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# Impact of secondary coatings on the dissolution rate of K-feldspar: A combined experimental and modeling study

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## 23 **Abstract**

24 Heat transfer fluid mining represents a thermodynamic perturbation for geothermal  
25 reservoirs: The pumping of hot water coupled with the re-injection of colder water at depth  
26 favors the dissolution of some rock-forming minerals of the deep reservoir (e.g. feldspars),  
27 while promoting the precipitation of secondary phases, resulting in a possible change in the  
28 permeability and porosity of the reservoir. Such an impact is even greater when one considers  
29 the acid stimulations aimed at increasing the injectivity of the geothermal system. In that  
30 respect, no consensus exists in the literature regarding the impact of secondary phases on the  
31 dissolution rate of primary phases and therefore, on the sustained modification of pore  
32 structure. The present study aimed at shedding new light on these questions. Hydrothermal  
33 experiments of K-feldspar alteration were conducted at conditions relevant for the geothermal  
34 reservoir of Soultz-sous-Forêts ( $T = 180\text{ }^{\circ}\text{C}$ , acidic pH domain). Measurements of cation  
35 release rates were combined with characterizations of secondary coatings (mineralogy, extent  
36 of coverage, thickness and porosity) to determine the reactivity of submillimeter K-feldspar  
37 powders with and without secondary precipitates. The formation of  $\mu\text{m}$ -thick boehmite  
38 coatings on K-feldspar grains was found to result in a modest decrease in its reactivity, which  
39 might be better explained by the presence of dissolved Al in the bulk solution. This result was  
40 independently confirmed by reactive transport simulations, which revealed that the impact of  
41 secondary coatings may become significant only when their thickness exceeds a few tens of  
42 microns, or if the dissolution rate of the primary phase is significantly greater ( $10^6$  times) than  
43 that of orthoclase. Taken together, this study offers new constraints on the intricate interplay  
44 between dissolution and precipitation reactions, of prime importance for modeling more  
45 accurately the impact of mass transfer and porosity generation resulting from fluid circulation  
46 in geothermal reservoirs.

47

## 48 **1. Introduction**

49       Enhanced geothermal systems (EGS), which generate geothermal electricity by  
50 circulating water in subsurface environments with a positive thermal anomaly, are among the  
51 strategies that are frequently invoked to contribute to the decarbonization of energy sources  
52 and reduce greenhouse gas emissions. ‘Hot Dry Rock’ (HDR) projects emerged in the middle  
53 of the 1980s, aiming to circulate heat-bearing fluids in closed loops to harness the heat stored  
54 in deep rocks through fracture networks developed in the rock by fracking. In parallel, several  
55 groups over the world explored complementary strategies, such as those consisting in taking  
56 advantage of the geothermal potential that could be offered by naturally fractured deep  
57 crystalline rocks that may maintain deep natural convective loops. These circulation paths  
58 could be used for heat transfer fluid mining without additional fracking. In that respect, the  
59 Soultz-sous-Forêts geothermal power plant located in the Upper Rhine Graben, 50 km north  
60 of Strasbourg, represented one of such pioneering sites in France that has been selected as it  
61 exhibits a strong thermal anomaly, extensively studied since the 1920s and oil field research  
62 in that area ([Munck et al., 1979](#); [Gérard et al., 1984](#)). The subsurface at this site is a natural  
63 deep hydrothermal system with a geothermal gradient noticeably higher than normal in the  
64 first km of the sedimentary cover (~100 °C/ km) and natural brine circulation in the  
65 underlying fractured granite, which is responsible for a reduced geothermal gradient (30  
66 °C/km) between 1 and 3.5 km. The Soultz-sous-Forêts geothermal project was initiated by a  
67 French-German team in 1986, and has been in operation for almost 40 years, supplying  
68 electricity since 2008 (a summary of the history of the project can be found in e.g., [Genter et](#)  
69 [al., 2010](#)).

70       From a geochemical standpoint, the pumping of hot water coupled with the re-injection  
71 of colder water at depth favors the dissolution of some rock-forming minerals of the deep  
72 reservoir (e.g. feldspars), while promoting the precipitation of secondary phases ([Fritz et al.,](#)

73 [2010; Ngo et al., 2016](#)). The relative intensities of primary mineral leaching and secondary  
74 phase formation may affect porosity and permeability of the reservoir, thereby influencing its  
75 hydraulic performance. Such changes in mineral composition and reservoir permeability /  
76 porosity are among the most important parameters when acid stimulations, aimed at  
77 increasing the productivity and injectivity of a given geothermal system, are considered (e.g.  
78 [Lucas et al., 2020](#)). Therefore, predicting the fate of fluid injection in geological reservoirs  
79 represents a critical issue for evaluating the modification of reservoir permeability / porosity  
80 resulting from fluid-rock interactions in general ([Cui et al., 2021a, b](#)), and the efficiency of  
81 EGS in particular ([Alt-Epping et al., 2013a; Alt-Epping et al., 2013b; Griffiths et al., 2016;](#)  
82 [Lucas et al., 2020; Vital et al., 2020](#)). However, the predictive ability of reactive transport  
83 models is frequently questioned. Indeed, the kinetics of water-rock interactions are rarely  
84 successfully reproduced without the use of fitting parameters, most often aimed at refining the  
85 “effective surface area” of minerals, whose value remains somewhat arbitrarily fixed in  
86 modeling exercises, and supposed to be related to the proportion of the surface of primary  
87 minerals that is not covered by secondary phases (e.g. [Montes-H et al., 2005; Maher et al.,](#)  
88 [2009; Aradóttir et al., 2012](#)).

89       This fundamental issue has given rise to a wealth of experimental and theoretical work  
90 aimed at investigating the feedback effects between coupled dissolution and precipitation  
91 reactions, some of the main results of which are briefly reviewed below. On the one hand,  
92 coupled dissolution-precipitation reactions were demonstrated to act as an autocatalytic  
93 system, where the consumption by secondary precipitates of the released ions maintains  
94 conditions of undersaturation with respect to the primary phases, thereby sustaining a high  
95 dissolution flux, resulting in an equally high precipitation rate of secondary phases (e.g.  
96 [Putnis, 2002; Frugier et al., 2008; Putnis, 2009](#) and references therein). On the other hand, the  
97 formation of secondary phases has also long been suspected to potentially result in so-called

98 “armoring” or “passivating” effects, preventing the transport of reactants between the bulk  
99 fluid and the surface of the dissolving primary phases (Luce et al., 1972; Velbel, 1993).  
100 Several parameters were identified as crucial in predicting the passivating ability of a given  
101 coating, including (i) the molar volume ratio of product to reactant (with ratio > 1 possibly  
102 resulting in passivation of the primary phases Velbel, 1993); (ii) the potential  
103 crystallographic relationships between primary and secondary phases (with epitaxial growth  
104 favoring passivation; e.g. Cubillas et al., 2005); or (3) if the coating is a silica gel, its potential  
105 evolution from a porous to a denser and less permeable structure due to various aging  
106 mechanisms (Gin et al., 2001; Cailleateau et al., 2008; Gin et al., 2015; Saldi et al., 2015;  
107 Daval et al., 2017; Daval et al., 2018; Fournier et al., 2019).

108 Overall, previous experimental work suggested that secondary phases can have opposite  
109 impacts on the dissolution of the parent phases, and the extent of coverage resulting from  
110 mineral precipitation has often been used in modeling exercises as a fitting parameter to  
111 decrease accordingly the proportion of the surface area of the mineral that actually contributes  
112 to the dissolution flux. To shed new light on these questions, the present study was designed  
113 to investigate the impact of secondary coatings on the reactivity of K-feldspar, one of the  
114 main rock-forming minerals in granitic geothermal reservoirs, such as the one at the Soultz-  
115 sous-Forêts site. At this site, K-feldspar represents 23.6 vol% of the fresh granite  
116 composition, other major phases including plagioclase (42.5 vol%), quartz (24.2 vol%), and  
117 biotite (4.2 vol%) (Fritz et al., 2010). The experiments were conducted under conditions  
118 relevant for this specific site of interest, in acidic solutions ( $T = 180\text{ }^{\circ}\text{C}$ ;  $2 < \text{pH} < 4$ ). The  
119 reasons for targeting these pH conditions are two-fold: first, they are well suited to simulating  
120 the impact of an acid stimulation of the reservoir, as the HCl concentration of the stimulating  
121 fluid can be as high as 0.45% (pH ~ 1) (Lucas et al., 2020) while the pH of granitic reservoirs  
122 is generally slightly acidic (e.g., close to 4.8 in the case of Soultz-sous-Forêts; Fritz et al.,

123 2010). Secondly, from an experimental standpoint, running experiments in the acid pH range  
124 makes it possible to take advantage of the low solubility of Al at high temperature ( $< 10^{-5}$  M  
125 for  $2 < \text{pH} < 7$  at 180 °C) to develop secondary coatings on timescales of days to weeks.  
126 Although investigating the impact of barite on K-feldspar dissolution could have been  
127 considered even more relevant in the case of Soultz-sous-Forêts as barite represents one of the  
128 most abundant scaling phases (e.g., Griffiths et al., 2016 and references therein), the massive  
129 precipitation of barite remains out of reach experimentally, as it results from the long-term  
130 release of trace amounts of barium contained in K-feldspar (e.g., Pauwels et al., 1993;  
131 Azaroual and Fouillac, 1997). Therefore, we purposely decided to focus on studying the  
132 impact of major Al-rich secondary phases resulting from the dissolution of a primary rock-  
133 forming mineral to specifically investigate a model coupled interfacial dissolution-  
134 reprecipitation system (i.e., where secondary phases grow directly at the contact surface with  
135 the primary dissolving phase) because of its broad relevance for a wide range of geological  
136 processes (Ruiz-Agudo et al., 2014). In addition, as the acid stimulation on site may  
137 eventually drive K-feldspar dissolution and additional Ba release in the fluid, this enhanced  
138 dissolution may compete with barite removal targeted by the acid stimulation on the longer  
139 terms. As detailed below, the use of reactive transport modeling enabled us to unravel the  
140 contribution of secondary coatings to the modest decline in K-feldspar reactivity observed  
141 experimentally and to provide guidelines for anticipating the conditions under which  
142 secondary coatings may have a significant impact on the reactivity of primary phases.

143

## 144 **2. Materials and methods**

### 145 **2.1 Sample characterization and preparation of K-feldspar powders**

146 Preliminary experiments were first conducted with K-feldspar originating from the  
147 Soultz-sous-Forêts site. However, the phenocrysts isolated from the granitic reservoir contain

148 several wt.% of accessory minerals and are perthitic in nature, resulting in the preferential  
149 dissolution of the albitic domains, which made it impossible to properly isolate the impact of  
150 secondary phases on K-feldspar reactivity following the approach described below. As a  
151 consequence, the selected starting material was a natural K-feldspar (orthoclase) crystal  
152 coming from Afghanistan, which we already described in some of our previous work (Pollet-  
153 Villard et al., 2016a; Pollet-Villard et al., 2016b). In brief, no minor phases were detected  
154 with scanning electron microscopy (SEM) or X-ray diffraction (XRD), bearing in mind that  
155 the detection limit of the apparatus we used is close to 1 wt.%. The chemical composition of  
156 the sample ( $\text{K}_{0.75}\text{Na}_{0.22}\text{Fe}_{0.01}\text{Al}_{0.98}\text{Si}_{3.02}\text{O}_8$ ) was determined by Inductively Coupled Plasma  
157 Atomic Emission Spectroscopy (ICP-AES; THERMA® ICAP 6000 Series) after a standard  
158 alkaline digestion. Dissolution experiments were carried out on orthoclase powders. Powders  
159 were obtained after crushing centimeter-sized orthoclase single crystals with a hydraulic press  
160 and sieving to recover the 800-1000  $\mu\text{m}$ -sized fraction. Fine particles were removed from this  
161 powder by five successive water baths followed by several ultrasonic cleaning in ethanol until  
162 the discarded supernatant became clear. The resulting orthoclase powder was then dried at 40  
163 °C during two hours. After cleaning cycles, a part of the powder was analyzed with a Tescan®  
164 VEGA II SEM to control that the powder was free of fine particles (Fig. S1). The specific  
165 surface area of the powder, measured with 7-points Kr BET, was  $0.012 \text{ m}^2 \cdot \text{g}^{-1}$ .

## 166 **2.2 Aqueous alteration experiment**

167 Powders were reacted in a synthetic acidic solution in a Parr® mixed-flow reactor (see  
168 Fig. S1b and Hellmann et al., 1997 for more details) at 180 °C and 50 bars for durations  
169 ranging from one to three weeks. Inlet solutions were made with ultrapure deionized water  
170 (18.2 M $\Omega$ .cm) and analytical grade  $\text{Na}_2\text{SiO}_3$ , LiCl and  $\text{AlCl}_3$  powders and HCl. The pH was  
171 adjusted with the concentration of HCl in the solution. No pH buffer was used in solution



172 because buffers can influence the dissolution rate of silicates (e.g. Golubev and Pokrovsky,  
173 2006).

174 Before each experiment, the system was cleaned in a 0.1 M HCl bath for several hours  
175 and was subjected to a circulation (at a flow rate  $v = 1 \text{ mL}\cdot\text{min}^{-1}$ ) of 0.01 M HCl solution for 2  
176 hours. Then, the inlet solution (used to carry out alteration experiments) was circulated in the  
177 reactor (without powder) for at least three days, at 180 °C, until the concentrations of K, Al  
178 and Si were below the detection limit. After this cleaning procedure, powders were introduced  
179 in the reactor to start the alteration experiments. Each experiment was performed at constant  
180 temperature (180 °C), pressure (50 bars), flow rate and inlet solution composition (Tables 1  
181 and 2).

182

183 **Table 1. Chemical conditions of experiments aimed at forming secondary coatings on orthoclase grains**  
184 **(MPA experiments).**

	Duration (days)	Flow rate ( $\text{mL}\cdot\text{min}^{-1}$ )	Mass (g)	Inlet concentrations ( $\text{mol}\cdot\text{L}^{-1}$ )					
				Si	Al	Na	K	Cl	Li
MPA1	9	0.1	0.1957	-	-	-	-	2.00E-2	1.00E-2
MPA2	9	0.1	0.4037	-	-	-	-	1.10E-2	1.00E-2
MPA3	17	0.1	0.4002	-	-	-	-	2.00E-2	1.00E-2
MPA4	9	0.1	0.4042	-	-	-	-	1.0E-4	-
MPA5	19	0.1	0.4118	-	-	-	-	5.65E-5	-
MPA6	12	0.1	0.4100	2.06E-4	2.00E-4	4.32E-4	-	7.00E-7	-
MPA7	9	0.13	0.4976	2.06E-4	2.00E-4	4.55E-4	-	1.60E-3	-
MPA8	11	0.15	0.4186	1.21E-4	1.00E-4	2.22E-4	-	1.03E-2	-
MPA9	16	0.1	0.4016	-	-	-	-	1.00E-2	-

	Outlet concentrations ( $\text{mol}\cdot\text{L}^{-1}$ )						pH	Ionic strength ( $\text{mol}\cdot\text{L}^{-1}$ )	$\Delta Gr$ ( $\text{kJ}\cdot\text{mol}^{-1}$ )
	Si	Al	Na	K	Cl	Li			
MPA1	3.09E-4	6.42E-5	1.78E-5	7.64E-5	2.00E-2	1.00E-2	2.1	2.00E-2	-72
MPA2	3.29E-4	2.63E-7	1.93E-5	8.52E-5	1.1E-2	1.00E-2	3.1	1.1E-2	-67
MPA3	5.38E-4	3.40E-5	3.00E-5	1.32E-4	2.00E-2	1.00E-2	2.1	2.00E-2	-66
MPA4	1.29E-4	1.50E-7	7.90E-6	3.80E-5	1.00E-4	-	4.3	1.00E-4	-70
MPA5	9.31E-5	2.50E-6	1.05E-5	2.60E-8	5.65E-5	-	4.7	5.70E-5	-65
MPA6	5.30E-4	9.80E-6	5.10E-4	8.30E-5	7.00E-4	-	3.8	7.00E-4	-49
MPA7	5.80E-4	9.50E-7	4.8E-4	1.00E-4	1.6E-3	-	3.0	1.60E-3	-48
MPA8	5.85E-4	3.50E-4	2.47E-4	1.34E-4	1.03E-2	-	2.1	1.00E-2	-64
MPA9	5.60E-4	4.14E-5	3.19E-5	1.51E-4	1.00E-2	-	2.1	1.00E-1	-63

185

186 The first four columns indicate the name of the experiments, their duration (days), the fluid flow rate and the  
187 initial powder mass. The following columns list the concentrations of the elements in the inlet and outlet  
188 solutions, determined by ICP-AES analysis. The last three columns show the *in situ* pH, the ionic strength  
189 and the Gibbs free energy with respect to orthoclase dissolution reaction, calculated using CHESS software.

