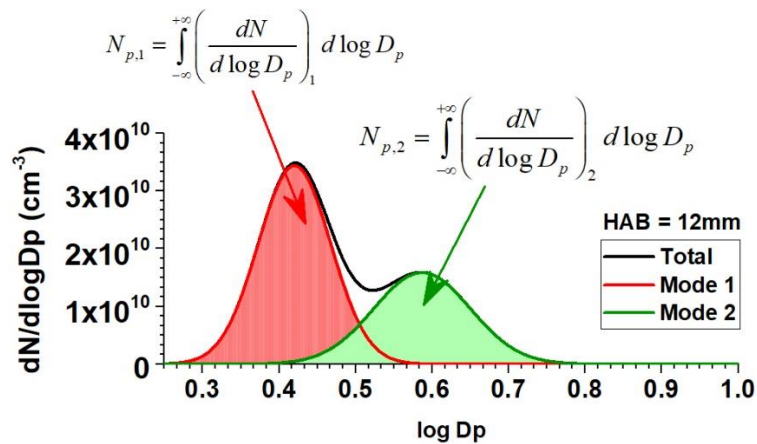
361 As explained above, the method of determination of the soot number density N_p relies
 362 on finding the empirical factor K that enables the calibration of the normalized PSDFs reported
 363 in SM1 (Fig. S6) obtained by SMPS into absolute number density, with f_v being known from
 364 CRDS experiments. This calibration factor K is defined in Eq 7 and independently calculated
 365 at each sampled HAB. For instance, at 12 mm HAB in the flame Φ -1.91:

$$K_{12\text{mm}} = \frac{f_v}{\frac{\pi}{6} \int_0^\infty D_p^3 \left(\frac{dN}{d \log D_p} \right)_{\text{SMPS}} d \log D_p} = \frac{1.24 \times 10^{-10}}{3.74 \times 10^{-21}} \approx 3.32 \times 10^{10} \quad \text{Eq. 9}$$

366 The integration of the PSDF allows deducing, according to Eq. 4, the total number
 367 density of soot particles that in the example at 12 mm HAB: $N_p = 6.59 \times 10^9 \text{ cm}^{-3}$. This protocol
 368 can be extended to the determination of the number density of soot particles in the different
 369 modes (mode 1 and mode 2) of the PSDF, as graphically shown in Fig. 3 ($N_{p,1} = 4.09 \times 10^9 \text{ cm}^{-3}$
 370 3 , in red and $N_{p,2} = 2.50 \times 10^9 \text{ cm}^{-3}$, in green).

371 This procedure has been applied to all the investigated flames to obtain the absolute soot
 372 numbers density profiles presented and discussed in the following sections.

373



374

375 Fig. 3: Determination of number density of mode 1 and 2 of soot particles at 12 mm HAB in the flame
 376 Φ -1.91.

377

4. Results and discussion

4.1. Effect of H₂ on the flame temperature profiles

Fig. 4 displays the experimental temperature profiles obtained with a coated Pt/Rh(6%)-Pt/Rh(30%) thermocouple for the three studied flames (Φ -1.91, Φ -1.91_H₂-S, and Φ -1.91_H₂-A). The reported temperatures were not corrected from the radiative heat loss. As it can be seen, the H₂ substitution (Φ -1.91_H₂-S) shifts the temperature profile toward the burner surface due to the laminar flame velocity increase (see Table 1), while the addition procedure (Φ -1.91_H₂-A) does not cause any shift. Indeed, the laminar flame velocity of flame Φ -1.91_H₂-S has been determined to be around 9.9 m/s which was higher than that calculated in flame Φ -1.91 around 9.2 m/s. By contrast, the laminar flame velocity of flame Φ -1.91_H₂-A around 9.1 m/s is close to that of reference flame Φ -1.91. In both approaches (addition or substitution), as expected by such a small introduction of H₂ (1.8%), all studied flames exhibit similar temperature peak, confirming the negligible influence of the additional H₂. Hence, the temperature measured in the post flame region where soot particles are formed and growing are very close in the three studied flames. The adiabatic temperature calculated using GASEQ [39] confirms the very limited impact of H₂ on the flame temperature profiles as shown in Table 1. The absence of modification in the three measured temperature profiles (except the slight shift towards the burner of the whole profile in the case of H₂ substitution) therefore allows attributing the change of the mole fraction of PAHs and soot volume fraction to the effect of H₂ and not to the temperature.

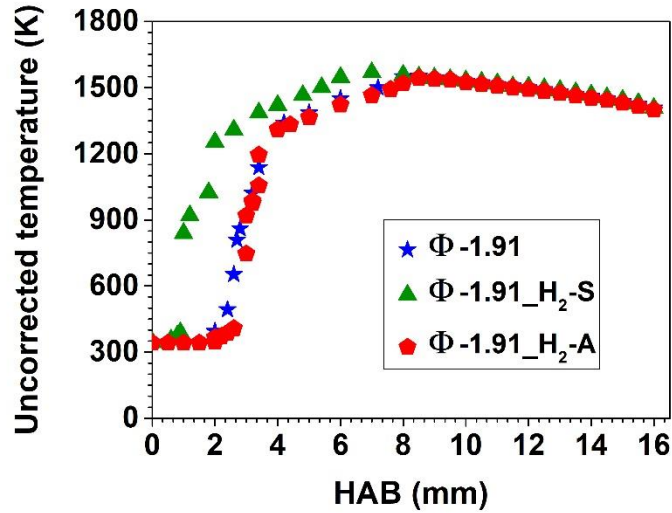


Fig. 4: Impact of H₂ on the uncorrected flame temperature profiles. Φ-1.91: CH₄ flame; Φ-1.91_H₂-S: CH₄ substituted-H₂ flame; Φ-1.91_H₂-A: CH₄ added-H₂ flame (see Table 1 for the flame conditions).