190

191 During experiments, the outlet fluid was sampled daily. The composition of the outlet  
 192 fluid reached a steady-state after a few days of alteration, which correspond, at least, to three  
 193 fluid residence times (defined as the reactor volume divided by the flow rate). Concentrations  
 194 of Si, Al and K in the inlet and the outlet solutions were measured by ICP-AES and are listed  
 195 in Tables 1 and 2. Outlet fluid compositions correspond to the mean aqueous concentrations  
 196 at steady-state conditions. The analytical uncertainties in the ICP-AES measurements, based  
 197 on repeated analyses of standard solutions and blanks, were estimated to be better than  $\pm 10\%$   
 198 (typically 6–7%). The CHESS code ([van der Lee and De Windt, 2002](#)), which is a computer  
 199 model for speciation, batch-reaction, and inverse geochemical calculations, was used to  
 200 determine the *in situ* pH, the ionic strength and saturation indices with respect to orthoclase  
 201 and secondary phases (Table 3).

202

203 **Table 2. Chemical conditions of dissolution experiments on fresh orthoclase powder.**

	Duration (days)	Flow rate (mL.min <sup>-1</sup> )	Powder mass (g)	Steady-state outlet concentrations (mol.L <sup>-1</sup> )					pH	Ionic strength (mol.L <sup>-1</sup> )
				Si	Al	Na	K	Cl		
MDA3	5	0.5	0.0524	2.90E-05	9.20E-06	1.99E-05	7.80E-06	1.00E-02	2.1	1.00E-02
MDA4	6	0.36	0.0522	3.59E-05	1.10E-05	2.50E-06	9.50E-06	1.00E-02	2.1	1.00E-02
MDA5	8	0.6	0.0526	2.35E-05	7.90E-06	1.45E-06	5.80E-06	1.00E-02	2.1	1.00E-02
MDA6	7	0.66	0.0519	1.60E-05	4.95E-06	1.40E-06	3.65E-06	1.00E-02	2.1	1.00E-02
MDA8	14	0.66	0.0504	1.85E-05	5.98E-06	7.74E-07	4.69E-06	1.26E-02	2.0	1.25E-02

204 The first four columns indicate the name of the experiments, their duration, the fluid flow rate and the initial  
 205 mass of powder. The following columns list the concentrations of the elements in the solution sampled  
 206 downstream of the reactor. These concentrations were determined by ICP-AES analysis. The last two columns  
 207 show the *in situ* pH and the ionic strength.

208

209 **Table 3. Thermodynamic status of aqueous solutions in the MDAf experiments.**

	$\Delta Gr(\text{K-spar})$	$\log(Q/K)$				
	(kJ.mol <sup>-1</sup> )	SiO <sub>2</sub> (am)	Gibbsite	Boehmite	Corundum	Diaspore
MDA3	-144	-2.658	-0.904	-0.397	-0.132	-0.189
MDA4	-110	-2.546	-0.828	-0.321	0.021	-0.113
MDA5	-118	-2.749	-0.973	-0.465	-0.269	-0.258
MDA6	-126	-2.916	-1.177	-0.669	-0.676	-0.462
MDA8	-126	-2.853	-1.331	-0.823	-0.984	-0.616

210 The Gibbs free energy with respect to orthoclase dissolution reaction is reported first. The saturation indices  
211 ( $\log(Q/K)$ ) for secondary phases likely to precipitate are reported next. These calculations were run using CHESS  
212 software.

213

214 The experimental strategy is depicted in Fig. 1. In brief, five different series of  
215 experiments were performed:

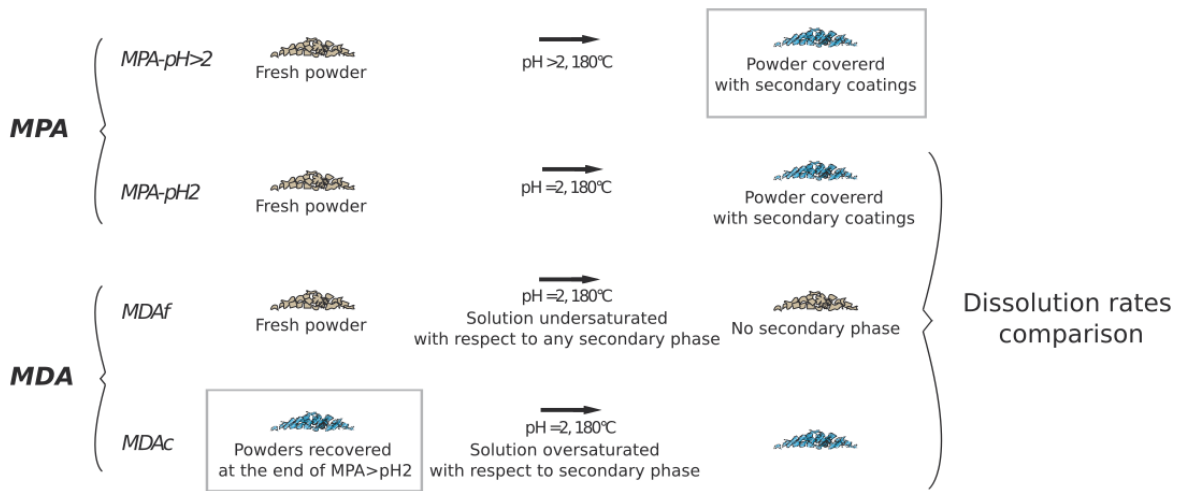
216 (1) Dissolution experiments at pH 2 (hereafter referred to as MD Af) in solutions  
217 undersaturated with respect to any secondary phase. These experiments aimed at providing an  
218 accurate baseline of the reactivity of fresh orthoclase powders devoid of secondary coatings,  
219 at far-from-equilibrium conditions;

220 (2) Coupled precipitation/dissolution reactions (hereafter referred to as MPA-pH2), where  
221 orthoclase dissolution rates were measured at pH 2 during boehmite precipitation. These  
222 experiments aimed at deciphering the impact of precipitated boehmite on orthoclase  
223 dissolution rate;

224 (3) Coupled precipitation/dissolution reactions carried out at pH > 2 (hereafter: MPA-pH>2),  
225 where the increase in pH possibly resulted either in the thickening of the secondary coating  
226 coverage on orthoclase grains, a modification of their texture or a modification of the nature  
227 of the precipitated minerals. The final coated orthoclase powders were then recovered to be  
228 used as starting materials for the series MD Ac described below;

229 (4) Dissolution experiments at pH 2 of the final powders recovered at the end of MPA-pH>2  
230 and covered with secondary coatings (hereafter referred to as MD Ac). These experiments  
231 aimed at estimating the impact of the coatings synthesized in the series MPA-pH>2 on the  
232 dissolution rate of orthoclase. Note that because the solubility of Al-bearing phases decreases  
233 with temperature, the powders were recovered at warm (40 °C; MPA1-MPA5) to hot (95 °C;  
234 MPA6-MPA9) temperatures to prevent dissolution of the coatings during the quench phase;

235 (5) Finally, a last experiment (hereafter referred to as: MPDA) was realized following two  
 236 steps: in the first step, a fresh orthoclase powder was altered in a pH 4 solution enriched in  
 237 Al(aq) in order to precipitate coatings of secondary Al-bearing minerals. After 11 days, the  
 238 inlet solution was replaced with a pH 2 solution, and the dissolution rate of orthoclase was  
 239 monitored through the measurements of aqueous K and Si. This experiment was designed to  
 240 circumvent the potential damages of the coatings covering orthoclase at the end of the MPA-  
 241 pH>2 series: actually, the decrease in pressure and temperature might have resulted in a  
 242 modification of the texture of the secondary coatings. Therefore, experiment MPDA  
 243 improved upon such potential shortcomings.



244  
 245 **Fig. 1.** Schematic of the experimental strategy followed in the present study. See text for details.  
 246

247 For each experiment, orthoclase dissolution rates were calculated from the steady-state  
 248 outlet concentrations of K and Si at the end of each experiment, following the equation (see  
 249 e.g. [Daval et al., 2010](#) for details):

$$r_i = \frac{v \cdot [i]}{\eta_i \cdot SSA \cdot m_0} \quad (1)$$

250 where  $v$  is the flow rate ( $\text{l}\cdot\text{s}^{-1}$ ),  $[i]$  is the outlet concentration of a solute  $i$  ( $\text{mol}\cdot\text{l}^{-1}$ ),  $\eta_i$  is the  
 251 stoichiometric coefficient of element  $i$  in the mineral,  $SSA$  is the specific surface area ( $\text{m}^2\cdot\text{g}^{-1}$ ),  
 252 and  $m_0$  is the starting mass of orthoclase (g), such that  $r_i$  is expressed in  $\text{mol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ .

253 **2.3 Coating characterizations**

254 At the end of each experiment, the reacted orthoclase powders were rinsed with ethanol  
255 and dried at 35°C during a few minutes to perform SEM and XRD analyses.

256 *2.3.1 XRD characterizations*

257 The mineralogical composition of the secondary coatings was characterized by X-ray  
258 diffraction. Samples were analyzed with a diffractometer equipped with a Cu anticathode, at  
259 40 kV and 30 mA (Bruker D5000). Scans were taken for  $2\theta$  ranging from 3° to 65° with  
260 0.03°/step, 25 s /step).

261 *2.3.2 SEM characterizations and focused ion beam milling*

262 SEM analyses of the final powders were conducted to estimate the chemical composition  
263 of the secondary coatings (using energy dispersive X-ray spectroscopy (EDXS), Edax  
264 PEGASUS) and the proportion of the surface of orthoclase that was covered by secondary  
265 coatings in each experiment. The powders were carbon-coated and analyzed with backscatter  
266 electron (BSE), which is sensitive to the chemical composition of the surface. BSE images  
267 were then processed by gray thresholding (Fig. S2) using the ImageJ software ([Abràmoff et](#)  
268 [al., 2004](#); [Schneider et al., 2012](#)) in order to calculate the proportion of orthoclase surface area  
269 coated with secondary phases. Measurements were carried out on a dozen of grains for each  
270 experiment. A part of the altered powders was also embedded into epoxy resin and polished  
271 through a multistep abrasive sequence using diamond suspensions of decreasing grain sizes  
272 and soft polishing cloths. Resulting samples were used to measure the thickness of secondary  
273 coatings with SEM analysis (Fig. S3).

274 Samples embedded in resin and polished were also used to estimate the porosity of  
275 coating. Ultrathin cross sections were milled by focused ion beam (FIB) through the coating  
276 (Fig. S4) using a HELIOS® 600 NANOLAB dual beam equipment operated at CP2M,  
277 Marseille, France. FIB Ga<sup>+</sup> ion milling was carried out at an ion beam voltage of 30 kV and

278 beam current of 0.9 nA. High resolution backscatter electron images were acquired with an  
279 in-lens detector at a beam voltage of 2 kV and beam current of 0.17 nA. Multiple successive  
280 sections were realized throughout the coatings following this method. The corresponding  
281 SEM images were processed by grey thresholding using ImageJ (Fig. S4). This protocol was  
282 followed to estimate the porosity of the coatings formed on the grains from experiments  
283 MPA3 and MPA6.

## 284 **2.4 Numerical reactive transport model**

285 As emphasized from a theoretical standpoint by e.g. [Emmanuel, 2022](#) or experimentally  
286 by [Ruiz-Agudo et al., 2016](#), secondary coatings formed on the surface of primary minerals  
287 may act as a diffusion barrier, limiting the transport of solutes that promote dissolution, such  
288 as protons. To test this hypothesis, a simple 1D reactive transport model was developed and  
289 run using the physical properties of the coatings determined experimentally.

290 Let us consider the transport of  $H^+$  ions in a porous medium. The transport equation in the  
291 direction  $x$  can be written using the classical diffusion equation:

$$\varphi \frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right) \quad (2)$$

292 where  $C$  ( $\text{mol.m}^{-3}$ ) denotes the proton concentration,  $D$  ( $\text{m}^2\text{s}^{-1}$ ) represents the effective  
293 diffusion coefficient and  $\varphi$  is the porosity of the medium. The mathematical formulation of  
294 the effective diffusion coefficient can be given by (e.g., [Archie, 1942](#)):

$$D = D_0 \varphi^m \quad (3)$$

295 where  $D_0$  ( $\text{m}^2\text{s}^{-1}$ ) is the water self-diffusion coefficient and  $m$  the cementation factor of the  
296 medium.

297 The finite volume method was used to solve Eq. (2). The study area is a 1D domain  
298 discretized into  $N$  equally spaced cells, where  $k$  represents the cell center,  $k-1/2$  is the  
299 upstream cell edge and  $k+1/2$  is the downstream cell edge. The parameters  $C$  and  $\varphi$  are

300 defined at the center of the cell, whereas  $D$  is defined at the cell edges. The integration of the  
301 transport equation (Eq. 2) is described in detail in the Appendix.

302 Initially, the  $H^+$  concentration in the porosity of the coating is considered negligible  
303 compared to the concentration in the solution upstream of the coating (i.e.,  $C(t=0) = 0$ ).