4.2. Effect of H₂ on major species (reactants and combustion products)

Fig. 5 reports the mole fraction profiles of the main species including reactants (fuel, O₂) and final products (CO, CO₂, H₂, H₂O) for the three studied flames. As observed for the temperature profiles presented above, the H₂ substitution (Φ-1.91_H₂-S) systematically shifts the profiles of the major species around 2 mm closer to the burner surface while the H₂ addition (Φ-1.91_H₂-A) does not significantly modify the flame position. The explanation for this effect is the same as the explanation for the temperature profiles discussed in Section 4.1. Briefly, this shift can be explained by the laminar flame velocity increase in the case of H₂ substitution (Φ-1.91_H₂-S). By contrast, in the case of H₂ addition (Φ-1.91_H₂-A), no significant modification of the flame velocity is calculated and therefore no significant influence on the flame position. It is to be noted that the higher mole fractions of H₂ observed at HABs from 0 mm to 11 mm in the latter flame compared to the reference flame are simply due to the added H₂ fraction in the initial gas mixture. The impact of H₂ on the evolution of the mole fraction profiles of the reactants and final products obtained in the three flames is similar as the one observed in the three nucleation flames reported in our recent work [32].

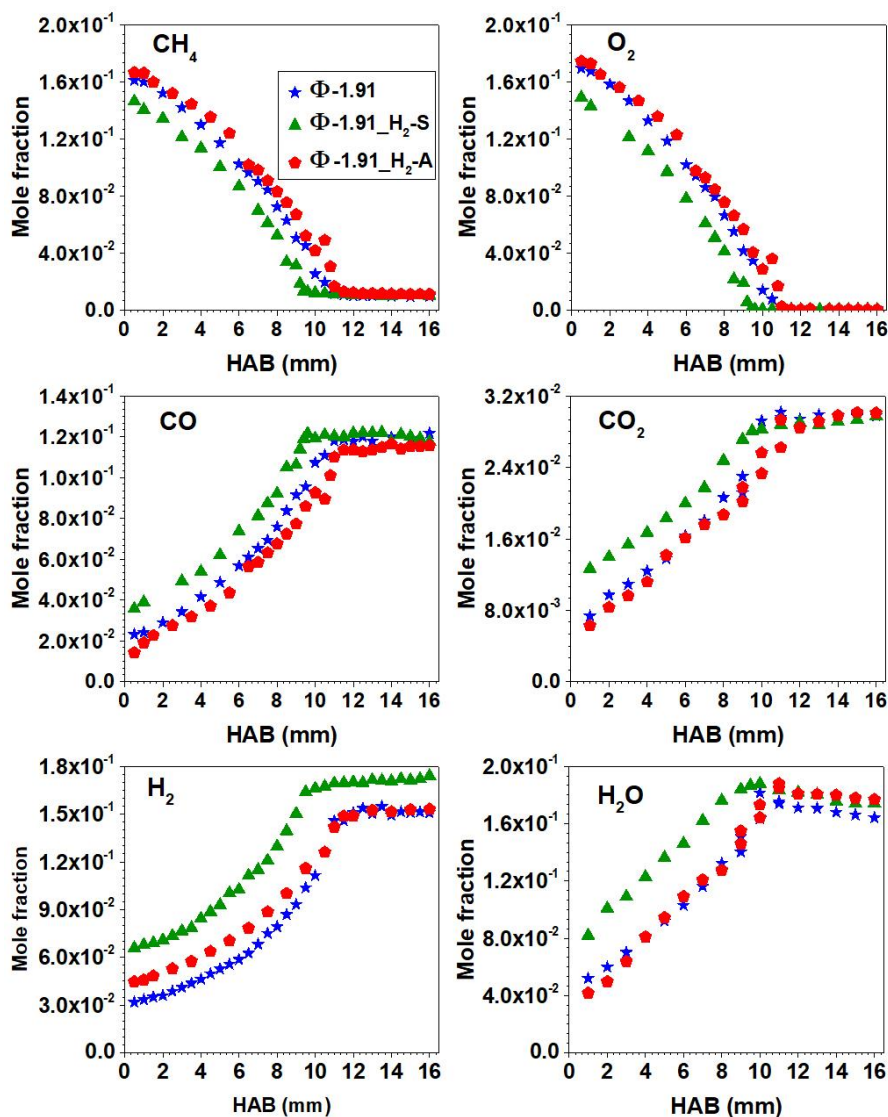


Fig. 5: Mole fraction profiles of reactants (fuel, O_2) and major products (CO , CO_2 , H_2 , H_2O) obtained in the three studied flames.

4.3. Effect of H_2 on soot precursors

Fig. 6 shows the mole fraction profiles of some aliphatic and aromatic species in the three flames. We present here the mole fraction profiles of acetylene (C_2H_2), allene (AC_3H_4) and propyne (PC_3H_4) which are considered as important precursors of the first aromatic ring, PAHs and soot [68–71]. The mole fraction profiles of other aliphatic species analyzed in this work are available in SM1 (Fig. S2). Fig. 6 also displays the measured mole fraction profiles

of three aromatic compounds (benzene C_6H_6 , naphthalene $C_{10}H_8$ and pyrene $C_{16}H_{10}$) which are considered as crucial soot precursors [32,72–74].

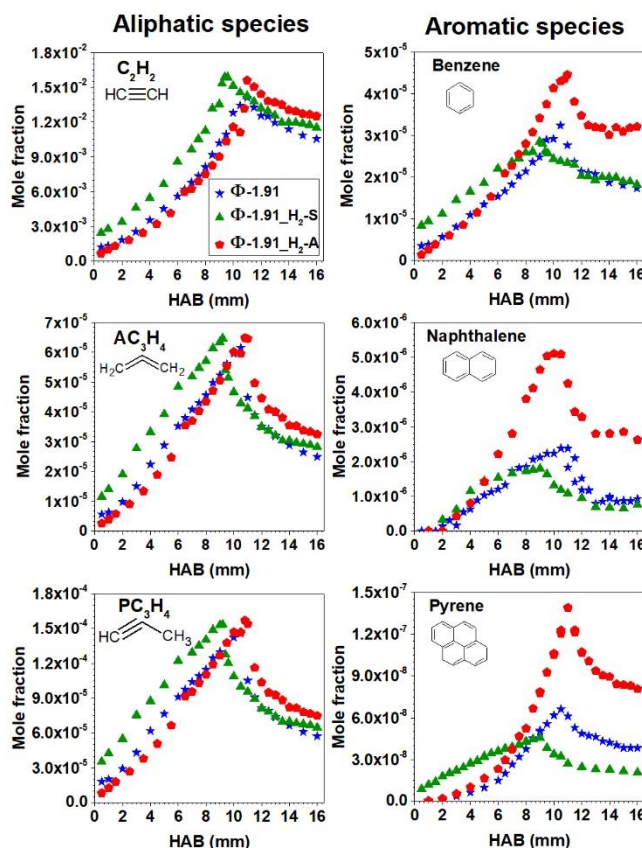


Fig. 6: Mole fraction profiles of aliphatic species (acetylene, allene, propyne) and aromatic species (benzene, naphthalene and pyrene) obtained in the three studied flames.