304 At  $x = 0$ , the concentration ( $C_0$ ) is fixed at a constant value imposed by the pH of the bulk  
305 fluid. At the boundary between the coating and orthoclase, the concentration depends on a  
306 sink term ( $P$ ) due to the  $H^+$  consumption rate by the orthoclase dissolution reaction. Given  
307 that the dissolution rate of orthoclase varies as the square root of proton concentration in the  
308 aqueous medium (Palandri and Kharaka, 2004), the sink term can be written following:

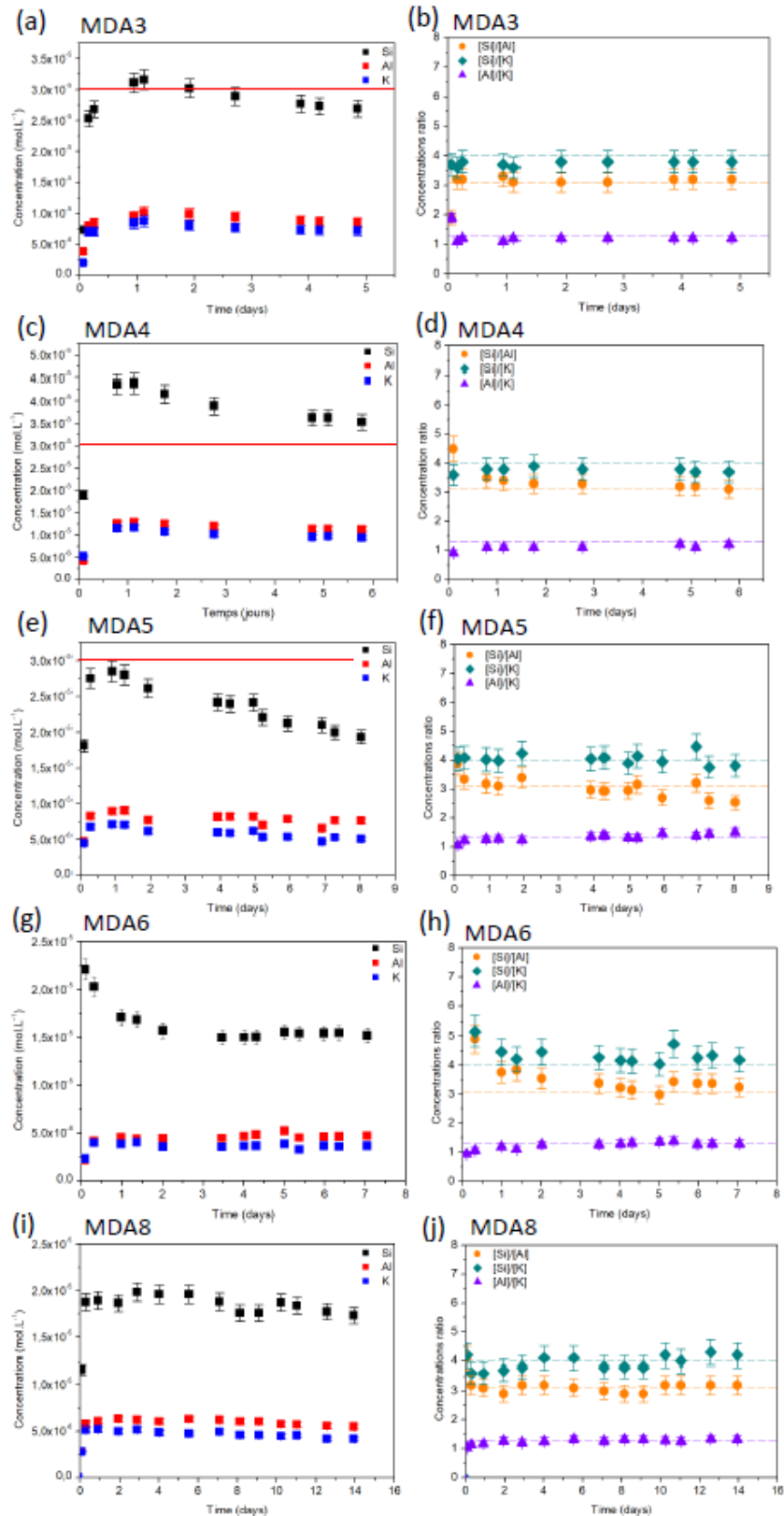
$$P = \frac{4r_0}{\varphi_N \Delta x} \sqrt{\frac{C_N^t}{C_0}} \quad (4)$$

309 In equation (5),  $r_0$  ( $\text{mol.m}^{-2}.\text{s}^{-1}$ ) is the orthoclase dissolution rate in a solution containing a  $H^+$   
310 concentration equal to  $C_0$ ,  $C_N^t$  and  $\varphi_N$  correspond to the  $H^+$  concentration in cell  $N$  at time  $t$   
311 and porosity of cell  $N$ , respectively, and  $\Delta x$  is the size of the cell. The factor 4 results from the  
312 stoichiometry of the dissolution reaction, as 4 moles of  $H^+$  ions are consumed per mole of  
313 orthoclase. The sink term is integrated in the downstream boundary condition of the  
314 numerical transport model as shown in the matrix form of Eq. A6 (see Appendix). In this  
315 simple model, we do not consider the possible evolution of the speciation in the fluid, nor the  
316 impact of  $\Delta G_r$ , as this parameter does not play a significant role in the acidic pH domain (see  
317 Section 4.1).

318

### 319 **3. Experimental results**

320 **3.1 Experiments conducted at pH 2 on fresh powders in undersaturated conditions**  
321 **with respect to secondary phases (experiments MDaf)**



322  
 323  
 324  
 325  
 326  
 327

**Fig. 2. Time-resolved fluid analyses of MDAf experiments.** (a, c, e, g, i) Time-resolved concentrations of released elements (outlet concentration subtracted from inlet concentration). The red lines indicate boehmite solubility. (b, d, f, h, j) ratios of these concentrations. The dashed lines represent the theoretical values of these ratios for stoichiometric dissolution. The MDAf experiments were carried out at pH 2 and under conditions of undersaturation with respect to Al-bearing secondary phases.



328 The concentrations of elements released during orthoclase dissolution (i.e., the difference  
 329 between the outlet concentrations and the concentration measured in the blanks) are shown in  
 330 Fig. 2, corresponding to experiments MDA3, MDA4, MDA5, MDA6 and MDA8. From these  
 331 data, the [Si]/[Al] and [Si]/[K] ratios were calculated to check whether the stoichiometry of  
 332 orthoclase was respected (Fig. 2b). Note that the uncertainties in the concentration  
 333 measurements are between 5% and 10%.

334 Steady-state conditions were reached for all experiments, with the possible exception of  
 335 MDA5, where the Si concentration appeared to decrease slightly over time (Fig. 2a). In this  
 336 experiment, the stock solution was refilled after 5 days of experiment, and a possible slight  
 337 difference in the composition of these two inlet solutions might have resulted in a  
 338 correspondingly slight drop in outlet concentrations.

339 Overall, the cation release observed orthoclase stoichiometry in all experiments (Fig. 2b).  
 340 Therefore, the few precipitates observed at the end of the MDA3 and MDA4 experiments (see  
 341 below and Fig.S5) did not significantly affect the Al concentration measured in the fluid.

342 From the average concentrations measured at steady-state, orthoclase dissolution rates  
 343 were calculated for each experiment (Eq. 1). These rates represent the average of the rates  
 344 calculated from Si and K concentrations (Table 4), and range from  $0.9$  to  $1.3 \times 10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ .  
 345 <sup>1</sup>. Measurement reproducibility was therefore very good, given the uncertainties ( $\sim 1 - 2 \times 10^{-8}$   
 346  $\text{mol.m}^{-2}.\text{s}^{-1}$ ).

347 **Table 4. Orthoclase dissolution rates at 180 °C and pH 2 measured from MDA3, MDA4, MDA5, MDA6**  
 348 **and MDA7 experiments at far from equilibrium conditions ( $\Delta G_r < -110 \text{ kJ.mol}^{-1}$ ).**

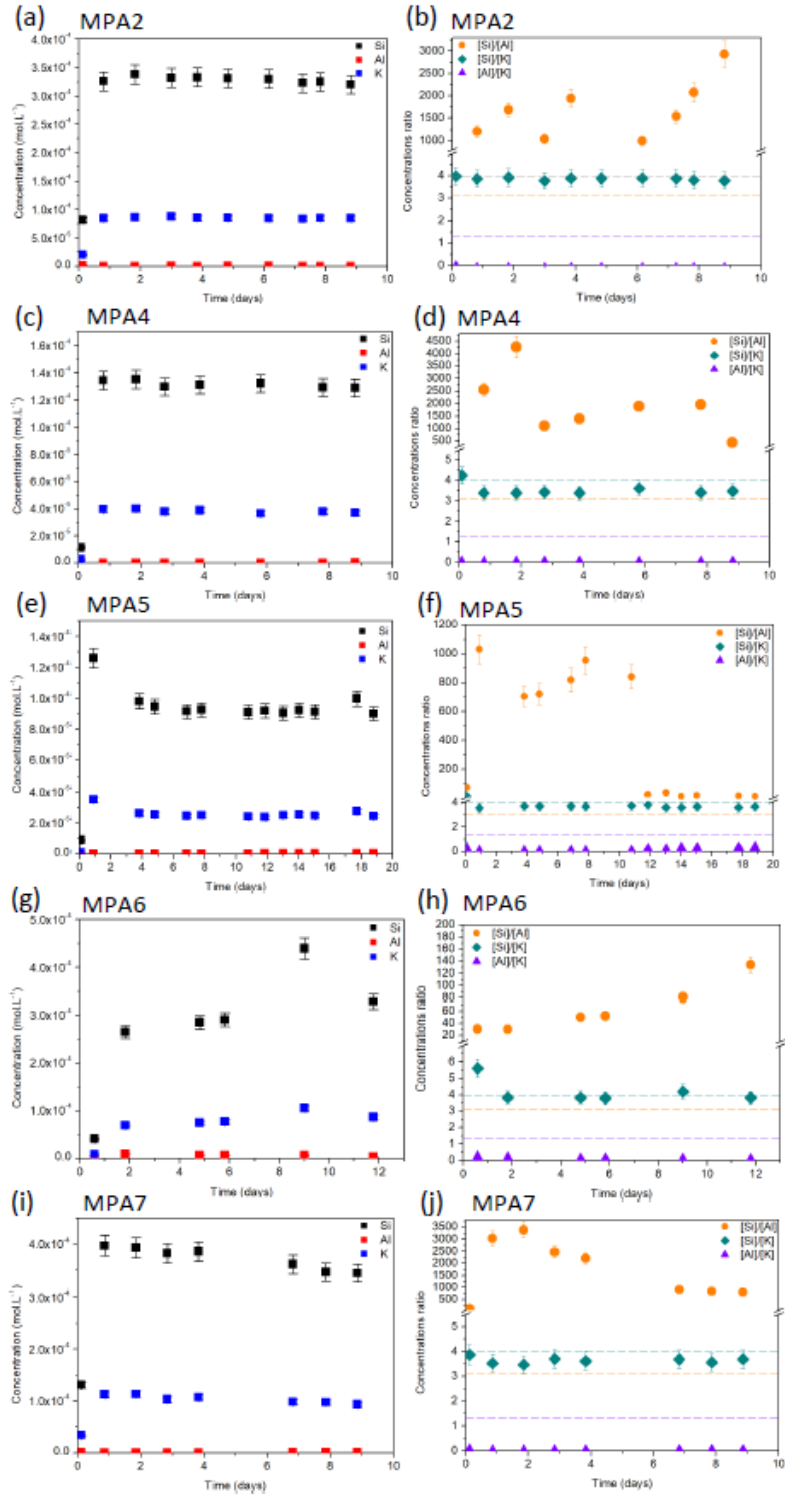
	$\Delta G_r \text{ (kJ.mol}^{-1}\text{)}$	$[\text{Al}] \text{ (mol.L}^{-1}\text{)}$	$r \text{ (}10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}\text{)}$
MDA3	-114	9.20E-06	$1.2 \pm 0.1$
MDA4	-110	1.10E-05	$1.2 \pm 0.1$
MDA5	-118	7.90E-06	$1.3 \pm 0.2$
MDA6	-126	4.95E-06	$0.9 \pm 0.1$
MDA8	-126	5.98E-06	$1.1 \pm 0.1$

349 The average Al concentration and the Gibbs free energy of the reaction, two parameters known to impact the  
 350 dissolution rate, are listed.

351 **3.2 Experiments conducted on fresh powders under conditions of supersaturation**

352 **with respect to secondary phases (experiments MPA)**

353 *3.2.1 Results of MPA-pH>2 experiments*



354 **Fig. 3. Time-resolved fluid analyses of MPA-pH>2 experiments.** (a, c, e, g, i) Time-resolved concentrations  
355 of released elements (outlet concentration subtracted from inlet concentration) and (b, d, f, h, j) ratios of these  
356 concentrations. The dashed lines represent the theoretical values of these ratios for stoichiometric dissolution.  
357

358 The MPA-pH>2 experiments were carried out at pH > 2 and under conditions supersaturated with respect to Al-  
 359 bearing phases. The [Si]/[Al] and [Al]/[K] ratios reveal a lack of Al in solution, resulting from the precipitation  
 360 of Al-rich secondary phases.

361  
 362 The same treatment as presented in the previous section was carried out for experiments  
 363 MPA2, MPA4, MPA5, MPA6 and MPA7. All these experiments were conducted at pH > 2,  
 364 with the aim of forming a coating of secondary phases covering the orthoclase grains.

365 Figure 3 shows the differences between the measured outlet and inlet cation  
 366 concentrations, which makes it possible to discuss the stoichiometry of the dissolution  
 367 reaction (Fig. 3b). Aluminum depletion was observed in the fluid, as inferred from the  
 368 [Si]/[Al] ratio, which is more than ten times higher than its theoretical value (3.1), while  
 369 conversely, the [Al]/[K] ratio is very low (< 0.3) compared to its theoretical stoichiometric  
 370 value (1.3). As the [Si]/[K] ratios are systematically close to their theoretical stoichiometric  
 371 values (Fig. 3b), those results suggest that Al-rich secondary phases precipitated in these  
 372 experiments, which was confirmed by the characterizations of the run products (see section  
 373 3.2.3). The dissolution rates of orthoclase for these different experiments based on Si and K  
 374 concentrations were calculated, and are listed in Table 5.

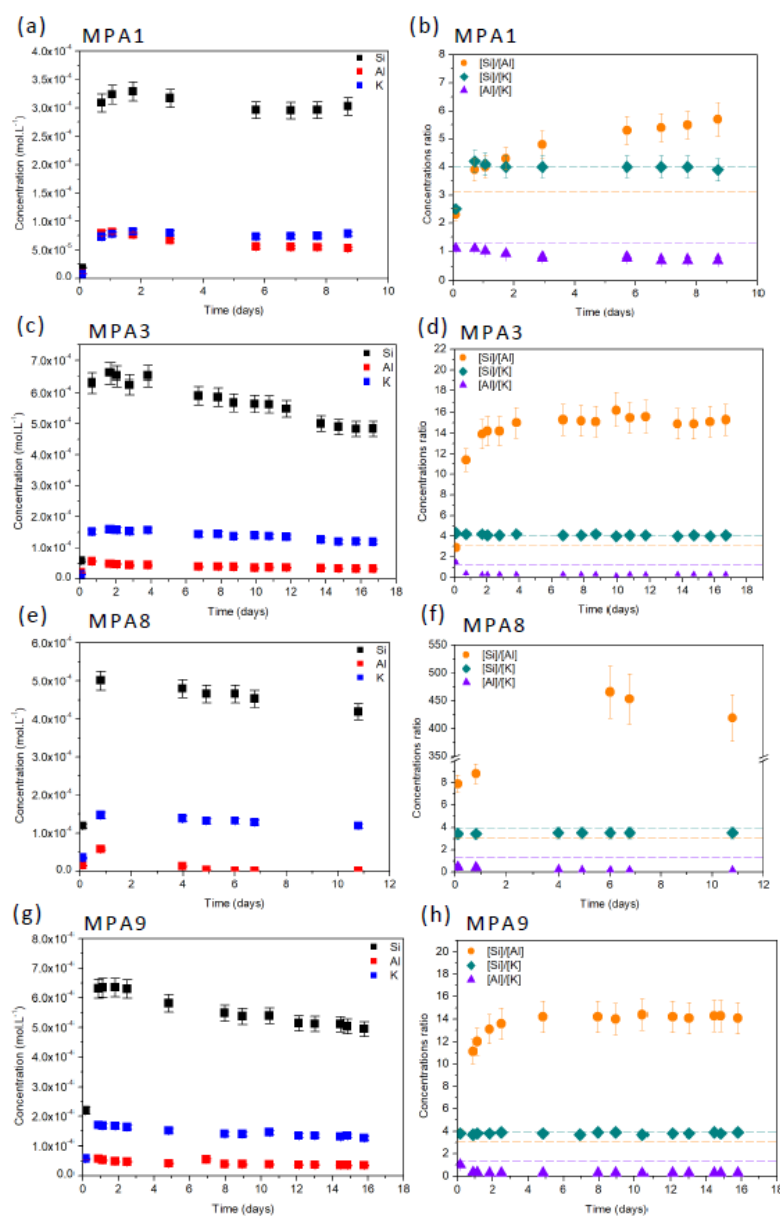
375 **Table 5. Orthoclase dissolution rates at 180 °C and pH > 2 measured from experiments MPA2,**  
 376 **MPA4, MPA5, MPA6 and MPA7 (MPA-pH>2).**

	pH	$\Delta G_r$ (kJ.mol <sup>-1</sup> )	[Al] (mol.L <sup>-1</sup> )	r (10 <sup>-7</sup> mol.m <sup>-2</sup> .s <sup>-1</sup> )
MPA2	3.1	-67	2.63E-07	0.39 ± 0.02
MPA4	4.3	-70	1.50E-07	0.16 ± 0.02
MPA5	4.7	-62	2.50E-06	0.11 ± 0.02
MPA6	3.8	-49	9.80E-06	0.27 ± 0.03
MPA7	3.0	-48	9.50E-07	0.47 ± 0.04

377 The pH, the Gibbs free energy of orthoclase dissolution ( $\Delta G_r$ ) and the average aluminum concentration are  
 378 listed here. These parameters can influence the dissolution rate.

379  
 380 *3.2.2 Results of MPA-pH2 experiments*

381 Figure 4 shows the evolution of concentrations measured in experiments MPA1, MPA3,  
 382 MPA8 and MPA9.



383

384 **Fig. 4. Time-resolved fluid analyses of MPA-pH2 experiments.** (a, c, e, g) Time-resolved concentrations of  
 385 released elements (outlet concentration subtracted from inlet concentration) and (b, d, f, h) ratios of these  
 386 concentrations. The dashed lines represent the theoretical values of the ratios calculated for stoichiometric  
 387 dissolution. The MPA-pH2 experiments were conducted at pH 2, under conditions supersaturated with respect to  
 388 Al-bearing phases. The [Si]/[Al] and [Al]/[K] ratios reveal a lack of Al in solution, resulting from boehmite  
 389 precipitation.

390

391 These experiments were carried out at pH = 2 using fresh powders, but under conditions  
 392 of supersaturation with respect to boehmite. The [Si]/[Al] and [Al]/[K] ratios indicate that the  
 393 solutions are depleted in Al, suggesting the precipitation of Al-rich secondary phases, which  
 394 was further confirmed by the characterizations of the run products (see section 3.2.3). The

395 dissolution rates of orthoclase for these different experiments based on Si and K  
 396 concentrations were calculated, and are listed in Table 6.

397 **Table 6. Orthoclase dissolution rates at 180 °C and pH 2 measured from experiments MPA1, MPA3,**  
 398 **MPA8 and MPA9 (MPA-pH2).**

	$\Delta Gr$ (kJ.mol <sup>-1</sup> )	[Al] (mol.L <sup>-1</sup> )	$r$ (10 <sup>-7</sup> mol.m <sup>-2</sup> .s <sup>-1</sup> )
MPA1	-72	6.42E-05	0.72 ± 0.03
MPA3	-66	3.40E-05	0.66 ± 0.07
MPA8	-64	3.50E-05	0.78 ± 0.07
MPA9	-63	4.14E-05	0.95 ± 0.07

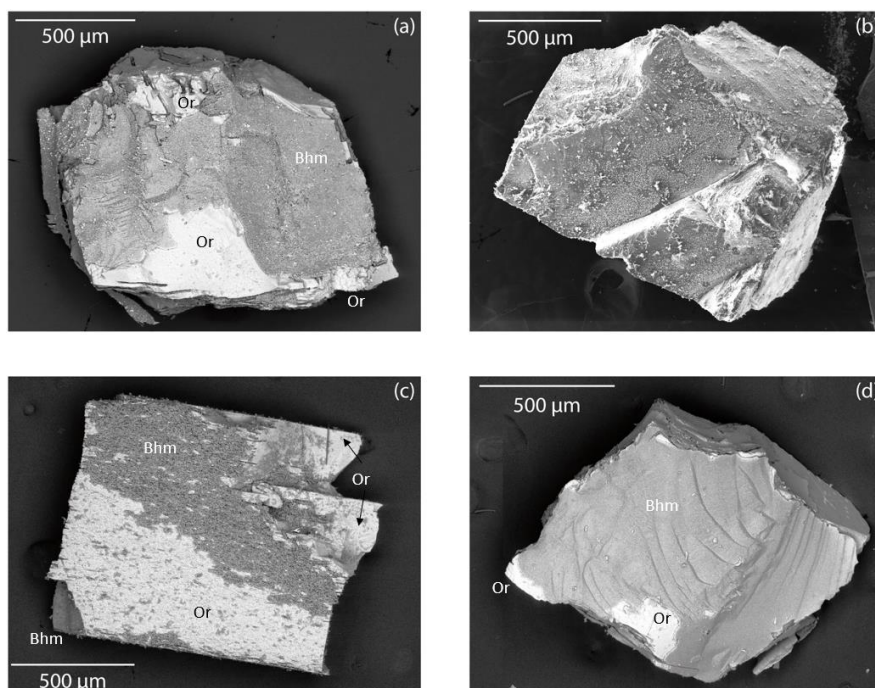
399 The average Al concentration and the Gibbs free energy of the reaction, two parameters known to impact the  
 400 dissolution rate, are listed.

401

### 402 3.2.3 Physicochemical properties of the coatings

#### 403 3.2.3.1 Coating identification and structure

404 Figure 5 provides an overview of some orthoclase grains representative of the run  
 405 products recovered at the end of the MPA experiments. It shows secondary precipitates  
 406 partially (Fig. 5a-c) or totally (Fig. 5d) covering the surface of orthoclase grains.



407

408 **Fig. 5. Representative images of grains from experiments MPA-pH>2.** The grains were collected from  
 409 experiments (a) MPA2, (b) MPA4, (c) MPA5 and (d) MPA6. SEM images were taken either in SE (5b) or BSE  
 410 (5a, c, d) mode. Orthoclase grains covered with secondary phase are visible. In the BSE images, the Al-rich  
 411 phases appear darker than orthoclase.

412 XRD analyses of the powders from the MPA experiments showed that all secondary  
 413 crystals consisted of boehmite (AlO(OH); see Fig. S6) whose chemical composition  
 414 determined by EDXS is identical in all experiments, and whose shape and size was found to  
 415 differ according to the chemical composition of the fluid (Fig. S7). This observation may be  
 416 related to the saturation state of the fluid, which is known to control the respective rates of  
 417 crystal nucleation and growth. If the fluid is only slightly supersaturated, the nucleation rate is  
 418 low and the crystal growth process prevails. On the other hand, when the fluid is highly  
 419 supersaturated, the nucleation process dominates at the expense of the growth process (see  
 420 [Daval et al., 2009b](#)). In this case, numerous small crystals are observed. Moreover, the growth  
 421 rates of the different faces of a crystal change as a function of the fluid saturation state, pH or  
 422 composition (e.g., [Dhanaraj et al., 2010](#); [Godinho and Stack, 2015](#); [Vital et al., 2020](#)),  
 423 possibly contributing to the diversity of crystal morphology revealed experimentally.

#### 424 3.2.3.2 Grain surface coverage and coating thickness

425 **Table 7. Main physical characterizations of boehmite coatings formed on orthoclase powders from MPA**  
 426 **experiments (i.e., proportion of the powder surface covered with coatings and thickness of the coatings).**

<b>Experiment</b>	<b>Duration (days)</b>	<b>pH</b>	<b>Coverage (%)</b>	<b>Thickness (<math>\mu\text{m}</math>)</b>
MPA1	9	2.1	$20 \pm 5$	$2.8 \pm 0.1$
MPA2	9	3.1	$30 \pm 5$	$2.2 \pm 0.1$
MPA3	17	2.1	$22 \pm 5$	$5.2 \pm 0.1$
MPA4	9	4.3	$1.4 \pm 0.5$	$0.8 \pm 0.1$
MPA5	19	4.7	$11 \pm 3$	$2.6 \pm 0.1$
MPA6	12	3.8	$98 \pm 2$	$1.2 \pm 0.1$
MPA7	9	3.0	$55 \pm 5$	$1.3 \pm 0.1$
MPA8	11	2.1	$58 \pm 5$	$3.9 \pm 0.1$
MPA9	16	2.1	$7 \pm 3$	$4.9 \pm 0.1$

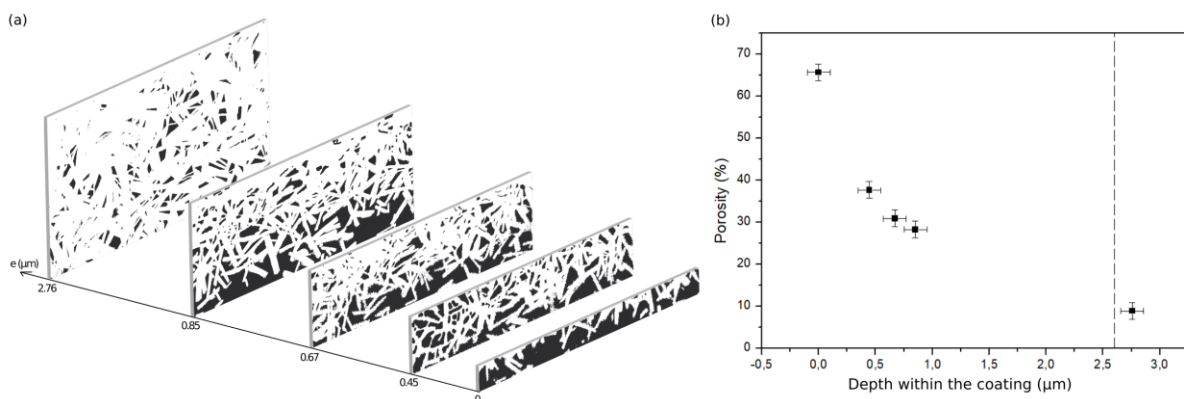
427  
 428 The proportion of orthoclase powders covered by boehmite crystals as well as the  
 429 thickness of the coatings are listed in Table 7. A strong correlation between reaction time and  
 430 coating thickness was observed: for experiments carried out at pH 2, a linear relationship can  
 431 be noticed between coating thickness and reaction time (Fig. S8). In addition, the lower the  
 432 pH, the thicker the coatings. This later observation is consistent with the fact that the

433 dissolution rate of K-feldspar decreases when pH increases in the acidic pH range (Palandri  
434 and Kharaka, 2004), resulting in a larger release of Al for lower pHs.

435 Of note, some secondary coatings have proved brittle and do not stick firmly to the  
436 surface of orthoclase grains. Figure S9 shows that coatings sometimes partially detached from  
437 the surface of orthoclase grains. This was observed in particular in the MPA1, MPA3 and  
438 MPA9 experiments carried out at pH 2. As a result, the extent of coverage may be  
439 underestimated for these experiments. Of note, the powders recovered at the highest  
440 temperature (i.e. 95 °C, see section 2.2), with the exception of experiment MPA9, are those  
441 with the highest proportion of coatings. This might indicate that recovering powders at room  
442 temperature (the temperature at which boehmite is the most soluble) would partially damage  
443 the coatings. Finally, no clear correlation between the proportion of coverage and reaction  
444 time could be evidenced, a result which may be related to the brittleness and delamination of  
445 certain coatings.

#### 446 3.2.3.3 Coating porosity

447 Porosity was measured on coatings from experiments MPA3 (conducted at pH 2),  
448 corresponding to the thickest coating, and MPA6 (conducted at pH 3.8), which exhibited  
449 almost 100% coverage.



450

451 **Fig. 6. An example of characterization of the porosity of boehmite coatings precipitated on orthoclase**  
452 **grains from MPA3 experiment.** (a) Images of successive FIB cuts made in the secondary phase coating  
453 present on orthoclase grains. The  $e$  axis represents the coating thickness at which the cuts were made. The  
454 images were processed (grayscale thresholding) using ImageJ software to determine the porosity of the coating.

455 In the images, secondary phases appear in white and pores in black. (b) Porosity evolution within the boehmite  
456 coating formed on the grains in the MPA3 experiment. The coating has a total thickness of 5.2  $\mu\text{m}$ . The dotted  
457 line represents the center of the coating. The point at  $x = 0 \mu\text{m}$  is at located at the contact with the solution.

458

459 Measurements were taken as a function of coating thickness on the grains from  
460 experiment MPA3, but only on the first half of the coating depth (Fig. 6a). The closer to the  
461 center of the coating, the lower the porosity (Fig. 6b). In contrast, the thickness of the coating  
462 on the grains from the MPA6 experiment is too thin for depth-dependent measurements. As a  
463 consequence, for this experiment, an average porosity was measured from the various cross-  
464 sections made within the coatings, and estimated at  $22 \pm 5\%$  on average.