The H_2 substitution shifts the mole fraction profiles of all gaseous species around 2 mm closer to the burner surface because of the increase of the laminar flame velocity as presented in Table 1, consistently with the consumption behavior, while H_2 addition does not induce any significant effect on the position of the mole fraction profiles of the detected species in the gas phase. Both H_2 substitution and addition show no significant effect on the peak values of the mole fraction of the aliphatic species. However, the presence of H_2 in the sooting flame Φ -1.91 strongly impacts the formation of aromatic species (Fig. 6). The H_2 substitution (Φ -1.91_ H_2 -S) exhibits an inhibitory effect (12-31%) on benzene, naphthalene, and pyrene formation whereas

the H₂ addition (Φ -1.91_H₂-A) clearly promotes their formation (30-53%). Such antagonistic effect was also observed for the nucleation flames in our recent work [32]. In this work we have also shown that the impact of H₂ can be specifically attributed to a chemical effect rather than dilution. Indeed, substituting the equivalent of 1.8% of N₂ by He did not affect the mole fraction profiles of benzene and aliphatic species in any flames as shown in SM1 (Fig. S3).

A detailed explanation of the chemical effect of H₂ on aromatic species was given in our previous work [32]. The same mechanism could be considered for the present flames, as summarized in Fig. S4. Under flame conditions, H₂ can be converted to H-atoms through several reactions, such as $\text{H}_2 + \text{OH} \rightarrow \text{H} + \text{H}_2\text{O}$, $\text{H}_2 + \text{O} \rightarrow \text{H} + \text{OH}$, and $\text{H}_2 + \text{M} \rightarrow \text{H} + \text{H} + \text{M}$. The H₂ effect is then the result of different competitive processes that share the resulted H-atoms as a reactant. As showed in Fig. S4 (left panel), the high temperature branching reaction $\text{H} + \text{O}_2 = \text{O} + \text{OH}$ (path A) competes with the benzene/PAH accumulation process (path B), the PAH growth processes (path C), and the soot particle growth processes (paths D and E) that are significant in the fuel richer flames. As showed in the right panel of Fig. S4 in the case of substitution, the path A is reinforced by the presence of H₂ which is proved by the observed increase of the laminar flame speed (Table 1). In these conditions, the H-atoms are thus largely converted to OH and O, resulting in the acceleration of the oxidation processes of aromatic species and in the decrease of the H-atoms available for the PAH growth through the HACA mechanism. These points explain the decrease of the mole fractions of the aromatic species under the H₂ substitution conditions.

In the case of H₂ addition, the reaction $\text{H} + \text{O}_2 = \text{O} + \text{OH}$ is not favored. This is confirmed by the flame front position and by the calculated laminar flame speed, which highlighted similar values for the flame with added H₂ (Φ -1.91_H₂-A) and the reference flame (Φ -1.91) as reported in Table 1. Thus, H-atoms from H₂ addition would primarily participate to the benzene/PAHs formation by termination reactions, promoting aromatic formation.

4.4. Effect of H₂ on soot formation

The measured soot volume fraction profiles determined for the three studied flames are reported in Fig. 7. The H₂ substitution shifts the soot volume fraction f_v profile around 2 mm closer to the burner surface, while H₂ addition does not induce this effect (Fig. 7a). The effect of H₂ on the position of the f_v profile is consistent with that of the gaseous soot precursors as reported in Fig. 6. The H₂ substitution decreases while H₂ addition increases the maximum f_v . Hence, the impact of H₂ on the soot quantities generated in flame Φ -1.91 may be directly related to the formed PAHs mole fractions as discussed above.

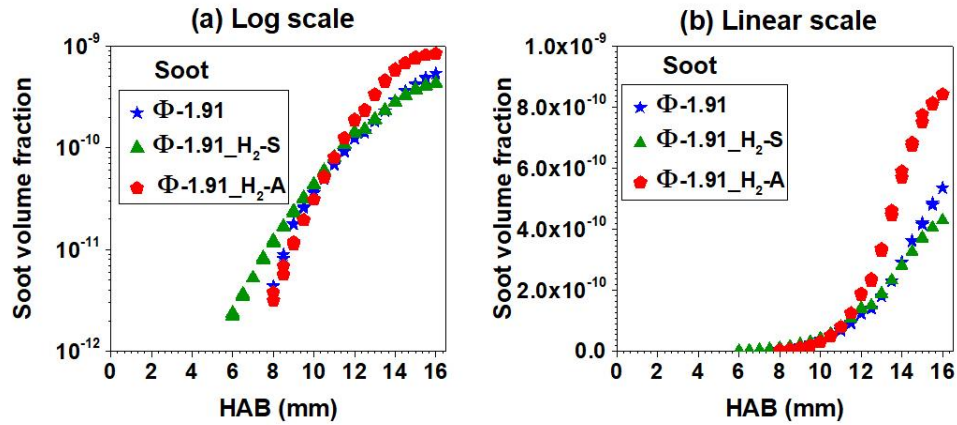


Fig.7: Soot volume fraction profiles measured in the three studied flames by LII /CRDS. (a) log scale and (b) linear scale.

4.4.1. Hypothesis about a PAH concentration threshold for soot nucleation

In flame Φ -1.91_H₂-S, we carefully determined by LII the HAB corresponding to the beginning of the soot formation according to the sensitivity of our optical setup (first measurable LII signals). Hence this point has been established at 6 mm HAB for this flame and the corresponding soot volume fraction at this HAB has been determined to be around 2 ppt, i.e. a value similar to that previously measured at the soot starting point of the nucleation flames