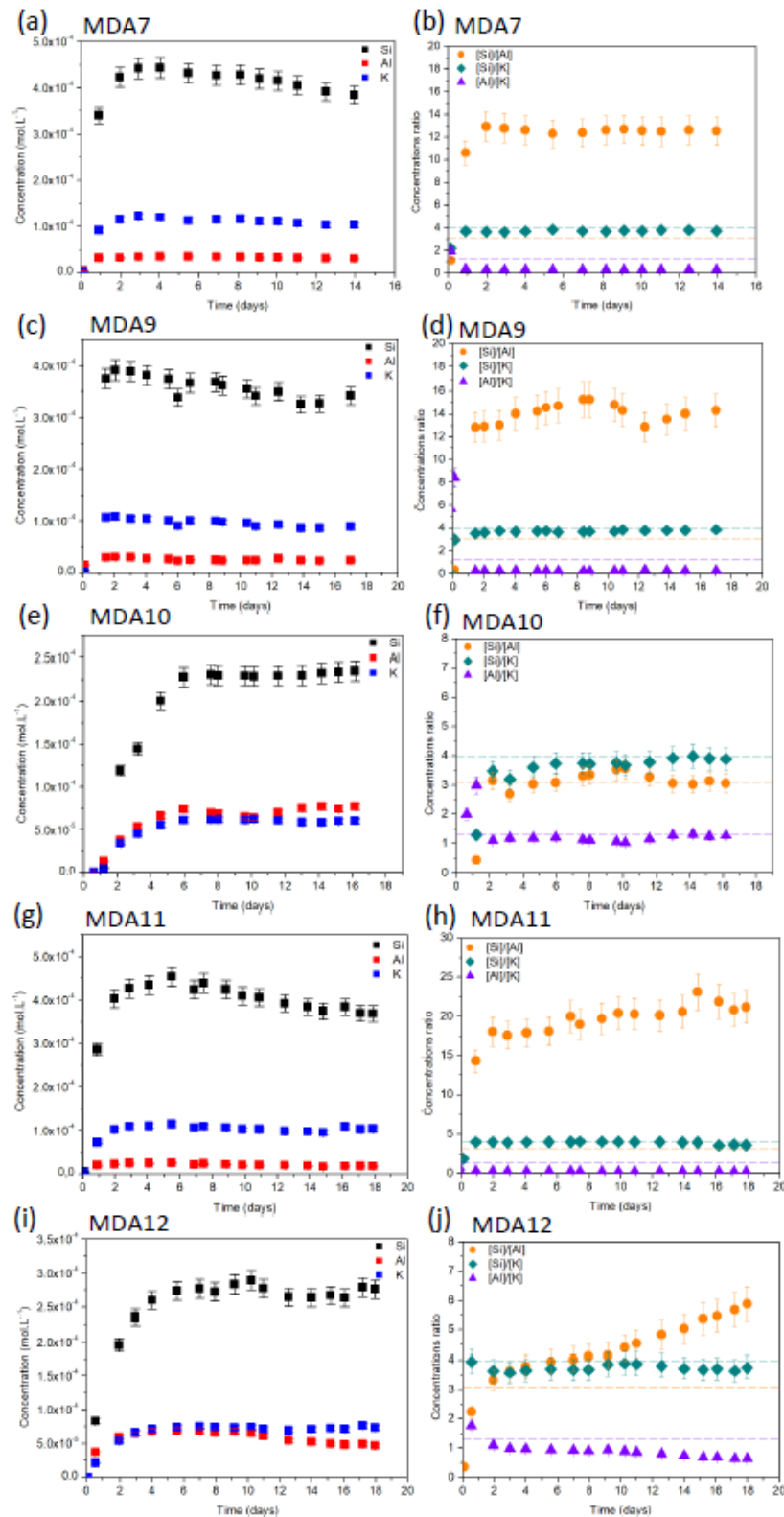
465 In the next section, the results of dissolution experiments carried out at pH 2 on powders  
466 initially coated with boehmite (experiment MDAc) are described. These powders were  
467 recovered from experiments MPA2, MPA4, MPA5, MPA6 and MPA7 (MPA-pH>2).

### 468 **3.3 Experiments conducted at pH 2 on boehmite-coated powders in solutions** 469 **supersaturated with respect to secondary phases (experiments MDAc).**

#### 470 *3.3.1 Dissolution rates*

471 Figure 7 shows the concentrations of elements released from orthoclase dissolution in the  
472 MDAc experiments. The Al concentration in experiments MDA7, MDA9 and MDA11 was  
473 found to be very low. The [Si]/[Al] and [Al]/[K] ratios do not correspond to the stoichiometric  
474 ratios of orthoclase (Fig. 7b), indicating the precipitation of Al-rich secondary phases.  
475 Conversely, the [Si]/[Al] and [Al]/[K] ratios of the MDA10 experiment are close to their  
476 theoretical stoichiometric ratios, indicating that no massive reprecipitation of secondary  
477 phases took place in this experiment. Finally, experiment MDA12 shows a drop in Al  
478 concentration after  $\sim 10$  days, which may correspond to the onset of Al-bearing phase  
479 precipitation. From the measured Si and K concentrations, the dissolution rates of orthoclase  
480 dissolution were calculated for all experiments, and are listed in Table 8.





481

482 **Fig. 7. Time-resolved fluid analyses of MDAc experiments.** (a, c, e, g, i) Time-resolved concentrations of  
 483 released elements (outlet concentration subtracted from inlet concentration) and (b, d, f, h, j) ratios of these  
 484 concentrations. The dashed lines represent the theoretical values of the ratios calculated for stoichiometric  
 485 dissolution. The MDAc experiments were carried out at pH 2 and under conditions supersaturated with respect to  
 486 Al-bearing phases. The [Si]/[Al] and [Al]/[K] ratios reveal a lack of Al, resulting from boehmite precipitation.

487 **Table 8. Measured dissolution rates for MDAC experiments conducted at pH 2, using powders covered**  
 488 **with boehmite coatings resulting from MPA-pH>2 experiments.**

Experiment	Starting materials	$\Delta Gr$ (kJ.mol <sup>-1</sup> )	[Al] (mol.L <sup>-1</sup> )	r (10 <sup>-7</sup> mol.m <sup>-2</sup> .s <sup>-1</sup> )
MDA7	MPA6	-69	5.92E-05	0.64 ± 0.05
MDA9	MPA5	-71	4.29E-05	0.60 ± 0.05
MDA10	MPA7	-74	7.52E-05	0.36 ± 0.02
MDA11	MPA4	-78	4.51E-05	0.70 ± 0.04
MDA12	MPA2	-72	6.80E-05	0.46 ± 0.02

489 The starting powders are indicated in the second column. In the last three columns, the Gibbs free energy of  
 490 orthoclase dissolution, the Al concentration and the dissolution rates are listed.

491

### 492 *3.3.2 Coating properties at the end of the experiments*

493 At the end of the MDAC experiments, the powders were analyzed by SEM (Fig. S10).

494 The extent of grain coverage after the MDAC experiments is below 10%, and virtually zero

495 for some powders (e.g. Fig. S10a). The powders used for the MDAC experiments are those

496 issued from the MPA-pH>2 experiments. It can be seen that the grains had a greater coverage

497 before their re-dissolution at pH 2 (Table 7 and Figure 5). This would therefore indicate that

498 part of the boehmite coating was lost either during the MDAC experiments or at the end of the

499 experiments. However, both the aqueous elemental ratios and the thermodynamic calculations

500 based on Al concentration (Fig. 7) indicate that Al-rich phases did indeed precipitate during

501 the MDAC experiments. Two hypotheses can be offered to explain these observations:

502 (1) Secondary coatings came off before or during the MDAC experiments. New precipitates

503 were formed in the autoclave, but not at the surface of orthoclase grains;

504 (2) The coatings came off at the end of the MDAC experiments, during recovery of the run

505 products.

506 As a consequence, one has to keep in mind that the interpretations of these experiments

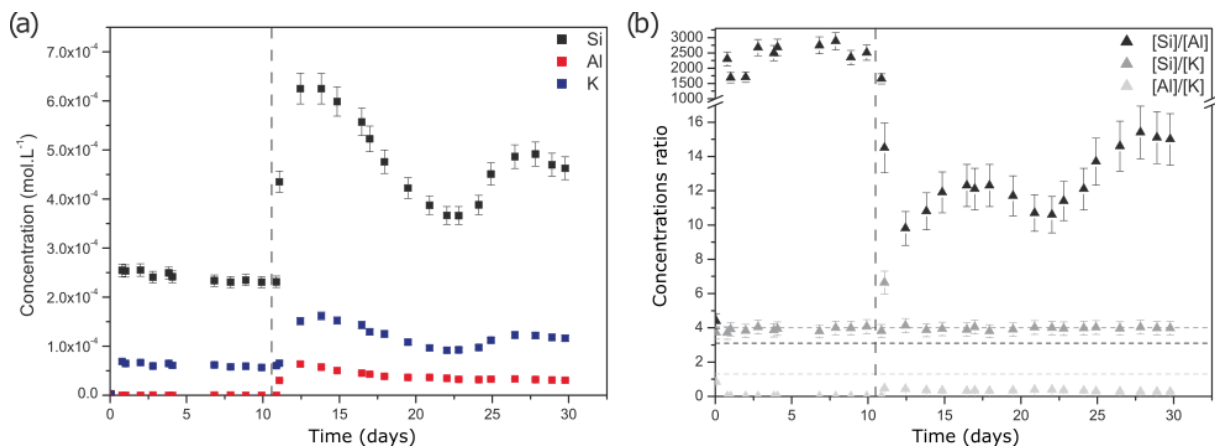
507 will differ depending on the actual scenario that took place during the experiments. Indeed, it

508 is possible that the dissolution rates measured during the MDAC experiments are relative to

509 boehmite-coated powders or not. The MPDA experiment was designed to circumvent these  
510 problems.

### 511 3.4 MPDA experiment

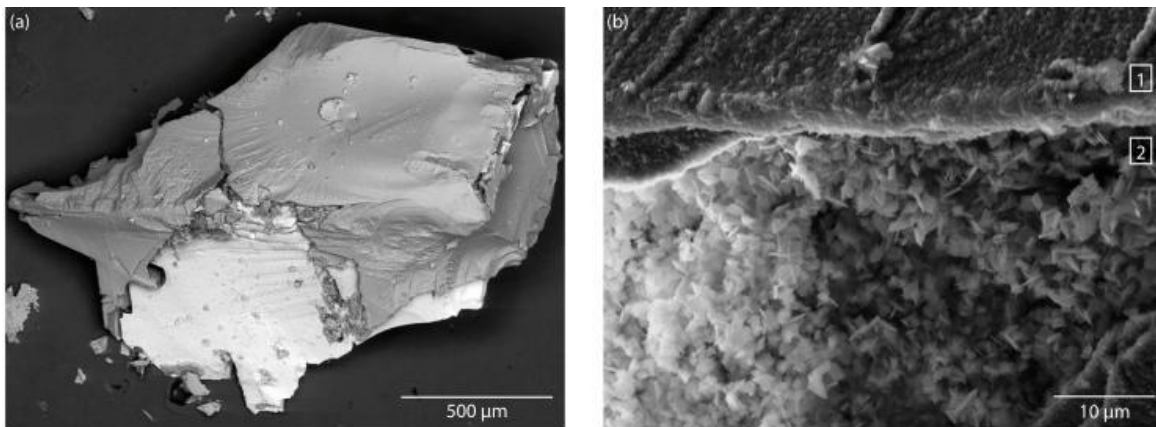
512 Figure 8a shows the concentrations of elements released during orthoclase dissolution,  
513 together with the ratios of these concentrations. Two stages (referred to as MPDAa and  
514 MPDAb) can be clearly distinguished during the experiment. The first one corresponds to the  
515 alteration of orthoclase at pH 4 in a solution highly supersaturated with respect to aluminum  
516 hydroxides. The second one, which began 11 days after the onset of the experiment,  
517 corresponds to the dissolution of the powder at pH 2. Concentrations were found to be higher  
518 in the MPDAb stage, as orthoclase dissolution rate is higher at pH 2 than at pH 4. However,  
519 while a steady-state can be observed during the MPDAa phase, sharp variations in  
520 concentrations were observed at the end of the experiment. These variations may be due to the  
521 precipitation/redissolution of other secondary phases containing Si and K, or to the possibility  
522 that the dissolution rate of orthoclase is not constant under these conditions.



523  
524 **Fig. 8. Time-resolved fluid analyses of MPDA experiment.** (a) Time-resolved concentrations of released  
525 elements (outlet concentration subtracted from inlet concentration) and (b) ratios of these concentrations.  
526 The dashed lines represent the theoretical values of the ratios calculated for stoichiometric dissolution.

527  
528 Figure 8b shows that stoichiometry was respected for Si and K concentrations. On the  
529 other hand, Al was released incongruently, suggesting its precipitation in secondary phases

530 throughout the experiment. Typical orthoclase grains representative of the run products at the  
531 end of the MPDA experiment are shown in Fig. 9. The grains are almost totally covered with  
532 boehmite (90% surface coverage), suggesting that powder handling at the end of the  
533 experiment may not affect the extent of the grain coverage. Although these observations do  
534 not allow us to draw definitive conclusions with respect to the (at least partial) lack of  
535 coatings in the MDAc experiments, it thus seems impossible to rule out the possibility that the  
536 coatings were damaged during the MDAc experiments, and more particularly when they were  
537 introduced into the reactor at the start of the experiment (hypothesis 1, section 3.3.2). The  
538 presence of the coatings during the MDAc experiments therefore remains uncertain.



539  
540 **Fig. 9. SEM images of grains from the MPDA experiment.** (a) BSE image of orthoclase grains are  
541 heavily coated with secondary phases. (b) SE image at higher magnification of secondary coatings.  
542 Two different textures (marked 1 and 2), already observed in the MPA experiments (Fig. S7), can be  
543 evidenced.

544  
545 Referring back to the MPDA experiment, the crystals that make up the coatings were  
546 observed to have two different sizes and morphologies (Fig. 9b), which were already  
547 observed in the MPA experiments (Fig. S7). These differences may be ascribed to the  
548 precipitation of two successive generations of boehmite coatings formed at pH 4 and pH 2,  
549 respectively. Their thickness was measured to be  $2.0 \pm 0.2 \mu\text{m}$  on average. No secondary  
550 phases other than boehmite was detected in the run products. This observation implies that the  
551 variations in concentration observed during the MPDA step can only be linked to a variation

552 in the rate of orthoclase dissolution. This variation may be due to the successive  
553 precipitation/dissolution of boehmite during the experiment.

554 Based on the measured concentrations, the average dissolution rate of orthoclase during  
555 the first stage of the experiment (performed at pH 4) is estimated at  $(0.27 \pm 0.01) \times 10^{-7}$   
556  $\text{mol.m}^{-2}.\text{s}^{-1}$ . Despite the variations in concentration observed during the second step performed  
557 at pH 2, the dissolution rate of orthoclase under these conditions can be estimated to range  
558 between  $0.42 \times 10^{-7}$  and  $0.68 \times 10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ , with a mean value of  $(0.54 \pm 0.09) \times 10^{-7}$   
559  $\text{mol.m}^{-2}.\text{s}^{-1}$  (the error corresponds to the standard deviation of the measurements made).

### 560 **3.5 Brief summary of the results**

561 In the MPA experiments, boehmite coatings formed on the surface of orthoclase grains.  
562 By varying pH and/or reaction time, coatings of different texture, thickness and surface  
563 coverage were formed. A comparison of dissolution rates measured at pH 2 on coated  
564 powders (experiments MPA-pH2, MDAc and MPDA) and powders not coated with  
565 secondary phases (experiments MD Af) provides information on the effect of coatings on  
566 orthoclase dissolution kinetics.

567 When the powders were recovered at the end of the MDAc experiments, most of the  
568 grains were no longer coated with secondary phases. The coatings may have dissolved or  
569 detached from the grains during the dissolution experiments or when the powders were  
570 collected at the end of the experiments. Uncertainty therefore remains as to the presence of  
571 coatings during these experiments. On the other hand, boehmite coatings were found at the  
572 end of the MPA-pH2 and MPDA experiments.

573 The dissolution rates measured for each series of experiments are listed in Table 9. It can  
574 be seen that dissolution rates measured on fresh powder in the absence of secondary coatings  
575 (experiments MD Af) are higher than those measured on boehmite-coated powders. The  
576 coating of secondary phases could therefore be responsible for a drop in the dissolution rate of

577 orthoclase. However, other factors, such as the chemical affinity of the reaction and the  
578 aluminum concentration in the reactor, can also result in a drop in reactivity. The influence of  
579 each of these parameters is discussed below.

580

581 **Table 9. A summary of orthoclase dissolution rates measured during the different series of experiments**  
582 **carried out at 180 °C and pH 2. The**

<b>Experiment</b>	<b>r (10<sup>-7</sup> mol.m<sup>-2</sup>.s<sup>-1</sup>)</b>
MDAf	0.90 – 1.30
MPA-pH2	0.66 – 0.95
MDAc	0.36 – 0.70
MPDAb	0.42 – 0.68

583 MDAf experiments were conducted using fresh powders, in the absence of secondary phases. In the MPA-pH2  
584 experiments, boehmite precipitated on the surface of orthoclase grains. The MDAc experiments were carried out  
585 on powders coated beforehand with boehmite. The MPDAb experiment corresponds to the alteration of  
586 boehmite-coated powder in which the grains were not dried or manipulated between the coating formation stage  
587 and the dissolution stage at pH 2.