[32]. The corresponding mole fractions of benzene, naphthalene and pyrene at this HAB were determined around 22 ppm, 1.5 ppm and 36 ppb, respectively, which are very close to the values measured at the onset of the soot nucleation point of the previously studied nucleation flames [32]. This observation therefore supports the hypothesis already suggested in [32] of a PAH concentration thresholds, potentially independent of the flame operating conditions and nature of the fuel, triggering the soot nucleation process. Unfortunately, the determination of this onset point in the other two flames was affected by higher uncertainty. Regarding our data, and notably the signal-to-noise ratio (SNR) of the LII signal measured at 8 mm, corresponding to the lowest studied HAB by LII in the Φ -1.91 and Φ -1.91_H₂-A flames (Fig S.5b and c), it is clear that the SNR appears much better than that observed at 6 mm in flame Φ -1.91_H₂-S. Hence, it is likely that the onset of the soot nucleation point for these two flames is located a little upstream 8 mm. However, the soot volume fractions determined at 8 mm in the flame Φ -1.91 (f_v =4.4ppt) and flame Φ -1.91_H₂-A (f_v =3.2 ppt) are still very close to that at the onset of the soot nucleation point in flame Φ -1.91_H₂-S (f_v =2 ppt). Moreover, it is noteworthy that the mole fractions reported in Table 2 of benzene, naphthalene and pyrene measured at the onset of the soot nucleation points in the three flames (Φ -1.91 flame, Φ -1.91_H₂-A, Φ -1.91_H₂-A) are similar and also very close those of previously investigated nucleation flames [32] (see also Table 2). These data support therefore the idea of a PAH concentration threshold required to initiate the soot nucleation process. However, it is clear that more experimental work, especially involving other fuels, is required to confirm this hypothesis.

Flame	Mole fractions (soot starting point)		
	Benzene (ppm)	Naphthalene (ppm)	Pyrene (ppb)
Φ -1.91	21	1.8	38
Φ -1.91_H ₂ -S	22	1.5	36
Φ -1.91_H ₂ -A	28	3.8	52
Φ -1.82 / Φ -1.82_H ₂ -S / Φ -1.82_H ₂ -A [32]	16	1.3	22

Table 2: Mole fractions of aromatic compounds determined at the onset of the soot nucleation in the three rich flames Φ -1.91 and previously studied nucleation flames Φ -1.82 [32].

4.4.2. Effect of H₂ on the particle size distribution function

In this section, the impact of H₂ on the soot particle diameter and number density and more specifically on its influence on the growth mechanism of soot formation is discussed in detail. Fig. 8 presents the PSDFs measured from SMPS, LII and CRDS experiments against HABs in the three studied flames. As it can be seen in this figure, the first measurable PSDFs by SMPS in these flames appears at slightly higher HABs than the detection of the first LII signals reported in Fig. 7. In the absence of a deepen comparison between the two techniques, it is difficult to conclude about the origin of this small shift, which might be due to several reasons as a lower detection limit of the LII setup or the flame perturbation induced by the probe sampling required for the SMPS measurements. However, this small discrepancy suggests that our microprobe only slightly perturbs the flame front, which validates the complementary use of these techniques implemented here to characterize the soot formation.

Concerning the Φ -1.91 flame, as already observed in the literature [75–77], we notice at the lowest HABs the appearance of a single mode characterized by a fixed diameter all along the flame height, followed by the formation of a second mode higher in the flame, highlighting

the growing particles. The first PSDF measured at 8 mm HAB, that characterizes the nascent soot particles generated in the nucleation process, features a monomodal lognormal distribution centered around 2.5 nm (mode 1). The monomodal distribution exists only up to 10.5 mm HAB. Above 10.5 mm HAB, a bimodal distribution appears. While mode 1 does not shift to higher D_p as the HAB increases, mode 2, newly appeared at 10.5 mm HAB and initially centered at 3.2 nm, shifts to higher D_p as HAB increases. The existence and shift of mode 2 point to the competition between nucleation, coagulation and surface reactions as already well established in the literature [58,77–79]. At 12 mm HAB, mode 2 appears more clearly and mode 1 reaches its maximum intensity. Above 12 mm HAB, mode 1 begins to decrease and disappears completely at 15 mm HAB, suggesting that the nucleation process is no longer active above this HAB probably because of the diminution of the concentration of aromatic soot precursors in the flame. Fig. 9 presents the evolution of the median diameter of mode 1 and 2 against HAB for the three studied flames. We observe that the median diameter of mode 1 is constant against HAB and that the median diameter of mode 2 increases gradually. This dynamic suggests that the soot growth process in flame Φ -1.91 are dominated by the HACA mechanism and by PAHs condensation on the soot surface rather than coagulation/coalescence processes.

Concerning the influence of H_2 (Φ 1.91_ H_2 -S and Φ 1.91_ H_2 -A flames), Figs. 8 and 9 show that both H_2 substitution and addition do not influence the PSDF (median diameter and geometric standard deviation) of mode 1. This result indicates that the mechanism of nascent soot formation from gaseous precursors is probably similar in the three studied flames, which will be further discussed in the next section. The end of the nucleation process observed in the Φ -1.91_ H_2 -S flame at 15 mm HAB is similar to the reference flame Φ -1.91. By contrast, it is noteworthy that the formation of nascent soot particles in flame Φ -1.91_ H_2 -A is promoted along the whole flame height.

Fig. 10 shows the evolution of the soot number density of mode 1, mode 2 and the total soot number density in the three studied flames. H₂ substitution slightly decreases the maximum soot number density of mode 1 while H₂ addition strongly increases this value. This decrease or increase of mode 1 with the H₂ substitution or addition could be a result of a decrease or an increase in the formation of aromatic species, respectively, as shown in Fig. 6. Above 15 mm in the two flames Φ -1.91 and Φ -1.91_H₂-S, the mole fraction of aromatic species is low (Fig. 6). Hence, aromatic species can not initiate anymore the soot nucleation process. By contrast, in the Φ -1.91_H₂-A, the H₂ addition strongly increases the formation of aromatic species. In this case, the mole fraction of these species is always above the aromatic concentration threshold associated to the formation of the very first soot particles [32] and this, even for the higher HAB in this flame. In this case, the nucleation process is always active along the flame height in flame Φ -1.91_H₂-A. These data therefore again point out to the need of a minimum concentration of PAHs required for the activation of the soot nucleation process

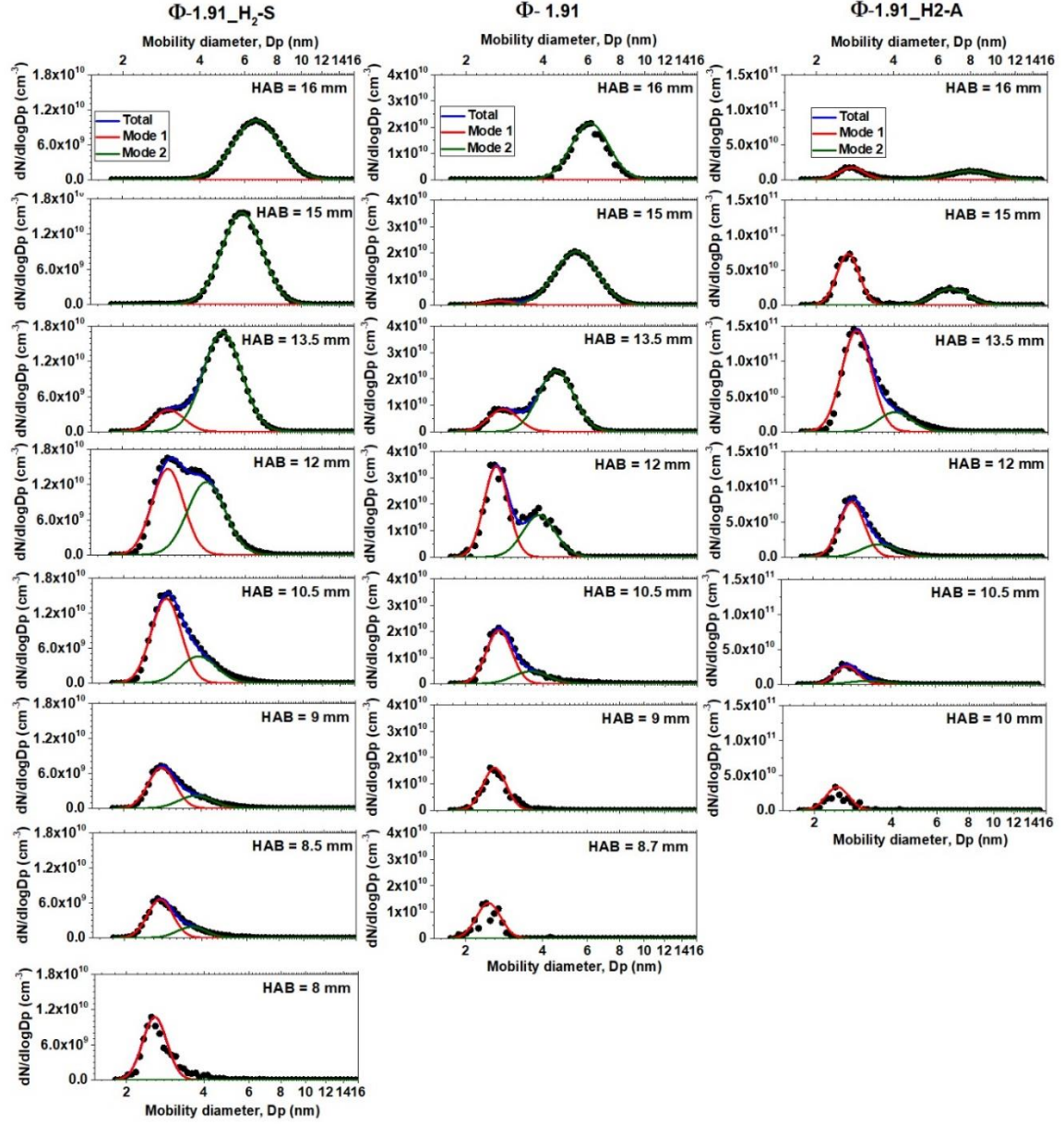


Fig. 8: Particles size distribution functions measured by SMPS, LII and CRDS obtained in the three studied flames.

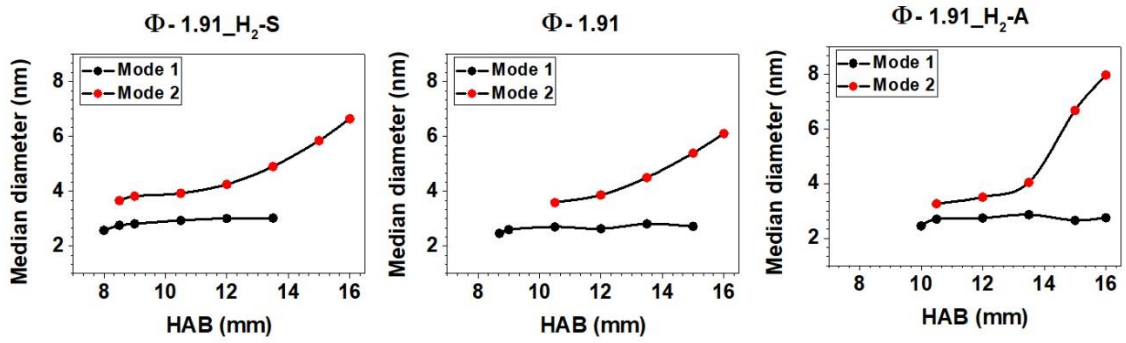


Fig. 9: Median diameter of mode 1 and mode 2 against HAB obtained by fitting the PSDFs in the three studied flames.

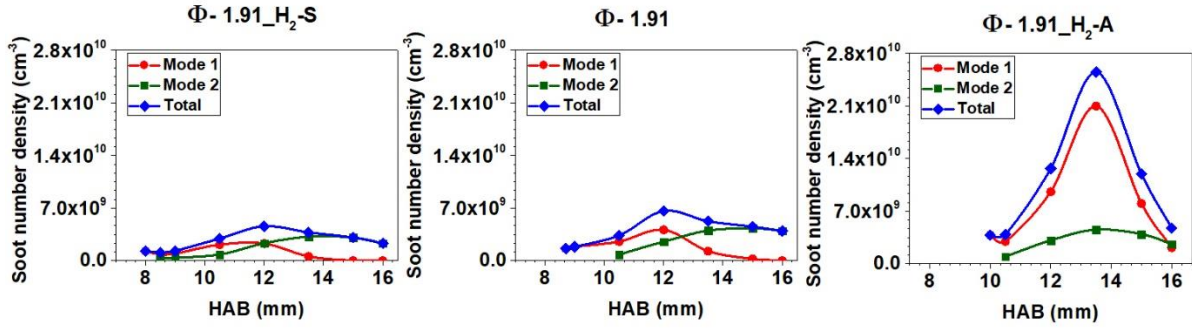


Fig. 10: Evolution of soot number density against HAB in the three studied flames.