588

## 589 **4. Discussion**

590 In this study, variations in the dissolution rate of orthoclase may be due to the presence of  
591 secondary phases, which could mask part of the reactive surface of the grains and/or favor the  
592 development of microenvironments with fluid composition deviating from that of the bulk  
593 fluid. However, two other parameters, i.e., the Gibbs free energy ( $\Delta G_r$ ) of the reaction (Burch  
594 et al., 1993; Gautier et al., 1994; Hellmann and Tisserand, 2006; Hellmann et al., 2010;  
595 Pollet-Villard et al., 2016b) and the Al concentration in the bulk fluid (Gautier et al., 1994;  
596 Oelkers et al., 1994) may have also contributed to the rate decrease. These hypotheses are  
597 discussed below.

### 598 **4.1 Influence of the Gibbs free energy of reaction on orthoclase dissolution rate**

599 For over 30 years, several studies have demonstrated that mineral dissolution rates do not  
600 simply follow rate laws derived from the transition state theory (TST). Whereas TST-based

601 rate laws predict that the dissolution rate of a given chemical process is virtually unaffected  
602 by the distance to equilibrium as long as  $\Delta G_r < \sim -20$  kJ/mol, a dramatic drop in the  
603 dissolution rate was actually observed experimentally for various minerals at much lower  
604 values (Daval et al., 2010; Taylor et al., 2000; Burch et al., 1993; Hellmann and Tisserand,  
605 2006; Hellmann et al., 2010). Regarding orthoclase, Pollet-Villard et al., 2016a suggested that  
606 a drop in orthoclase dissolution rate could be observed for values as low as  $\sim -68$  kJ.mol<sup>-1</sup>.

607 In the MD Af experiments, the Gibbs free energy of orthoclase dissolution is consistently  
608 below -110 kJ.mol<sup>-1</sup>. There is therefore no influence of  $\Delta G_r$  on the dissolution rates calculated  
609 in these experiments. Regarding MPA-pH2 experiments,  $\Delta G_r$  varies from -72 to -63 kJ.mol<sup>-1</sup>.  
610 Accordingly, this variation can only result in a very modest decrease in reactivity, on the  
611 order of 1% at most, based on the empirical relations proposed in Pollet-Villard et al., 2016a.  
612 Such an impact remains much lower than the uncertainties on measured concentrations (5-  
613 10%). Finally, all MD Ac experiments and the MPDA experiment (second step) were carried  
614 out at  $\Delta G_r \leq -67$  kJ.mol<sup>-1</sup>, such that the fluid saturation state should have not influenced  
615 orthoclase dissolution rate.

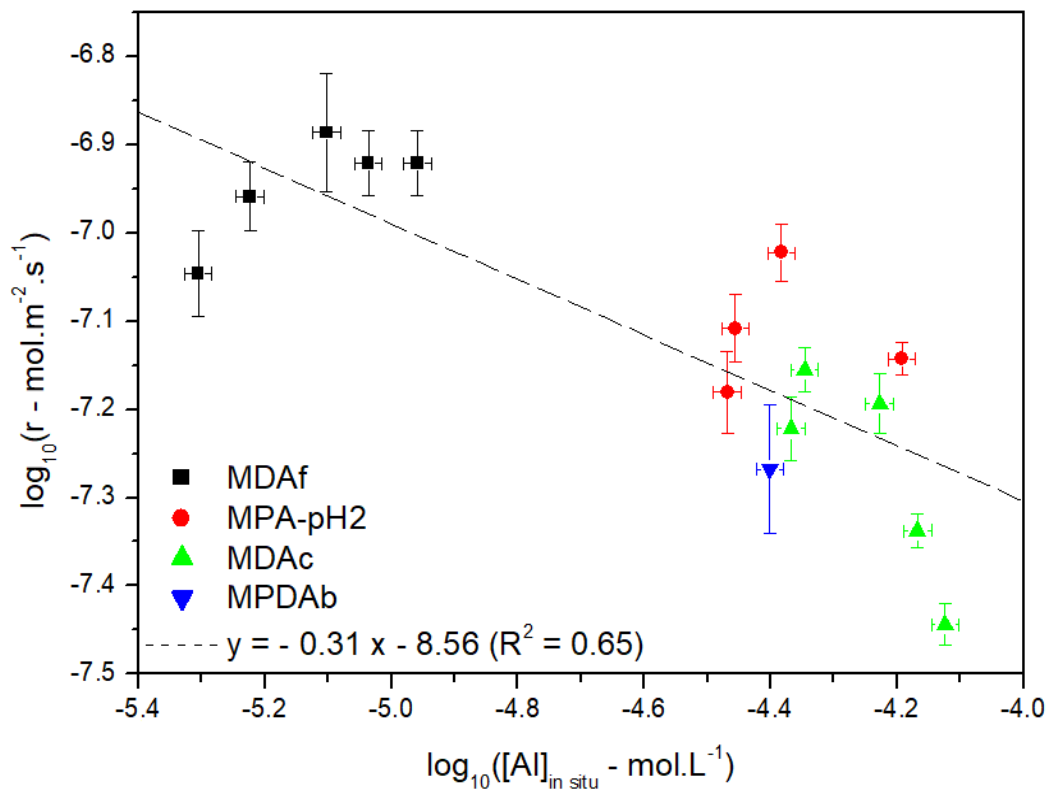
616 Overall, it can therefore be concluded that any difference in terms of orthoclase reactivity  
617 between the various experiments could not be ascribed to the Gibbs free energy of orthoclase  
618 dissolution.

#### 619 **4.2 Influence of aqueous Al concentration on orthoclase dissolution rates**

620 According to several studies, aqueous Al may inhibit the dissolution rate of feldspars  
621 (e.g., Gautier et al., 1994; Oelkers et al., 1994; Oelkers, 2001). At far from equilibrium  
622 conditions and in the acidic pH domain, the dependence of feldspar dissolution rate on the  
623 activity of Al<sup>3+</sup> has been suggested to observe:

$$r = k_d \cdot \left( \frac{a_{H^+}}{a_{Al^{3+}}} \right)^q \quad (5)$$

624 where  $a_i$  represents the activity of species  $i$  and  $k_d$  a dissolution constant. The value of  $q$  was  
 625 proposed to depend on the stoichiometry of a so-called ‘activated complex’ or ‘surface  
 626 precursor’, with a value equal to  $-1/3$  for K-feldspar (Gautier et al., 1994). To test the possible  
 627 impact of Al in our experiments, the logarithm of the dissolution rate was plotted as a  
 628 function of the logarithm of Al concentration measured in the solution (Fig. 10). The rate data  
 629 observe a negative correlation with Al concentration. Despite a rather low correlation  
 630 coefficient ( $R^2 = 0.65$ ), the slope of the linear regression ( $-0.31$ ) is in very good agreement  
 631 with the value of  $-1/3$  predicted by Eq. (5).



632  
 633 **Fig. 10. Logarithm of orthoclase dissolution rates measured at pH 2 as a function of the**  
 634 **logarithm of Al concentration in solution.** The dashed line corresponds to a linear regression of the  
 635 data. The slope of the line is equal to  $-0.31$ . According to Gautier et al., 1994, the theoretical value of  
 636 the slope is equal to  $-1/3$ . See text for details.

637  
 638 To better appreciate the contribution of Al aqueous concentration on orthoclase  
 639 reactivity, dissolution rates were recalculated using Eq. (5) and an arbitrary Al concentration  
 640 equal to  $10^{-5} \text{ mol.L}^{-1}$  (Table 10). As can be seen, whereas the recalculated dissolution rate of



641 fresh orthoclase powders (i.e., not covered with secondary coatings) range from  $0.9$  to  $1.2 \times$   
642  $10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ , the recalculated dissolution rates of coated orthoclase powders range from  
643  $0.7$  to  $1.5 \times 10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ . With the possible exception of experiment MDA10, if aqueous  
644 Al does contribute to the decline in orthoclase reactivity, then the dissolution rate of fresh and  
645 coated powders overlap. Therefore, and although it should be reminded that the theoretical  
646 and experimental validity of Eq. (5) has been extensively questioned in the literature (e.g.,  
647 [Luttge, 2006](#)), it follows from such calculations that the effect of secondary coatings could be  
648 considered negligible. In the next section we test whether the slight difference in reactivity  
649 between coated and uncoated orthoclase powders could alternatively be explained by some  
650 physical characteristics of the secondary coatings.

651 **Table 10. Orthoclase dissolution rates at 180°C and pH 2 measured from MD Af, MPA-pH2, MD Ac and**  
652 **MPDA experiments and recalculated for an Al concentration of  $10^{-5} \text{ mol.L}^{-1}$  using Eq. (5).**

Experiment		$r_{\text{corr}}$ ( $10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ )
MD Af	MDA3	$1.2 \pm 0.1$
	MDA4	$1.2 \pm 0.1$
	MDA5	$1.2 \pm 0.2$
	MDA6	$0.7 \pm 0.1$
	MDA8	$0.9 \pm 0.1$
MPA-pH2	MPA1	$1.30 \pm 0.03$
	MPA3	$1.00 \pm 0.07$
	MPA8	$1.20 \pm 0.07$
	MPA9	$1.50 \pm 0.07$
MD Ac	MDA7	$1.16 \pm 0.05$
	MDA9	$0.97 \pm 0.05$
	MDA10	$0.71 \pm 0.02$
	MDA11	$1.16 \pm 0.04$
	MDA12	$0.87 \pm 0.02$
MPDA	MPDAb	$0.86 \pm 0.09$

653

### 654 **4.3 Influence of coatings on orthoclase dissolution rates**

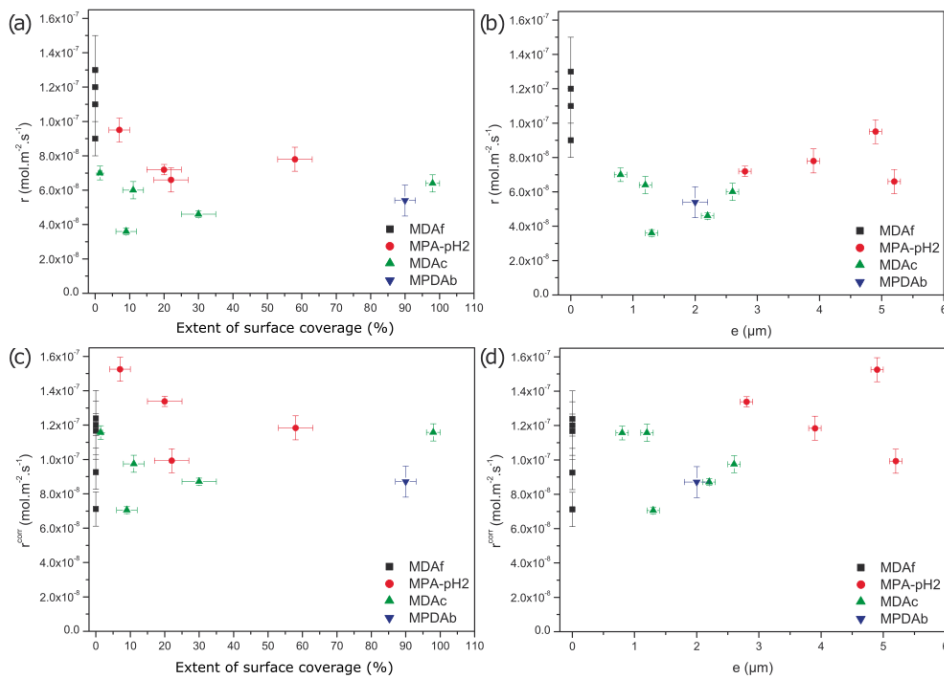
655 To highlight a possible relation between orthoclase reactivity and the presence of  
656 secondary coatings, graphs representing the rates of orthoclase dissolution, using rates either

657 uncorrected for the impact of Al ( $r$ ) or taking into account a possible impact of Al ( $r_{corr}$ ), were  
658 plotted as a function of the proportion of surface covered and the thickness  $e$  of the coatings  
659 respectively, both measured at the end of the experiments (Fig. 11). Note that the MDAf  
660 experiments (black squares in Fig. 11) were carried out in the absence of secondary phases  
661 throughout the experiments while conversely, the MPA-pH2 experiments (red circles) were  
662 free of coatings only at the beginning of the experiments. In contrast, the MDAc experiments  
663 (green triangles) were carried out on powders initially covered with secondary phases  
664 (starting powders coming from the MPA-pH>2 experiments).

665 Overall, the dissolution rate of coated powders is generally lower than the dissolution  
666 rates measured in the absence of a secondary phases, with an apparent decrease in reactivity  
667 of around 44% (Figs. 11a and b). Conversely, and as suggested in the previous section,  
668 accounting for a possible impact of Al on orthoclase reactivity results in dissolution rates that  
669 no longer depend on the properties of the orthoclase powders (coated with secondary coatings  
670 or not). No clear trend that would relate the dissolution rates to the proportion of surface  
671 covered and/or the thickness  $e$  of the coatings can be evidenced.

672 Overall, the results suggest that secondary phases formed on orthoclase grains have no  
673 major influence on dissolution rates. A modest decrease in reactivity of the order of 40% is  
674 observed when the grains are covered with boehmite, which could also be attributed to the  
675 inhibiting effect of aluminum in solution. Interestingly, the present study confirms the results  
676 reported in several previous experimental efforts focused on coupled dissolution-precipitation  
677 reactions. For instance, [Hellmann et al., 1989](#) observed that the formation of 100s  $\mu\text{m}$ -thick  
678 boehmite coatings on albite crystals altered at pH 2.4 and 300 °C had a negligible impact on  
679 albite dissolution rates. Studies aimed at unravelling the impact of carbonate formation  
680 throughout water-silicate-CO<sub>2</sub> interactions on the rate and yield of silicate carbonation have  
681 also reported only a modest decrease in silicate reactivity (e.g., [Stockmann et al., 2008](#); [Daval](#)

682 et al., 2009a; Stockmann et al., 2011; Saldi et al., 2013; Stockmann et al., 2013). For all those  
 683 studies, including the present one, a striking common feature is the lack of crystallographic  
 684 relationship between the parent phase and the secondary phases, whereas Cubillas et al., 2005  
 685 proposed that a crystallographic template adapted for epitaxial growth could be a prerequisite  
 686 to efficiently decreasing primary mineral dissolution rates. Contrasting with this suggestion,  
 687 the reactive-transport simulations conducted by Emmanuel, 2022 showed that some properties  
 688 of the coatings that are not related to the crystalline structure of the parent phase and/or the  
 689 secondary coatings are critical in controlling the reactivity of the parent phase and in  
 690 particular, (i) the thickness and (ii) the porosity/tortuosity ratio inside the coatings. Following  
 691 a similar approach, we explore numerically in the next section whether the specific physical  
 692 properties of the boehmite coatings reported above were likely to act as a barrier to ion  
 693 diffusion from mineral to solution (and vice versa), and thus assess independently the impact  
 694 of these coatings on orthoclase dissolution rates.



695  
 696 **Fig. 11. Relation between dissolution rates  $r$  measured at pH 2 and (a) the extent of surface**  
 697 **coverage and (b) coating thickness  $e$  ( $\mu\text{m}$ ).** The same graphs ((c) and (d)) were plotted considering  
 698  $r_{corr}$  instead of  $r$ , which have been recalculated at an Al concentration arbitrarily set at a value of  $10^{-5}$   
 699  $\text{mol.L}^{-1}$ .

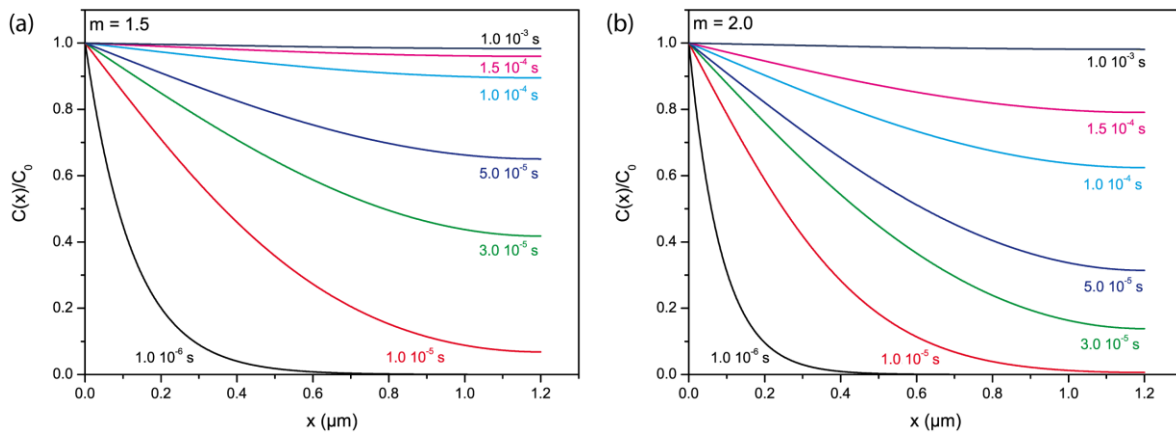
#### 4.4 Contribution of reactive transport modeling

As mentioned above, the secondary coatings formed on the surface of orthoclase do not seem to act as a diffusion barrier, nor isolate the orthoclase surface from the bulk fluid, as suggested by the modest decrease in K-feldspar reactivity measured experimentally (see Sections 4.1-4.3). The question arises as to whether such results are compatible with and/or could have been predicted based on the physical properties of the coatings. The 1D reactive transport model described in Section 2.4 and parameterized following the physical characterizations described above was used to address this question. The simulations were used to calculate the flux of  $H^+$  ions through the coatings and estimate the characteristic time required for  $H^+$  ions to pass through the coatings, as well as the pH at the boundary between the primary mineral and the coating. An estimate of the apparent dissolution rate of the mineral could then be calculated as a function of the coatings' characteristics of experiments MPA6 and MPA3, for which the characterization of the coatings was the most extensive. Finally, the model was also used to explain why coatings may significantly affect very reactive phases such as calcite, while their effect on orthoclase alteration is negligible.

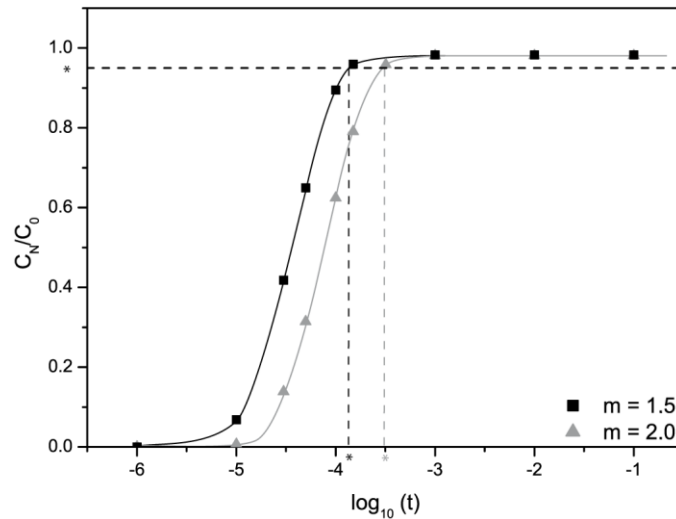
##### 4.4.1 Model outputs for experiment MPA6

Regarding experiment MPA6, both the porosity  $\phi$  and the effective diffusion coefficient  $D$  were assumed to be constant within the coating. With a porosity of 22%, the effective coefficients  $D_{m=2.0}$  and  $D_{m=1.5}$  are equal to  $1.6 \times 10^{-9}$  and  $3.4 \times 10^{-9} \text{ m}^2 \cdot \text{s}^{-1}$ , respectively (Eq. 3). Figure 12 shows the  $H^+$  concentration profiles ( $C(x)$ ) within the coating for different times  $t$ , both for  $m = 1.5$  and  $m = 2$ . In addition, the evolution of  $H^+$  concentration as a function of time in the  $C_N$  cell, which is in contact with orthoclase, is depicted in Figure 13. It can be seen that the proton concentration in the coating quickly reaches a steady state (for  $t < 1 \text{ ms}$ ). The concentration in the cell in contact with orthoclase ( $C_N$ ) then reaches a steady-state value corresponding to  $0.98C_0$ , i.e.,  $\text{pH} = 2.01$  (using  $\text{pH}_0 = 2.00$ ). Assuming that the dissolution

725 rate of orthoclase at pH 2.00 is  $r_0 = 1.00 \times 10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ , the dissolution rate of orthoclase  
 726 coated with secondary phases would be  $0.99 \times 10^{-7} \text{ mol.m}^{-2}.\text{s}^{-1}$ , considering a reaction order of  
 727  $n = 0.5$  with respect to  $a_{H^+}$ . Under these conditions, the decrease in reactivity would be too  
 728 weak to be detected. Therefore, the model constrained with the physical properties of the  
 729 secondary coatings independently confirms the conclusions reached in the previous sections:  
 730 the impact of secondary coatings was negligible throughout the experiment.



731  
 732 **Fig. 12. Evolution of the  $C(x)/C_0$  ratio in the coating of experiment MPA6 at different times  $t$  (s),**  
 733 **for simulations performed with (a)  $m = 1.5$  and (b)  $m = 2.0$ , respectively.**  
 734

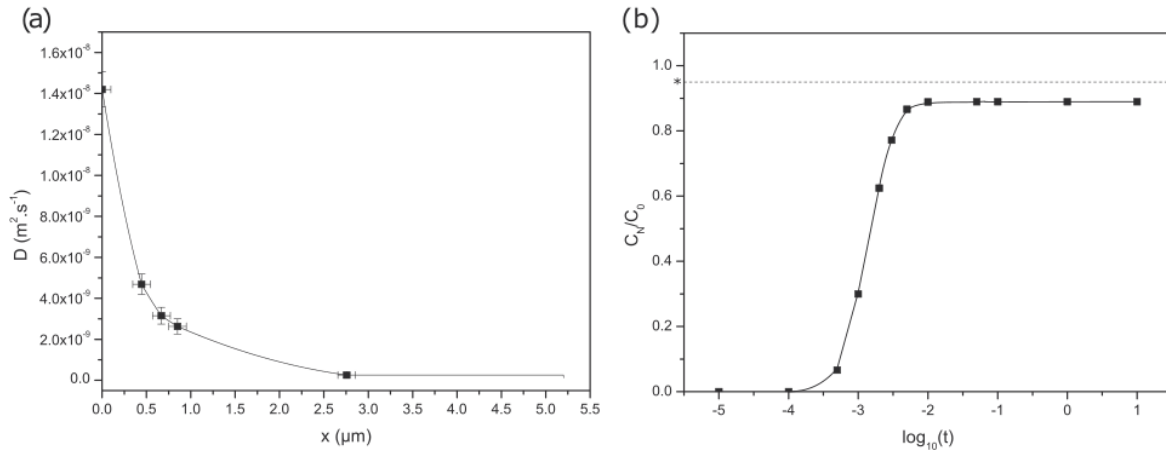


735  
 736 **Fig. 13. Evolution of the  $C_N / C_0$  ratio as a function of  $\log(t)$  for  $m = 1.5$  (black curve) and  $m =$**   
 737  **$2.0$  (gray curve).  $C_N$  represents the  $H^+$  concentration in the last  $N$  cell of the coating,  $t$  (s) is the**  
 738 **diffusion time within the coating. The star (\*) marks the time after which  $C = 0.95C_0$ .**  
 739

740 In addition, because the choice of  $m$  has little influence on the results, we have chosen to run  
741 the subsequent simulations with  $m = 2.0$ . This corresponds to the case where  $D$  is the lowest,  
742 and therefore, the condition under which the buildup of a diffusion boundary layer within the  
743 coating is the most likely.

#### 744 *4.4.2 Model outputs for experiment MPA3*

745 In the MPA3 experiment, porosity decreases from the coating/fluid interface inwards  
746 (Fig. 6b). Note that the porosity of the coating at a depth exceeding  $2.6 \mu\text{m}$  could not be  
747 measured. For the numerical simulations, it was assumed that for  $x > 2.6 \mu\text{m}$ , the porosity  
748 remained equal and constant to that measured at  $x = 2.6 \mu\text{m}$ . The profile of the effective  
749 diffusion coefficient  $D(x)$  within the coating (Fig. 14a) was then calculated from Archie's law  
750 (Eq. 3). Under such conditions, when the  $\text{H}^+$  concentration profile reaches steady-state  
751 conditions, the  $\text{H}^+$  concentration in the cell contacting the orthoclase surface corresponds to  
752  $C_N = 0.89C_0$  (Fig. 14b). The apparent dissolution rate of orthoclase in this case is  $0.94 \times 10^{-7}$   
753  $\text{mol.m}^{-2}.\text{s}^{-1}$ , which is impossible to distinguish experimentally from the expected rate at  $\text{pH} =$   
754  $2$ . In addition, the duration required to reach a steady-state  $\text{H}^+$  profile within the coating is  
755 negligible compared to the duration of the experiment ( $t^* = 1.7 \times 10^{-2} \text{ s}$ ), so that the impact of  
756 the coating on the orthoclase dissolution rate was not significant for experiment MPA3.  
757 Consequently, the slight loss of reactivity reported previously might be better explained by  
758 the Al inhibition previously suggested in the literature for feldspars (Gautier et al., 1994;  
759 Oelkers et al., 1994) rather than by ion diffusion limitation in the coating.



760

761 **Fig. 14. Main results for the reactive transport modeling of experiment MPA3.** (a) Diffusion  
 762 coefficient across the coating thickness estimated following Archie's law. (b) Evolution of the  $C_N /$   
 763  $C_0$  ratio as a function of  $\log(t)$  for  $m = 2.0$ .  $C_N$  represents the  $\text{H}^+$  concentration in the last  $N$  cell of the  
 764 coating,  $t$  (s) is the diffusion time within the coating.

765

#### 766 4.4.3 Sensitivity tests

767 In order to determine the conditions under which coatings could affect the dissolution  
 768 rate to a greater extent, additional simulations were carried out. Two parameters were  
 769 considered in particular, i.e., the thickness of the secondary coatings and the pH of the bulk  
 770 fluid. For geothermal systems, such parameters are particularly relevant to estimate the impact  
 771 of the coatings on the longer term: on the one hand, the pH of circulating waters will  
 772 gradually return to its value before the acid stimulation, while on the other hand, it can also be  
 773 expected that the thickness of the coatings will gradually increase with time. Finally, the  
 774 impact of the intrinsic dissolution rate constant of the mineral considered will also be  
 775 investigated, to shed light on the impact that secondary coatings may have on minerals more  
 776 reactive than K-feldspars.

777 All simulations were carried out considering a homogenous coating (i.e.,  $\varphi$  and  $D$   
 778 independent of  $x$ ), using time and space increments of  $\Delta t = 10^{-5}$  s and  $\Delta x = 1$  nm, respectively.  
 779 The characteristic time ( $t_{eq}$ ) required to reach steady-state conditions (constant  $C_N$   
 780 concentration) was systematically lower than  $t_{max} = 10$  s, and therefore negligible compared

781 with the duration actually simulated. As emphasized previously, the key parameter for  
782 estimating the effect of coatings on the dissolution rate of orthoclase is the concentration of  
783  $H^+$  ions in the last cell of the coating when the steady-state is reached.

#### 784 *4.4.3.1 Influence of pH*

785 In order to simulate conditions closer to those of the Soultz-sous-Forêts reservoir at the  
786 end of an acid stimulation, the model was run with a bulk fluid at  $pH = 5.3$ , corresponding to  
787 that of the brine measured on-site (e.g., [Sanjuan et al., 2010](#)).

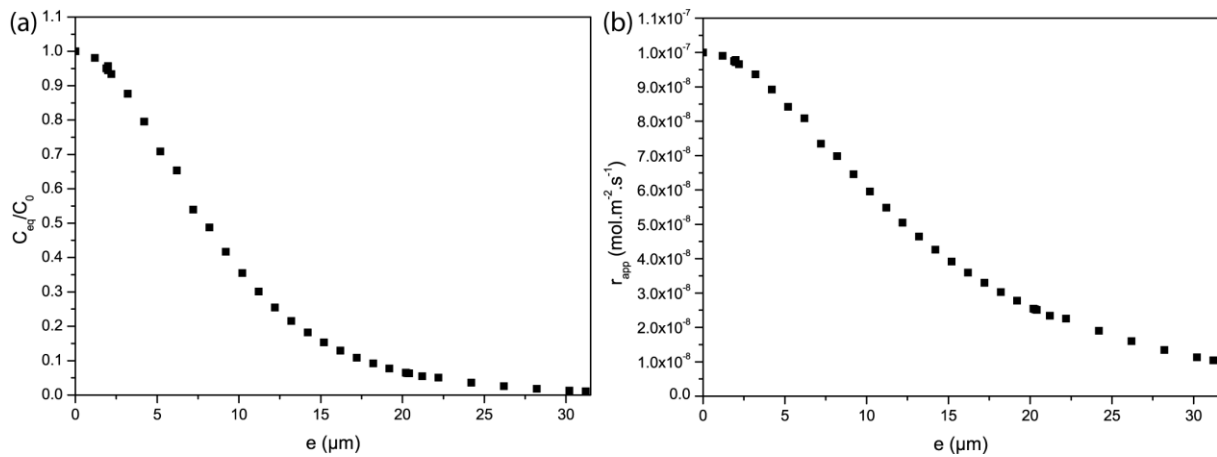
788 Considering the pH-dependence reported in [Palandri and Kharaka, 2004](#), the dissolution  
789 rate of orthoclase is  $2.2 \times 10^{-9} \text{ mol.m}^{-2}.\text{s}^{-1}$  at  $pH 5.3$  and  $180 \text{ }^\circ\text{C}$ . For direct comparison with  
790 previous simulations, porosity and coating thickness were maintained at 22% and  $5.2 \text{ }\mu\text{m}$ . The  
791 results showed that at steady-state, the  $H^+$  concentration in the cell contacting orthoclase is  
792  $0.70C_0 = 3.5 \times 10^{-6} \text{ mol.L}^{-1}$ , corresponding to an apparent dissolution rate of  $1.9 \times 10^{-9} \text{ mol.m}^{-2}.\text{s}^{-1}$  (Fig. S11). The decrease in orthoclase dissolution rate thus reaches 15%, pointing out  
793 that under such conditions, the secondary coating do not play a major role in orthoclase  
794 dissolution kinetics. As a matter of fact, the observed drop in reactivity is close to that  
795 calculated at  $pH 2$ . As a consequence, the gradual increase in  $pH$  after an acid stimulation will  
796 not drastically modify the intrinsic impact of the coatings on orthoclase reactivity.