Regarding the soot growth process, based on the evolution of the measured PSDFs (Fig. 8), we can deduce that the dynamic of these processes in the flame Φ -1.91_H₂-S is quite similar to that in flame Φ -1.91. Indeed, mode 2 in this flame appears gradually as shown in Fig. 9, and similarly the median diameter of mode 2 increases gradually at higher HAB. This suggests a soot growth process mainly driven by surface growth processes as the HACA mechanism and PAHs condensation on soot surface in these two flames. However, it is noteworthy that the H₂ substitution shifts the onset of the soot growth process to lower HAB than that in flame Φ -1.91. Indeed, according to Fig. 6, the H₂ substitution also shifts to lower HAB the mole fraction profile of soot precursors as C₂H₂ and aromatic species. The median diameter of mode 2 at 16 mm HAB in flame Φ -1.91_H₂-S is therefore slightly higher than in flame Φ -1.91 because the residence time of soot particles for soot growth process in the flame Φ -1.91_H₂-S is slightly longer than in the flame Φ -1.91. Finally, the H₂ substitution decreases the soot number density of mode 2 and total soot number density because of the diminution of the initial quantity of nascent soot particles formed in this flame.

In flame Φ -1.91_H₂-A, mode 2 initially appears very close to mode 1 at 10.5 mm HAB, characterized by a median diameter evolving from 3.3 to 4.1 nm between 10.5 and 13.5 mm HAB, similar to the reference flame. However, by contrast with the reference flame Φ -1.91, in the Φ -1.91_H₂-A, mode 2 against HAB shows a substantial change of slope around 13.5 mm

HAB as shown in Fig. 9. The evolution of this mode, very different from that observed in the reference flame Φ -1.91, indicates the predominance of additional growth processes to those observed in the reference flame Φ -1.91, probably coagulation and/or coalescence. The sudden appearance of this mode 2 with median diameter 6.7 nm at 15 mm is indeed consistent with a stronger efficiency of the coagulation/coalescence processes of the particles of the mode 1 with a median diameter of 2.6 nm.

If this hypothesis is correct, the predominance of the coagulation/coalescence growth processes might be correlated with the larger number of soot particles formed in the flame Φ -1.91_H₂-A due to the addition of H₂ and therefore to the greater probability of particle collisions under these conditions. As shown in Fig. 10, H₂ addition strongly increases the number of soot particles of mode 1 compared to reference flame Φ -1.91, clearly highlighting the major role of H₂ in the nucleation process. The increase of nascent soot particles number density stops at 13.5 mm HAB and a drastic decrease of nascent soot particles is then observed between 13.5 and 15 mm HAB, directly correlated to the appearance of the isolated mode 2. It is interesting to note that this specific evolution only appears in this flame in which the quantity of nascent soot particles is up to 5 times higher than that in the reference flame Φ -1.91. The ensemble of the experimental data seems to suggest the existence of a threshold value for the particle concentrations above which the coagulation/coalescence processes would become dominant due to a greater probability of collision of soot particles. A complete understanding of this phenomena would require detailed modelling that was beyond the scope of this work and will be the subject of further investigations.

4.4.3. Effect of H₂ on nascent soot particles

As observed in Section 4.4.2, the H₂ addition induces a persistence of the soot nucleation process all along the flame height characterized by the presence of the mode 1 in substantial number density. To further explore the effect of H₂ addition on the nucleation process in sooting flame Φ -1.91, Fig.11 recaps the profiles of temperature, H₂, pyrene and soot number density of mode 1 in the two flames Φ -1.91, Φ -1.91_H₂-A.

As already stated, H₂ addition does not impact the temperature profile reported in Fig. 11a. Therefore, the observed modifications in the formation of aromatic species and soot reported in Fig.11c,d is rather related to the chemical effect due to the addition of H₂. We observe in Fig. 11b that the mole fraction of H₂ near the burner surface of flame Φ -1.91_H₂-A is higher than in the reference flame Φ -1.91 and tends to approach the mole fraction profile of H₂ of the reference flame from 8 mm up to 10.5 mm HAB (green area in the figure). The mole fraction of pyrene increases strongly in this zone due to the H₂ addition (Fig. 11c). As discussed earlier, the consumption of H atoms from the H₂ addition mainly serves to termination reactions involving aromatic radicals and yields stable aromatic compounds. Above 10.5 mm, the mole fraction of H₂ measured in the two flames Φ -1.91, Φ -1.91_H₂-A is similar. Therefore, the soot nucleation process after the pyrene peak is mainly impacted by a higher concentration of PAHs due to the H₂ addition, and resulting in the formation of a large number of nascent soot particles after the pyrene peak in flame Φ -1.91_H₂-A (10.5 – 13.5 mm, violet zone in the figure). The large number density of nascent soot particles at 13.5 mm HAB increases the coagulation/coalescence rate and results in the drastic reduction of the soot particles number density above this zone and the concomitant appearance of mode 2 centered around 6.7 nm at 15 mm HAB (see Fig. 8).

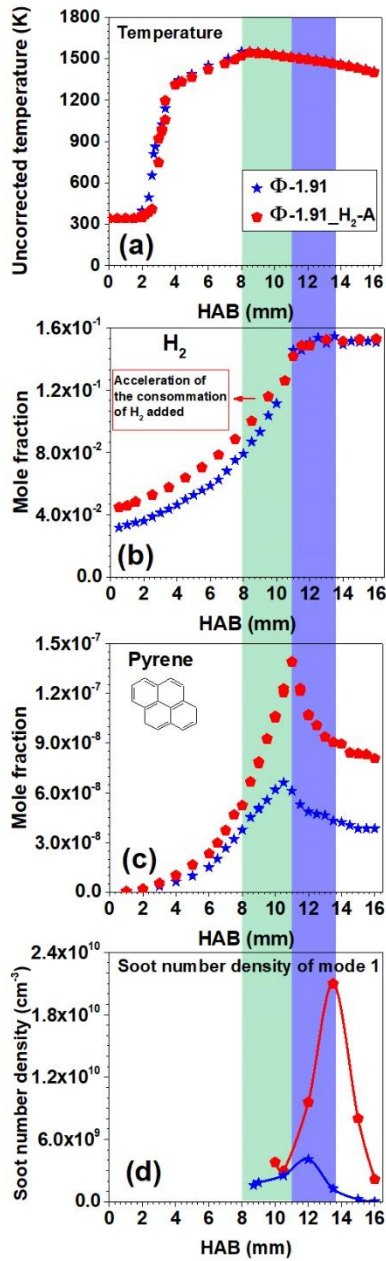


Fig. 11: Profiles of temperature, and mole fraction of H_2 , pyrene and soot number density of mode 1 in the two flames Φ -1.91 (blue), Φ -1.91- H_2 -A (red). The green zone defines the accumulation of aromatic species; the violet zone defines the consumption of aromatic species for nascent soot formation. The line in Fig. 11d has been added to the plot to guide the eye.