#### 798 *4.4.3.2 Influence of coating thickness*

799 In order to estimate the impact of secondary coatings at further progress of reaction,  
800 supplementary simulations were conducted, using a fixed porosity maintained at 22%,  
801 corresponding to  $D = 1.6 \times 10^{-9} \text{ m}^2.\text{s}^{-1}$ . The results are reported in Fig. 15. A dramatic drop in  
802  $H^+$  concentration in the cell in contact with orthoclase can be observed when increasing the  
803 coating thickness, which translates into an equivalent drop in the orthoclase dissolution rate  
804 (Fig. 15b). For coating thickness exceeding  $30 \text{ }\mu\text{m}$ , the dissolution rate decreased by nearly  
805 one order of magnitude, illustrating that the coating thickness is a crucial parameter in the



806 buildup of a diffusion boundary layer at the interface with the primary silicate. Of note,  
 807 similar conclusions were reached in previous studies (e.g., [Emmanuel, 2022](#)). Therefore, it is  
 808 likely that in geothermal systems similar to that of Soultz-sous-Forêts, the primary minerals  
 809 will be gradually isolated from the fluid circulations within timescales of a few months,  
 810 according to the combined results of our experimental and simulation observations.



811  
 812 **Fig. 15. Main results for the reactive transport simulations aimed at testing the impact of**  
 813 **secondary coating thickness on orthoclase dissolution rate.** (a) Evolution of the concentration of  
 814  $\text{H}^+$  in the cell in contact with orthoclase with coating thickness. (b) Corresponding evolution of  
 815 orthoclase dissolution rate. See text for details.

816

#### 817 *4.4.3.3 Influence of the intrinsic mineral dissolution rate*

818 A striking feature of all previous simulations is that it was impossible to evidence a  
 819 dramatic drop in the reactivity of the primary phase with coatings having thickness on the  
 820 order of a few microns. However, [Cubillas et al., 2005](#) observed a decrease of 1 to 2 orders of  
 821 magnitude in the dissolution rate of calcite in the presence of secondary phase coatings with a  
 822 thickness of between 3 and 10  $\mu\text{m}$ . Their study was conducted with a mineral whose  
 823 dissolution rate is much higher than that of orthoclase. In an attempt to explain these  
 824 observations, the influence of the intrinsic dissolution rate constant is tested below.

825 To test whether the model developed here can reproduce such a drop in reactivity,  
 826 simulations were carried out using a dissolution rate of  $2.69 \times 10^{-4} \text{ mol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ . This rate is of  
 827 the same order of magnitude as that of calcite at pH 2 and 25 °C ([Palandri and Kharaka, 2004](#);

828 [Cubillas et al., 2005](#)). It should also be noted that the dissolution rate of calcite varies  
829 proportionally to the  $H^+$  concentration ([Palandri and Kharaka, 2004](#)), as opposed to  
830 orthoclase, whose dissolution rate varies proportionally to the square root of  $[H^+]$ . Therefore,  
831 the sink term was adjusted to  $P = \frac{2r_0}{\varphi_N \Delta x} \frac{C_N^t}{C_0}$ .

832 Figure 16 shows the concentration profiles obtained with this dissolution rate. The  
833 simulations were carried out for a coating with a porosity of 22% and a thickness of 5.2  $\mu\text{m}$  or  
834 10  $\mu\text{m}$ . It can be seen that the steady-state concentration in the mesh in contact with the  
835 dissolving mineral is much lower for calcite than for orthoclase (Fig. 16a-b), which translated  
836 into an apparent dissolution rate of calcite of  $1.30 \times 10^{-4} \text{ mol.m}^{-2}.\text{s}^{-1}$ . The observed reduction  
837 in reactivity is 52% for calcite, whereas it was only around 16% for orthoclase (see section  
838 4.4.3), illustrating the critical importance of the magnitude of the sink term in the steady-state  
839 gradient of  $H^+$  across the coating. The impact is even more dramatic if the thickness of the  
840 coating is increased to 10  $\mu\text{m}$  coating (Fig. 16c-d): Under these conditions, the apparent  
841 dissolution rate of calcite is  $5.75 \times 10^{-5} \text{ mol.m}^{-2}.\text{s}^{-1}$ , corresponding to a drop in reactivity of  
842 80%. These results show that a coating of around ten  $\mu\text{m}$  on the calcite surface causes a drop  
843 in reactivity of almost an order of magnitude. This is due to the very high rate at which  $H^+$   
844 ions are consumed by this mineral compared with their transport across the coating. Thus, the  
845 observations of [Cubillas et al., 2005](#) could, in part, be explained by this model.

#### 846 *4.4.3.4 Concluding remarks and role of coatings on long-term scenarios*

847 The simple reactive transport model used here highlighted that the thickness of the  
848 coatings and the intrinsic dissolution rate constant of the dissolving phases are the most  
849 sensitive parameters that can eventually result in a decrease in the dissolution rate of the  
850 primary minerals. Considering coatings of a few tens of  $\mu\text{m}$  and a high  $H^+$  ion consumption  
851 rate at the mineral surface ( $\sim 10^6$  times greater in the case of calcite than orthoclase), the drop  
852 in reactivity induced by the limitation of  $H^+$  ion transport within the coating can be significant

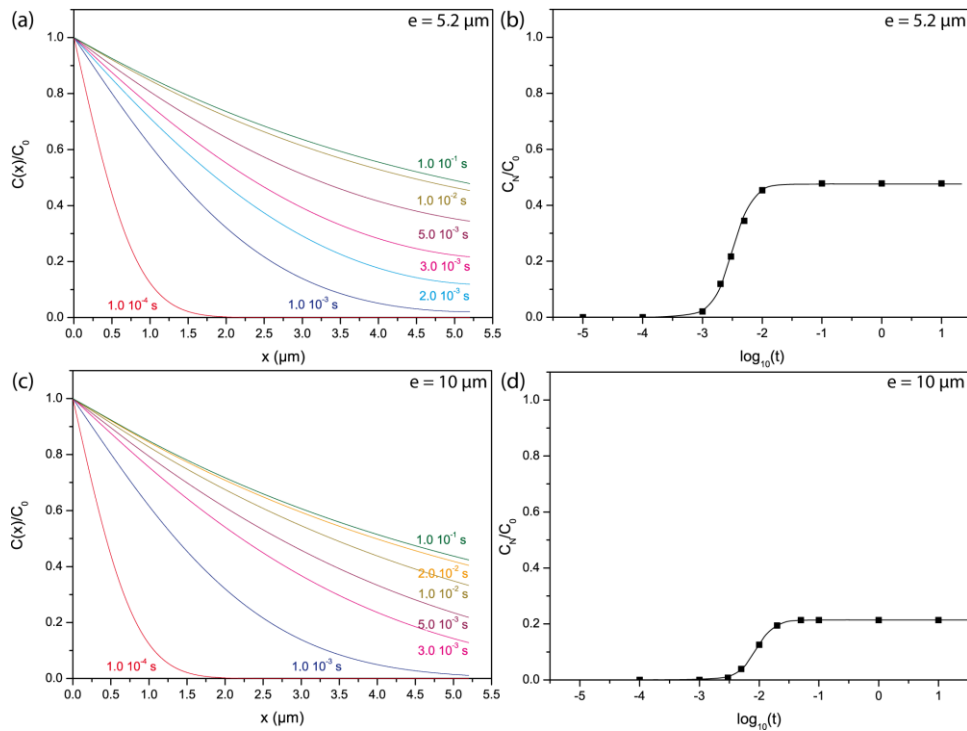
853 (approximately one order of magnitude). This explains why the presence of micron-thick  
854 coatings can have significant effects on calcite (Cubillas et al., 2005) and negligible effects on  
855 feldspars (Hellmann et al., 1989, this study).

856 Regarding the specific case of mineral reactivity in the granitic reservoir of Soultz-sous-  
857 Forêts, combining the experimental observations with modeling results lead to two main  
858 conclusions:

859 (i) first, in case of an acid stimulation aimed at removing barite scaling from the fractures,  
860 the exposure of fresh K-feldspar surfaces resulting from fluid circulation and barite removal  
861 will lead to the formation of new Al-rich coatings that will negligibly impact K-feldspar  
862 dissolution rates, as long those coatings do not fully cover the K-feldspar surfaces, and their  
863 thickness remains limited to a  $\leq 10 \mu\text{m}$ .

864 (ii) Since K-feldspar is the main supplier of Ba (e.g., Azaroual and Fouillac, 1997), the  
865 exposure of K-feldspar surfaces will result in a sustained flux of Ba, which might ultimately  
866 limit the benefits of the acid stimulation. However, the outputs of the model also suggested  
867 that as soon as the Al-rich secondary coatings reach a thickness of several 10s of  $\mu\text{m}$  (which  
868 is expected to happen within a few months), then K-feldspar dissolution rate drops. Therefore,  
869 the increase in Ba release following enhanced K-feldspar dissolution should be transient only,  
870 and the benefit from acidic stimulation should be long-lasting.

871



872

873 **Fig. 16. Main results for the reactive transport simulations aimed at testing the impact of**  
 874 **secondary coating on calcite dissolution rate at pH = 2 and 25 °C for a coating thickness of 5.2**  
 875  **$\mu\text{m}$  (a, b) or 10  $\mu\text{m}$  (c, d). The  $\text{H}^+$  concentration across the coating as a function of time is**  
 876 **represented in Figs 16a and 16c, while the concentration of  $\text{H}^+$  in the mesh contacting calcite is**  
 877 **represented in Figs. 16b and 16d. See text for details.**

878

## 879 5. Conclusions

880 In this study, dissolution experiments and coupled dissolution-precipitation experiments  
 881 were conducted to evaluate the impact of secondary coatings on the reactivity of orthoclase, a  
 882 feldspar representing one of the main rock-forming minerals of the granitic reservoir of the  
 883 Soultz-sous-Forêts geothermal system. This study was conducted in view of the limited  
 884 existing literature aimed at quantifying the impact of secondary coatings on primary mineral  
 885 dissolution at high pressure-high temperature conditions. Overall, we found that experiments  
 886 conducted in conditions of supersaturation with respect to Al-bearing secondary phases  
 887 resulted in a modest decline of orthoclase dissolution rate only. The precipitation of boehmite  
 888 directly on orthoclase grains did not seem to significantly impact orthoclase reactivity, whose  
 889 rate decrease may be better explained by the impact of dissolved Al in the bulk fluid. This

890 result was independently confirmed by running reactive transport simulations, which revealed  
 891 that the impact of secondary coatings may become significant only when their thickness  
 892 exceeds a few tens of microns, or if the reactivity of the primary phase is significantly greater  
 893 ( $10^6$  times) than that of orthoclase.

894 This study should be seen as a first step in a general effort aimed at better constraining  
 895 the evolution of the ‘effective surface area’ of dissolving phases, a critical parameter for  
 896 predicting mineral dissolution rates in the field, which is more often than not used as a fitting  
 897 parameter in modeling exercises. Future studies may include experiments run over longer  
 898 durations to enlighten the impact of the increase in coating thickness (suggested numerically  
 899 to play an important role in the decrease in dissolution rate of the primary phases) and/or a  
 900 change in the mineralogy of secondary phases, as clays might have an even more important  
 901 armoring impact on silicate dissolution rates (e.g., [Zhu, 2005](#)).

902

903

## 904 **Appendix**

### 905 **A1. Integration of the transport equation**

906 The integral of the transport equation (Eq. 2) is defined as follows:

$$907 \int_{k-1/2}^{k+1/2} \varphi \frac{\partial C}{\partial t} dx = \int_{k-1/2}^{k+1/2} \frac{\partial}{\partial x} \left( D \left( \frac{\partial C}{\partial x} \right) \right) dx \quad (\text{A1})$$

908 Using an implicit time scheme (discretization at  $t+1$ ) the integrals for cell  $k$  can be expressed  
 909 as:

$$910 E(k)C_k^{t+1} + F(k)C_{k+1}^{t+1} + G(k)C_{k-1}^{t+1} = C_k^t \quad (\text{A2})$$

911 where:

$$912 E(k) = 1 + \frac{\Delta t}{\varphi_k \Delta x^2} D_{k+\frac{1}{2}} + \frac{\Delta t}{\varphi_k \Delta x^2} D_{k-\frac{1}{2}} \quad (\text{A3})$$

$$913 F(k) = -\frac{\Delta t}{\varphi_k \Delta x^2} D_{k+\frac{1}{2}} \quad (\text{A4})$$

914  $G(k) = -\frac{\Delta t}{\varphi_k \Delta x^2} D_{k-\frac{1}{2}}$  (A5)

915 Implementing the upstream and downstream boundary conditions, Equation (A1) can then be  
 916 written in matrix form as follows:

917 
$$\begin{pmatrix} E(1) & F(1) & 0 & \dots & 0 & 0 & 0 \\ G(2) & E(2) & F(2) & \dots & 0 & 0 & 0 \\ 0 & \vdots & \vdots & \dots & \vdots & 0 & 0 \\ 0 & \vdots & \vdots & \ddots & \vdots & \vdots & 0 \\ 0 & 0 & \vdots & \dots & \vdots & \vdots & 0 \\ 0 & 0 & 0 & \dots & G(N-1) & E(N-1) & F(N-1) \\ 0 & 0 & 0 & \dots & 0 & G(N) & E(N) \end{pmatrix} \begin{pmatrix} C_1^{t+1} \\ C_2^{t+1} \\ \vdots \\ \vdots \\ C_{N-1}^{t+1} \\ C_N^{t+1} \end{pmatrix} =$$

918 
$$\begin{pmatrix} C_1^t - G(1)C_0 \\ C_2^t \\ \vdots \\ \vdots \\ C_{N-1}^t \\ C_N^t - \frac{4r_0\Delta t}{\varphi_N\Delta x} \sqrt{\frac{C_N^t}{C_0}} \end{pmatrix}$$
 (A6)

919 where:

920  $E(1) = 1 + \frac{\Delta t}{\varphi_1\Delta x^2} D_{1+1/2} + \frac{2\Delta t}{\varphi_1\Delta x^2} D_{1-1/2}$

921  $E(k) = 1 + \frac{\Delta t}{\varphi_k\Delta x^2} D_{k+1/2} + \frac{\Delta t}{\varphi_k\Delta x^2} D_{k-1/2}$ , for  $1 < k < N$

922  $E(N) = 1 + \frac{\Delta t}{\varphi_N\Delta x^2} D_{N-1/2}$

923  $F(k) = -\frac{\Delta t}{\varphi_k\Delta x^2} D_{k+1/2}$ , for  $1 \leq k \leq N$

924  $G(1) = -\frac{2\Delta t}{\varphi_1\Delta x^2} D_{1-1/2}$

925  $G(k) = -\frac{\Delta t}{\varphi_k\Delta x^2} D_{k-1/2}$ , for  $1 < k \leq N$

926 The system of equations was solved using Gauss's direct Pivot method. Simulations were  
 927 performed with a cell size  $\Delta x = 1$  nm and a constant time step  $\Delta t = 10^{-6}$  s.

928

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940

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