This statement can be further corroborated by the analysis of previous experiments we carried out in slightly a sooting methane flame (Φ -1.82) [32] generating much less PAHs and soot particles than the Φ -1.91 flames. In this work, we also slightly perturbed the reference Φ -1.82 flame by H_2 addition or substitution according to the same protocol as used for the Φ -1.91. The PSDFs of the soot particles in these flames (not reported in [32]) was newly measured in the present work and reported in Fig. 12. The determination of the absolute soot number density N_p has been carried out according to the method described section 3.1, using the normalized PSDFs obtained by SMPS reported in SM1 (Fig. S8).

The Φ -1.82 reference flame has been defined as a nucleation flame, i.e. a flame generating soot particles which do not undergo or very limited growth processes all along the flame height. Hence, the soot PSDFs for this flame are characterized by almost one mode. As can be seen in SM1 (Fig. S9), this mode highlights a quasi-constant median diameter around 2.6 nm all along the flame height, similar to the mode 1 characterizing the nascent soot particles generated in the Φ -1.91 flames. A much weaker second mode however appears at 13.5 mm HAB, indicating that soot growth processes are still somewhat activated in the nucleation flame Φ -1.82, but actually well balanced by oxidation along a large part of the flame, precluding the growth of the soot particles excepted at the highest HABs [38].

According to Fig. 12, the introduction of H_2 , either by addition or substitution, in these nucleation flames, does not impact the PSDF of the generated soot particles. By contrast, the introduction of H_2 in the nucleation flame Φ -1.82 strongly impacts the formation of aromatic species and soot volume fraction [32] as well as the soot number density as reported in Fig. 13. Similarly to the observations made for the Φ -1.91 flame, the H_2 substitution in the nucleation flame Φ -1.82 decreases the nascent soot particles number density while the H_2 addition strongly increases the nascent soot particles number density. However, the H_2 addition in the nucleation flame does not seem to modify the soot growth dynamic by enhancing the

coagulation/coalescence processes as observed in the richer flame Φ -1.91_H₂-A, probably because of the much lower number density of soot particles (around 10 times less) generated in the flame Φ -1.82_H₂-A in comparison with the Φ -1.91-A, therefore limiting the probability of collision of soot particles.

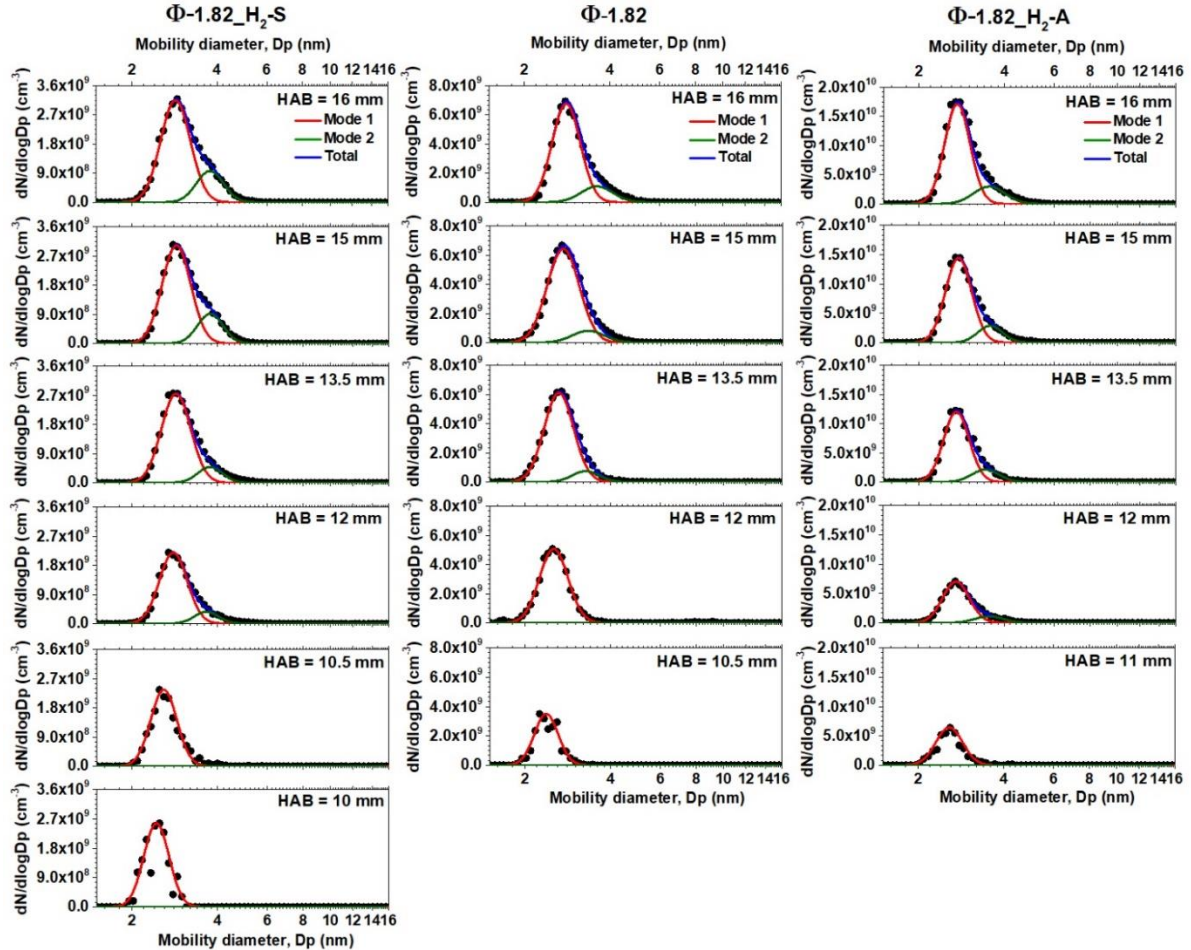


Fig. 12. Particles size distribution functions measured by SMPS obtained in the three methane nucleation flames.

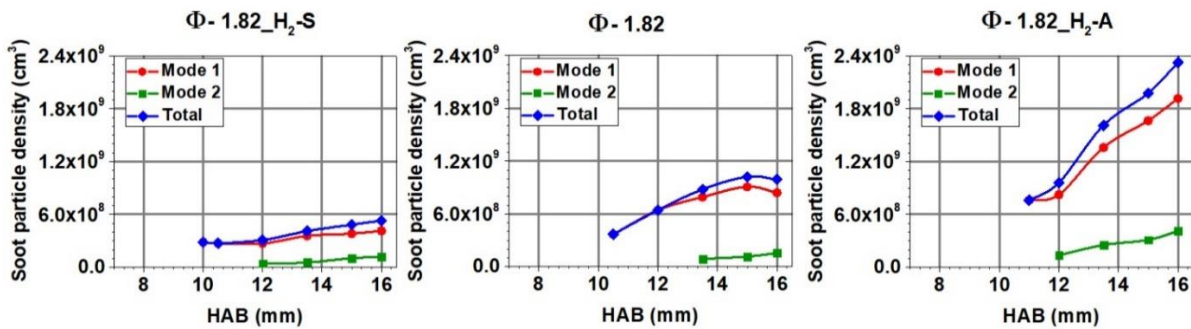


Fig. 13. Evolution of soot number density in the three methane nucleation flames.

5. Conclusion

This work reports new experimental data obtained in three atmospheric sooting premixed methane flames with and without added/substituted H_2 (~10% molar comparing to CH_4 fuel, at $\Phi_C=1.91$). An original analytical methodology has been developed relying on the coupling of the data obtained by SMPS and LII/CRDS measurements to determine the soot number density. This method does not require accurate knowledge of the dilution in the sampling line, which is a strong limitation for quantitative SMSP measurements of particle number density.

Our results clearly show the influence of H_2 as a fuel additive to the formation of soot precursors, soot nucleation and soot growth. Similarly to previous observations on nucleation flames [32], the results obtained in the presented fuel-richer flames notably show that the introduction of H_2 strongly influences the concentration of aromatic species and soot, either increasing or decreasing, that depends on the operating conditions (H_2 addition or substitution). Finally, the invariance of the concentration of PAHs and the soot volume fraction measured at the beginning of the soot formation in the sooting flames $\Phi=1.91$, similarly to previous experiments carried out in different nucleation flames, again supports the idea that onset of the soot particle might be controlled by specific concentrations thresholds of aromatic precursors already mentioned in [32].

Regarding the soot size distribution, we observed that neither H_2 substitution nor H_2 addition influence the PSDF and in particular the median diameter of mode 1 featuring the nascent particles either in the rich flames $\Phi=1.91$ or in the nucleation flame $\Phi=1.82$. This result indicates that the mechanism of nascent soot formation from gaseous precursors is probably similar in the three studied flames. The H_2 substitution in the flame does not influence the mechanism of soot growth, either. By contrast, we observe in the case of H_2 addition a substantial modification in the dynamic of the soot growth processes. This modification might

be due a better efficiency of the coagulation/coalescence processes because of the strong increase in the number of nascent soot particles. The H₂ addition indeed promotes the accumulation of PAHs in the area preceding the pyrene peak through termination reactions involving H atoms and PAH radicals. The accumulation of aromatic species prior to the pyrene peak provides a large reservoir of nascent soot particles molecular precursors resulting in the increase in the number of these particles after the pyrene peak. This large increase of the number of nascent soot particles in the Φ -1.91_H₂-A flame might therefore favor the coagulation/coalescence processes thus promoting their size increase in the burnt gas zone. From this study, we hypothesized the existence of a soot particle number density threshold above which the coagulation/coalescence processes might become more effective due to a greater probability of collision of soot particles. However, only the use of detailed soot growth models will enable an accurate description of the real dynamic and of the involved equilibria between the different soot growth processes taking place in these flames. This detailed modeling study will certainly be investigated in the near future.

Acknowledgements

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Figure Captions:

Fig.1: Normalized fluence curves at 0.2 J/cm^2 obtained in three studied flames. Φ -1.91: CH_4 sooting reference flame; Φ -1.91_ H_2 -S: CH_4 substituted- H_2 flame; Φ -1.91_ H_2 -A: CH_4 added- H_2 flame.

Fig. 2: Result of the fitting procedure by using two lognormal functions at the onset of the bimodality of size distribution at 12 mm HAB in sooting flame Φ -1.91.

Fig. 3: Determination of number density of mode 1 and 2 of soot particles at 12 mm HAB in the flame Φ -1.91.

Fig. 4: Impact of H_2 on the uncorrected flame temperature profiles. Φ -1.91: CH_4 flame; Φ -1.91_ H_2 -S: CH_4 substituted- H_2 flame; Φ -1.91_ H_2 -A: CH_4 added- H_2 flame (see Table 1 for the flame conditions).

Fig. 5: Mole fraction profiles of reactants (fuel, O_2) and major products (CO , CO_2 , H_2 , H_2O) obtained in the three studied flames.

Fig. 6: Mole fraction profiles of aliphatic species (acetylene, allene, propyne) and aromatic species (benzene, naphthalene and pyrene) obtained in the three studied flames.

Fig.7: Soot volume fraction profiles measured in the three studied flames by LII /CRDS. (a) log scale and (b) linear scale.

Fig. 8: Particles size distribution functions measured by SMPS, LII and CRDS obtained in the three studied flames.

Fig. 9: Median diameter of mode 1 and mode 2 against HAB obtained by fitting the PSDFs in the three studied flames.

Fig. 10: Evolution of soot number density against HAB in the three studied flames.

Fig. 11: Profiles of temperature, and mole fraction of H_2 , pyrene and soot number density of mode 1 in the two flames Φ -1.91 (blue), Φ -1.91_ H_2 -A (red). The green zone defines the

1006 accumulation of aromatic species; the violet zone defines the consumption of aromatic species
1007 for nascent soot formation. The line in Fig. 11d has been added to the plot to guide the eye.
1008 Fig. 12. Particles size distribution function measured by SMPS obtained in the three methane
1009 nucleation flames.
1010 Fig. 13. Evolution of soot number density in the three methane nucleation flames.
1011